

Business from technology

Finnish Country Highlights – Biomass Gasification in 2014

IEA Task 33 meeting, KIT Nov2014 Ilkka Hannula

Metsä-Botnia, Joutseno gasification plant for lime kiln Metso's Gasification Projects



CARBONA

RECENT PROJECTS:

Biomass and waste gasification for boilers and kilns

Vaskiluodon Voima – Substituting Coal for Biomass in a PC boiler

- 140 MW_{th} gasifier adjoined to the existing 560 MW coal-fired power plant
- PC boiler in operation since 1982
- Coal consumption 400,000 – 500,000 t/a
- Enables to replace up to 40 percent of coal
- Production capacity
 - electricity 230 MW
 - district heating 170 MW
- Vaskiluodon Voima's total investment ~40 MEUR

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Lahti Energia – Gasification Power Plant

2 x 80 MW_{th} gasifiers Waste-derived fuel 50 MW_e & 90 MW_{heat}

- 1. Fuel handling
- 2. Gasifier
- 3. Gas cooling
- 4. Gas filter
- Gas boiler and flue gas cleaning

Start-up April 2012 Total investment 157 M€









Model:

Volter 30 (40)

Fuel:	Wood chips (birch, spruce, pine, aspen)	
Fuel moisture:	<18%	
Particle size:	8 mm $\leq P \leq 50$ mm, fine particles (<3,15mm) <1%, all <63mm	
Plant structure:	Steel frame, Insulated with paroc (or similar) panels	
Color:	As per agreement	
Fuel supply:	Spring agitator, auger, rotating feeder	
Generator:	Agco Sisu Power 4,9L, 4-cyl. <mark>(8,4L, 6-cyl.)</mark>	
Dutput:	Generator output 30kW (40kW), thermal 80kW (100kW)	
Plant usage (e):	ca. 1,5-2,5kW	
Fuel consumption:	ca. 3,5 m3 (4,5 m3) of chips/24h at 100% power level	
Automation:	Schneider electric PLC, GSM –alarms, remote internet control	
Connections:	Electricity cable, Heat channel, water line, broadband, GSM-connection	
nstallation:	Asphalt or concrete base	
Ash removal:	Automatic ash removal	
Max. o.t./a:	7000h	SIVIALL-SCALE
Maint. interval:	once a week	CONTRICT LIEAT AND DOVATED
Other:		COMBINED HEAT AND POWER



R&D Partners: University of Eastern Finland



Volter 30
Installed inside an existing building

- VTT will move it's Gasification and Pyrolysis test facilities to an industrial area in Kivenlahti, Espoo
- New pilot plants will also be constructed
- Start-up at new site in Q4/2014-Q1/2015
- Efficient development from laboratory to industrial realization

Horizon 2020-projects, 2015-2020 Biofuels for transport sector, renewable chemicals Fuel gas & pyrolysis oil for CHP and industrial applications Waste-to-Energy with material recovery **Industrial projects VTT RES-Infra /TT RES-Infra** Ruukinmestarintie 2, Kivenlahti, Espoo Pyrolysis and gasification R&D Investment Testing and piloting services New R&D Platform Platform for new pilot plants 2013-2015

2G Biofuels R&D and Piloting project

7.2 M€: 2012-14, 2nd phase planned for 2015-16





Pilot/PDU-scale Gasification Test facilities

Intermediate pressure CFB gasification pilot plant (existing test rig)

- Pressure 2-6 bar, fuel capacity max. 0.5 MW, gas flow rate 200 m3n/h •
- CFB-gasifier, fluidisation by air/O₂/steam/recycle gas
- High-temperature filter, tar and methane reforming, gas cooling
- Slip stream or full stream testing of final gas clean-up and synthesis processes
- Large-scale synthesis gas applications

Dual fluidised-bed gasification pilot plant DFB (present plant will be modified)

- Fuel capacity max. 300 kW, Air gasification with single gasifier reactor (mainly waste gasification)
- Dual-Bed steam gasification High-temperature filter, tar and methane reforming, gas cooling •
- Smaller size syngas applications 50 .. 150 MW to be integrated to forest industries and CHP ٠

Bench-scale gasification and gas cleaning facilities

- Atmospheric-pressure BFB gasifier with hot filtration and catalytic reforming (syngas & fuel gas) New •
- Atmospheric-pressure CFB gasifier with hot filtration (fuel gas applications) •
- Pressurized BFB gasification reactor for fuel and bed material characterization New ٠
- Pressurized filtration and reforming test facilities (operation with slip streams or with synthetic gas) •
- Catalytic conversion R&D laboratory, Fuel reactivity and ash sintering R&D laboratory (at Otaniemi) •

High-Pressure BFB gasification PDU (new test facility, to be built in 2015)

- Bubbling Fluidised-Bed gasification, fluidisation by air/O₂/steam/recycle gas
- max. pressure 25 bar, thermal capacity max. 0.5 MW, gas flow rate ca. 200 m3n/h
- High-temperature filter, tar and methane reforming, gas cooling
- Slip stream or full stream testing of final gas clean-up and synthesis processes

Auxiliary equipment

- Gas boiler with two-way connection to DH network of Espoo
- Fuel pretreatment unit, steam generators, compressors, sampling and analytical systems





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Pyrolysis Test facilities at Kiviruukki

Fast Pyrolysis CFB Pilot Plant (current PDU to be scaled-up and modified)

- Bio fuel oil test production fuel for boilers and ovens
- Catalytic fast pyrolysis feed for hydro-treatment of co-feed to a refinery
- Capacity 350 kg of bio fuel oil or 150 kg of catalytic bio-oil a day, about 100 kW of feed biomass

Fast Pyrolysis BFB Bench-Scale Unit (current bench-unit to be modified)

- Characterization of biomass for fast pyrolysis base data for mass & energy balances for technoeconomic evaluations
- Both inert (Al₂O₃) and catalytic (zeolites) operation fuel oils and co-feeds for refineries
- Capacity 1 kg/h feed

Batch Unit for Slow Pyrolysis

- Indirect heating of samples
- Volume 100 liter, maximum temperature of heating oven 1100 °C
- Amount of sample 6 kg, maximum temperature reactor about 550 °C
- Computer controlled, sampling for solids, liquids and gases

Pyrolysis Bio-Oil Test Rig

- Development of filtration, pumping, heating, homogenization, and for material testing in pilot-scale
- Feed vessel 1 m3, volume flow up to 2 m³/h



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- Method for integrating RE with synthetic biofuels production via electrolytic hydrogen
- Implementation based on commercial components, no new technologies required
- Combines continuous biofuel production with periodical production boosts from RE

Electrolyser enhanced Biomass to fuels

Fig1. Configuration suitable for regulating syngas stoichiometry with a combination of water-gas shift and external hydrogen input









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Fig 3. Investment estimate and lev. production cost for a plant producing 200 MW of synthetic fuel: T=thermochem, E=electrochem. H=hybrid, N=natgas, M=MeOH, G=gasoline

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Thanks – Kiitos!

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