Status report on thermal gasification of bimass and waste 2019 Dr. Jitka Hrbek

Annex 4 Gasification facilities for fuel synthesis – Non operational, historical (project cancelled before 2012), stopped while under construction, deconstructed, idle, on hold

Owner	Project name	Country	Page
bioenergy 2020+	One Barrel per Day Pilot Plant	AT	2
BioMCN	BioMCN commercial	NL	3
BioMCN	Woodspirits	NL	4
Bio SNG Guessing	Synthesis Demo Guessing	AT	5
Chemrec AB	BioDME	SE	6
CHOREN Industries GmbH	Synthesis CHOREN alpha plant Freiberg	DE	7
CHOREN Fuel Freiberg GmbH & Co. KG	Synthesis CHOREN beta plant Freiberg	DE	8
CHOREN Industries GmbH	Synthesis CHOREN sigma plant Schwedt	DE	9
E.ON Gasification Development AB	Bio2G	SE	10
Goteborg Energi AB	GoBiGas Phase 1	SE	11
LTU Green Fuels	DP1+DME pilot	SE	12
Range Fuels, Inc.	K2A Optimization Plant	USA	14
Rottneros AB	Vallvik Biorefinery	SE	15
Tesoro	former Virent Eagle Demonstration Plant	USA	16
TUBITAK MRC - ENERGY INSTITUTE - TURKEY	Synthesis TUBITAK MRC Kocaeli	TR	17
Vienna University of Technology / BIOENERGY 2020+	FT pilot Guessing	AT	18

Project name	One Barrel per Day Pilot Plant
Project owner	Bioenergy 2020+
Status	On hold
Start up	2016
Country	Austria
City	Guessing
Type	TRL 4 - Demo
Technology	Fuel synthesis
Raw Material	Syngas from gasifier (50 m3/h)
Output Name	FT liquids
Output Capacity	53
Output 2 Unit	m3/y
Technology Brief	This pilot plant enabled to scale up from laboratory to pilot scale. In Guessing since 2005 research has been conducted at a biomass-based laboratory scale FT lab plant in the size of 10 LPD (liter per day) and valuable insights into the topics of gas purification and processing, long-term stability of FT catalysts, design of slurry reactors and product separation as well as fractionation have been gained. The collected findings have been incorporated into the planning of this pilot plant. The pilot scale represents an important if not the most important milestone on the way to a demonstration facility. The pilot plant consists of a gas cleaning section for purifying the synthesis gas to sulfur levels less than 10 ppbv. The gas is cleaned from aromatic compounds, sulfur, NH3 and water. The cleaned gas is subsequent compressed to a maximum pressure of 25 bar. The compressed gas enters the second part of the pilot plant, the synthesis part. H2 and CO are converted into a broad range from CH2-compounds ranging from C1 (methane) to more than C60.
Additional Information	https://www.bioenergy2020.eu/de/kompetenzbereiche/alle_projekte/view/394
Contact	Email: gerald.weber@bioenergy2020.euPhone: + 43 (0) 3322 42606-154 , reinhard.rauch@kit.edu



е	
iodiesel	
ane	
their	
le;	
iodiesel	
Contact BIOMCN Crude gycerol Landing facilities MP Super healer MP Steam HP Steam Turbine Turbine Titrone	
1	

Project name	Woodspirit
Project owner	BioMCN
Status	On hold
Country	The Netherlands
City	Delfzijl, Groningen
Туре	TRL 8 First-of-a-kind commercial demo
Technology	Fuel synthesis
Raw Material	Wood chips
Output 1 Name	Methanol
Output 1 Capacity	413 000
Output 1Unit	t/y
Partners	Waterland, Teijin, NOM
Technology Brief	no recent communication on plans to further carry on this project, probably awaiting investors
Additional Information	www.biomcn.eu
Contact	info@biomcn.eu

Project name	Synthesis Demo Guessing
Project owner	Bio SNG Guessing
Status	Operational
Start up	2008
Country	Austria
City	Guessing
Type	TRL 6-7 Demonstration
Technology	Fuel synthesis
Raw Material	Lignocellulosic crops
Input 1 Name	Syngas from gasifier (FICFB Guessing)
Input 1 Capacity	350
Input 1Unit	m3/y
Output 1 Name	SNG
Output 1 Capacity	576
Output 1Unit	t/y
Partners	Vienna University of Technology, Austria; Paul Scherrer
	Institute, Switzerland; Repotec, Austria
Contact	Martin Schaub martin.schaub@ctu.ch
A sh	Gas Engine H ₂ Recycle Streams
& Solid	Methanation SNG Purification SNG Fueling Station CO ₂ Product (to substitute N ₂)
• • • • • • • • • • • • • • • • • • •	/
	Bio-SNG Fue

Project name	BioDME
Project owner	Chemrec AB
Status	Idle
Start up	2011
Country	Sweden
City	Piteå
Type	TRL 4 - pilot
Technology	Fuel synthesis
Raw Material	Lignocellulosics
Input 1 Name	Black liquor gasification
Input 1 Capacity	20
Input 1Unit	t/d
Output 1 Name	DME
Output 1 Capacity	1 800
Output 1Unit	t/y
Total investmenst	EUR 28 500 000
Technology brief	The project was cancelled in 2012. The recovery boiler in the paper mill is replaced or supplemented by a gasification based fuel generating and pulp mill cooking chemicals recovery system. The BioDME pilot is an integrated part of heavy DME fuelled vehicle fleet trials.
Partners	AB Volvo, Haldor-Topsoe, Preem, Total, Delphi, ETC
Contact	Patrik Lownertz patrik.lownertz@chemrec.se

Low temperature gasifier

High temperature gasifier

Project name	Synthesis CHOREN alpha plant Freiberg
Project owner	CHOREN Industries GmbH
Status	Idle
Start up	2002
Country	Germany
City	Freiberg
Type	TRL 4-5 Pilot
Technology	Synthesis
Raw Material	Lignocellulosic biomass
Output 1 Name	FT liquids
Output 1 Capacity	53
Output 1Unit	t/y
Contact	info@choren.com +49 3731 2662 0
Biomass Recuperator Scrubber Upgrading	

Dustremoval Gas shift reactor

FT Synthesis

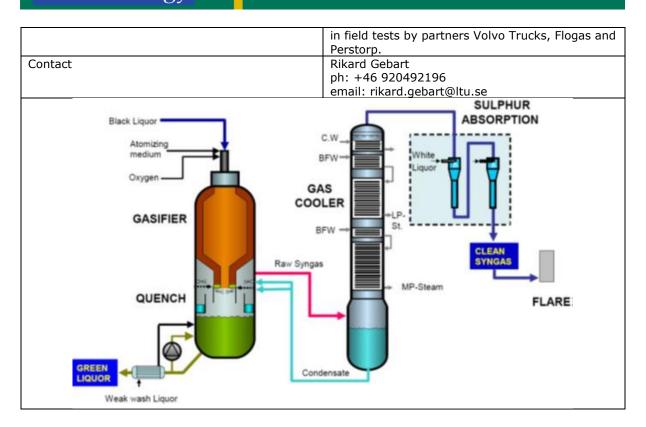
Project name	Synthesis CHOREN beta plant Freiberg
Project owner	CHOREN Fuel Freiberg GmbH
Status	Idle (project cancelled before 2012)
	2002
Start up	
Country	Germany
City	Freiberg TRL 6-7 demo
Type	
Technology	Synthesis
Raw Material	Lignocellulosic biomass
Input	dry wood chips from recycled wood and residual
	forestry wood; additionally in the future fast
	growing wood from short-rotation crops
Output 1 Name	FT liquids
Output 1 Capacity	13 500
Output 1Unit	t/y
Total investment	EUR 190 000 000
Contact	info@choren.com +49 3731 2662 0
Biomass Recuperator Low temperature gasifier High temperature gasifier Dust- removal	

Project name	Synthesis CHOREN sigma plant Schwedt
Project owner	CHOREN Industries GmbH
Status	Stopped while under construction
Start up	
Country	Germany
City	Schwedt
Type	TRL 8 First-of-a-kind commerial demo
Technology	Fuel synthesis
Raw Material	Lignocellulosic crops
Input 1 Name	Dry wood chips from recycled wood; fast growing
	wood from short-rotation crops
Output 1 Name	FT liquids
Output 1 Capacity	200 000
Output 1Unit	t/y
Contact	info@choren.com
	+49 3731 2662 0

Project name	Bio2G
Project owner	E.ON Gasification Development AB
Status	idle
Start up	
Country	Sweden
City	Scania province
Туре	TRL 9 Commercial
Technology	Fuel Synthesis
Raw Material	Other
Input 1 Name	Woody Biomass
Input 1 Capacity	300
Input 1Unit	MW
Output 1 Name	SNG / bio-methane
Output 1 Capacity	200
Output 1Unit	MW
Output 2 Name	Heat
Output 2 Capacity	50
Output 2 Unit	MWth
Partners	Partners in the technical and project development phase has been Andritz Carbona Oy and Haldor Topsoe AS
Technology Brief	The technology selected for the gasification system is based on pressurised oxygen blown gasification in a fludized bed followed by hot gas cleaning (tar reforming, HAT filter), cold gas cleaning (water scrubber, acid gas removal), compression, WGS and synthesis of methane.
Contact	Björn Fredriksson-Möller +46 40 255 716 email: bjorn.moller@eon.se

	T	
Project name	GoBiGas (phase I)	
Project owner	Goeteborg Energi	
Status	idle	
Start up	2014	
Country	Sweden	
City	Ryahamnen, Göteborg	
Type	TRL 8 First-of-a-kind commercial demo	
Technology	Fuel Synthesis	
Raw Material	Lignocellulosic crops	
Output 1 Name	SNG	
Output 1 Capacity	11 200	
Output 1Unit	t/y	
Output 2 Name	Heat	
Output 2 Capacity	5	
Output 2 Unit	MWth	
Output 3 Name	Power (electricity)	
Output S Name Output Capacity	6	
	MWel	
Output Unit		
Partners	Repotec, Metso Power, Jacobs Process, Haldor	
Takal bassa dan and	Topsoe	
Total investment	EUR 150 000 000	
Technology Brief	The gasification technology is based on the	
	Repotec indirect gasification, which is	
	supplemented by gas upgrading and SNG	
	synthesis. Goteborg Energi decided to divest the	
Additional Tofonsakian	plant in 2017, and this process is on-going.	
Additional Information	http://gobigas.goteborgenergi.se/	
Contact	Cecilia Erdaien	
Contact Cecilia Erdalen GoBiGas 20 MW GoBiGas 20		
<i>Ġ</i> Göteborg Energi		

Project name	DP1+DME pilot
Project owner	LTU Green Fuels
Status	On hold
Start up	2011
Country	Sweden
City	Pitea
Type	TRL 4-5 Pilot
Technology	Fuel Synthesis
Raw Material	Other
Input 1 Name	Black Liquor
Input 2 Name	Pyrolysis oil (co-gasification with black liquor)
Output 1 Name	Clean Syngas
Output 1 Capacity	2
Output 1Unit	MW
Output 2 Name	DME
Output 2 Capacity	4
Output 2 Unit	t/d
Output 3 Name	Methanol
Output 3 Capacity	4
Output 3 Unit	t/d For the Riccyngae program the partners are
Partners	For the Biosyngas program the partners are Chemrec AB, Haldor Topsöe, Volvo Truck, Preem,
	Smurfit Kappa, Sveaskog, Perstorp, Södra,
	Holmen, Flogas and ETC.
Technology Brief	The Chemrec process uses a refractory-lined
	entrained bed reactor in which concentrated black
	liquor (or black liquor + pyrolysis oil) is gasified
	under reducing conditions at around 1000°C. The
	liquor is decomposed in the reaction zone into
	melt droplets consisting of sodium compounds,
	and a combustible gas containing H2 and CO. The
	melt droplets and the combustible gas are
	separated in a quench dissolver where they are
	simultaneously brought into direct contact with a cooling liquid. The melt droplets dissolve in the
	liquid to form a green liquor solution. The gas
	leaving the quench dissolver is cooled producing
	steam. The cooling is done in counter current
	mode which means that the gas is efficiently
	washed of particulate matter. The gas is then free
	of melt droplets and can be scrubbed for H2S
	removal and then used as a clean fuel or syngas.
	The DME pilot was installed in 2011. Since the
	end of the Chemrec BLG program and the Bio-
	DME project in 2012, an industrially co-funded
	160 MSEK R&D program was initiated in 2014 with the obejct ive of widening the fuel basis,
	develop new synthesis gas cleaning and synthesis
	reactror and catalyst technologies
Additional information	Until May 2016 the plant has been operating as
	follows: • Entrained flow gasifier: 27 000 hours,
	most of the time with pressure close to 30 bar
	and fuel flow rate corresponding to 3 MWth. The
	oxidant has after initial optimization been nearly
	100% oxygen (and small amounts of nitrogen for
	safety and purging purposes). In the spring of
	2016 we co-gasified pyrolysis oil with black liquor
	for over 1000 hours. The pyrolysis oil came from
	two commercial plants in Finland (Fortum) and Holland (Empyro) and was transported in trucks
	to Piteå, Sweden. • Downstream syngas train: 12
	000 hours, more than 1000 ton DME. In the last
	few months of operation we extracted slightly
	more than 50 ton raw methanol for testing
	purposes. The DME and methanol has been used
<u> </u>	



Project name	K2A Optimization Plant
Project owner	Range Fuels, Inc.
Status	Non operational
Start up	2008
Country	USA, Colorado
City	Denver
Туре	TRL 4-5 Pilot
Technology	Fuel synthesis
Raw Material	Lignocellulosic crops
Input 1 Name	Georgia pine and hardwoods and Colorado beetle
	kill pine
Output 1 Name	Mixed alcohols
Partners	GreenWood Resources
Additional Information	Range Fuels is no longer a functioning company
Contact	Patrick Wright
	patrick@rangefuels.com
	www.rangefuels.com

Project name	Vallvik Biorefinery
Project owner	Rottneros AB
Status	idle
Start up	
Country	Sweden
City	Vallvik
Туре	TRL 9 Commercial
Technology	Fuel Synthesis
Raw Material	Lignocellulosic crops, black liquor
Output 1 Name	Methanol
Output 1 Capacity	200 000
Output 1Unit	t/y
Additional Information	www.rottneros.com
Contact	Ole Terland +46 70 667 0403
	ole.terland@rottneros.com

Project name	Former Virent Eagle Demo Plant
Project owner	Tesoro
Status	Idle
Start up	2009
Country	USA
City	Madison
State	Wisconsin
Type	TRL 6-7 Demonstration
Technology	Fuel Synthesis
Raw Material	Other
Input 1 Name	Cane sugar, beet sugar, corn syrup, hydrolysates from cellulosic biomass including pine residues, sugarcane bagasse and corn stover
Output 1 Name	Diesel-type hydrocarbons
Output 1 Capacity	30
Output 1Unit	t/y
Partners	Virent Inc.
Technology Brief	Virent™s BioForming® platform is based on a novel combination of Aqueous Phase Reforming (APR) technology with modified conventional catalytic processing. The APR technology was discovered at the University of Wisconsin in 2001 by Virent™s co-founders. The BioForming platform expands the utility of the APR process by combining APR with catalysts and reactor systems similar to those found in standard petroleum oil refineries and petrochemical complexes. The BioForming process converts aqueous carbohydrate solutions into mixtures of drop-in hydrocarbons. The process has been demonstrated with conventional sugars obtained from existing sugar sources (corn wet mills, sugarcane mills, etc.) as well as a wide variety of cellulosic biomass from nonfood sources. A key advantage to the BioForming process is the ability to produce hydrogen in-situ from the carbohydrate feedstock or utilize other sources of hydrogen such as natural gas for higher yields and lower costs.
Additional Information	Tesoro acquired Virent to proceed with the technology development but obviously the facility is idle.
Contact	aaron imrie@virent.com

Project name	Synthesis TUBITAK MRC Kocaeli
Project owner	TUBITAK MRC - ENERGY INSTITUTE - TURKEY
Status	Idle
Start up	2009
Country	Turkey
City	Kocaeli
Туре	TRL 4-5 Pilot
Technology	Fuel Synthesis
Raw Material	Biomass / biomass coal blends
Output 1 Name	SNG
Output 1 Capacity	0,2
Output 1Unit	MW
Partners	Nationally Funded Project
Technology Brief	Down draft fixed bed gasifier
Contact	Synthesis Kocaeli Mr. Alper Unlu

Project name	FT pilot Guessing
Project owner	Vienna University of Technology / BIOENERGY
	2020+
Status	On hold
Start up	2005
Country	Austria
City	Guessing
Туре	TRL 4-5 Pilot
Technology	Fuel synthesis
Raw Material	Syngas from FICFB Gasifier
Output 1 Name	FT liquids
Output 1 Capacity	5
Output 1Unit	kg/day
Output additional Information	Raw FT product 5 kg/d
Technology Brief	Aim of the work is to convert the product gas (PG) of the Biomass gasification plant with a Fischer-Tropsch (FT) process to liquid fuels, especially to diesel. A FT-pilot plant is operated, which converts about 5 Nm3/h PG at 20bar in a Slurry reactor to FT-products. The gas cleaning of the raw PG consists of several steps and consists of wet scrubbers and dry adsorbers. As catalyst in the slurry reactor, iron and cobalt based catalyst are used. The results from a Cobalt catalysts give mainly an n-alkane distribution from C1 to compounds higher than C60 n-alkanes. The iron based catalysts give more alkenes and oxygenated compounds. The analyses of the diesel fraction from the distillation of the FT-raw product show that the obtained diesel from the Cobalt catalyst has cetan-numbers of about 80 and is free of sulphur and aromatics.
Contact	Reinhard.rauch@kit.edu