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IMAGINEERING
NATURE

Results from the 100 kW dual fluidized bed gasifier at TU Wien

Florian Benedikt, Josef Fuchs, Anna Mauerhofer, Stefan Müller, Johannes Schmid, Hermann Hofbauer

IEA FBC and IEA Bioenergy Task 33 Gasification of Biomass and Waste

Joint workshop in Skive, Denmark:

Fluidized Bed Conversion of Biomass and Waste

24.10.2017

Vision for gasification technology at TU Wien

RESSOURCES



low grade wood chips



biogenic residues



industrial waste



homogenous municipal waste



sewage sludge manure

rising technological challenges with respect to gasification & gas cleaning




heat



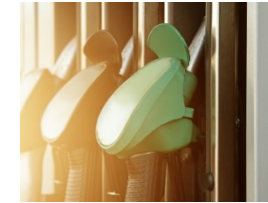
electricity



hydrogen



synthetic natural gas

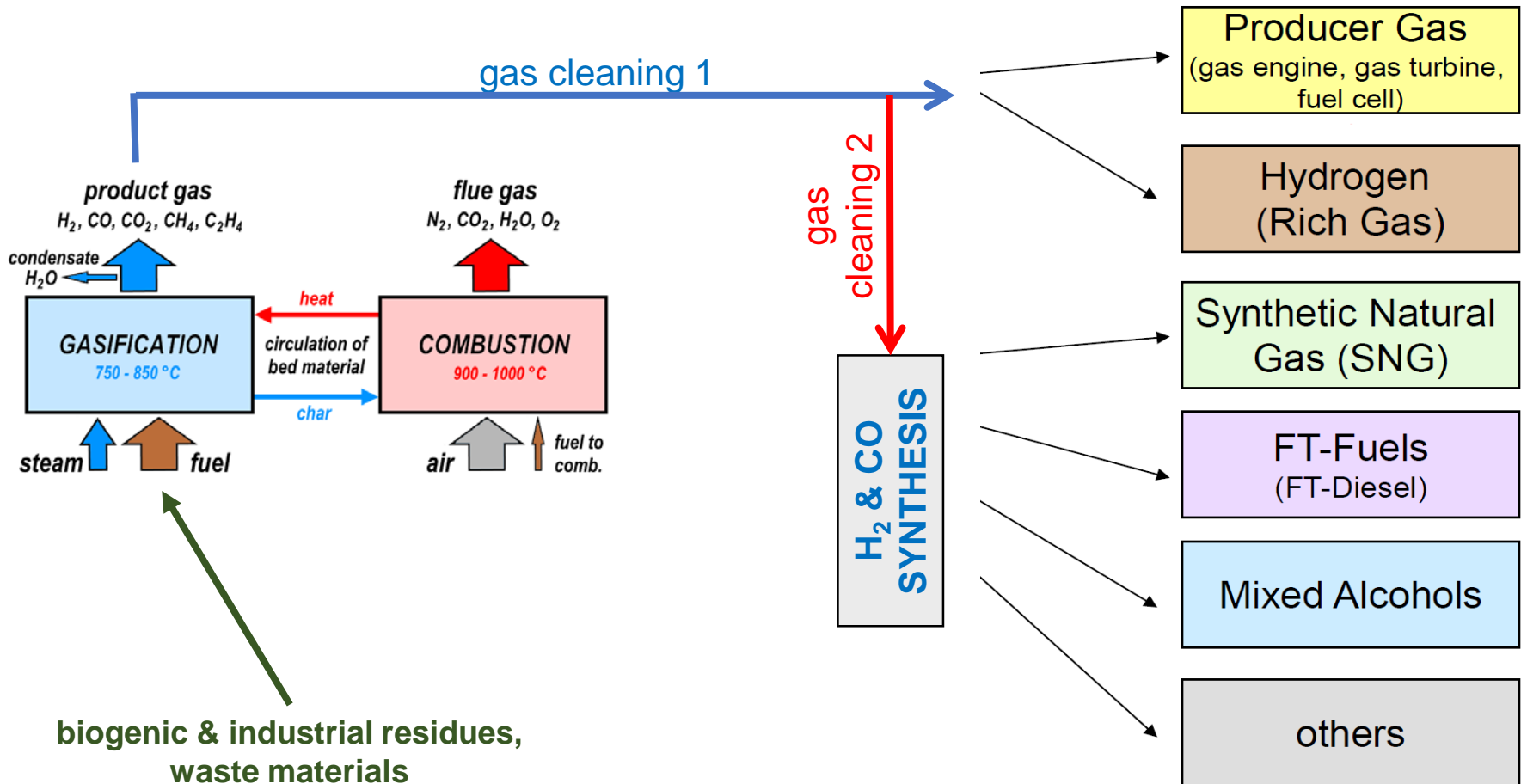


transportation fuels & basic chemicals

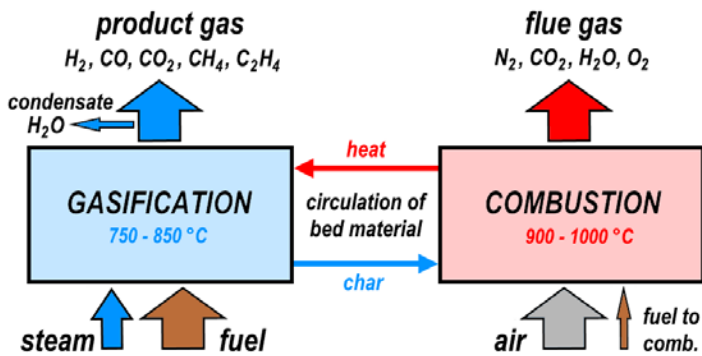
PRODUCTS

- Objectives:**
- Increasing the fuel flexibility
 - Optimization of gasification (bed materials)

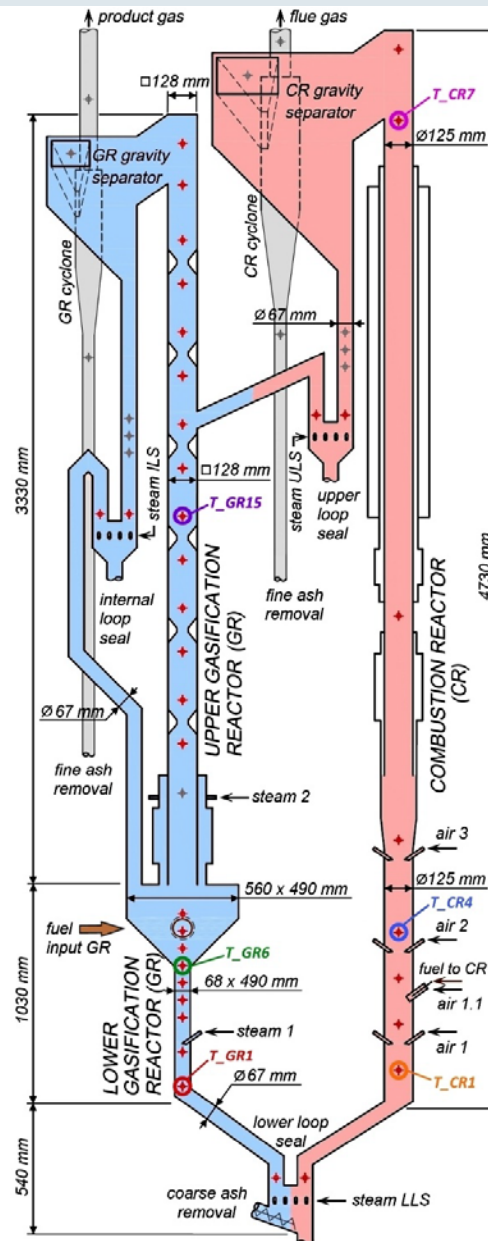
Dual fluidized bed steam gasification



Basic principle and Reactor system:



Dual fluidized bed steam gasification



100 kW_{th} Gasification Pilot Plant at TU Wien

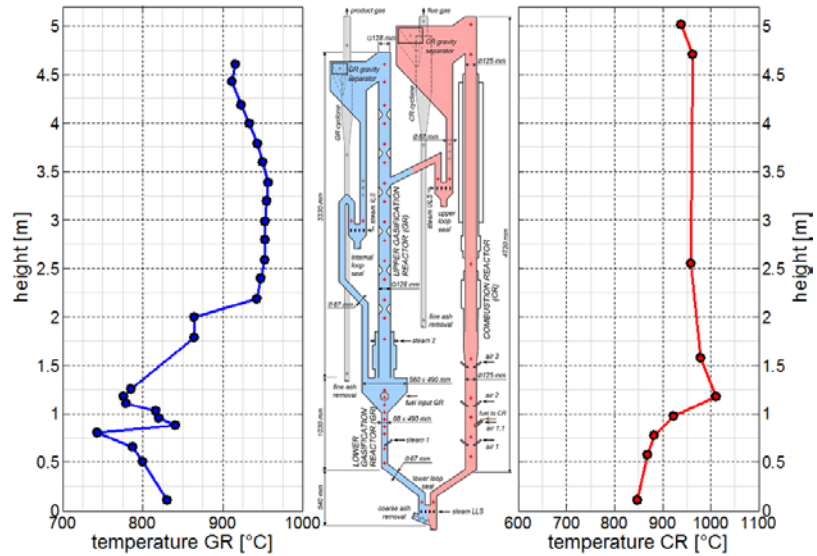


- Height: 7.5 m
- Base area: 35 m² per floor (2)
- 105 Temperatures
- 70 Pressures
- 13 Volume/mass flows
- 22 Values of gas analyses

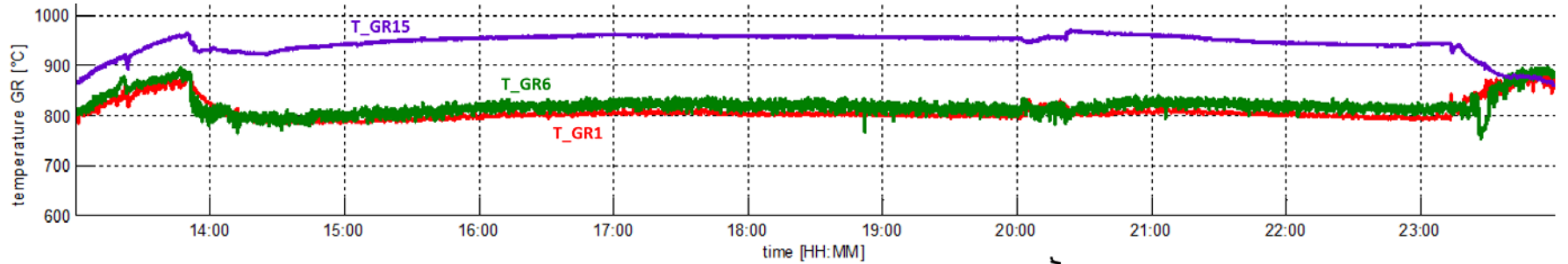


Typical test run:

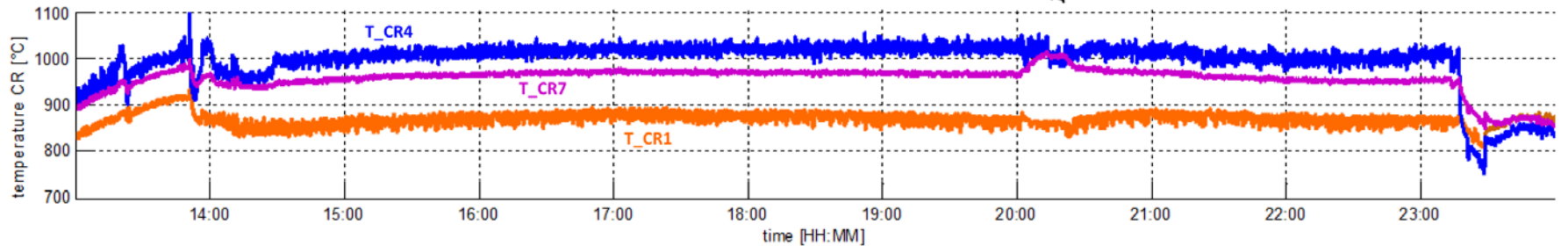
Temperature profiles



Temporal course of temperatures



end of heat-up procedure switching to steam tuning phase steady-state operation phase 1 top up fuel hopper tuning phase steady-state operation phase 2 start of shut-down procedure



?? Fuels of the future ??

Wood chips



soft wood pellets



Fuels gasified at TU Wien

Coal



Wood chips



Bark pellets



Wheat bran pellets



Reed grass



Empty palm fruits



Palm leaves



Sugar cane bagasse



Sugar cane residues



waste wood A



waste wood B



waste wood C



soft wood pellets



saw dust



granulates



MSW-plastics



SLF-plastics



PE+PS



Sewage Sludge



“Steam gasification at high temperature” with different bed material

feldspar



calcite



olivine



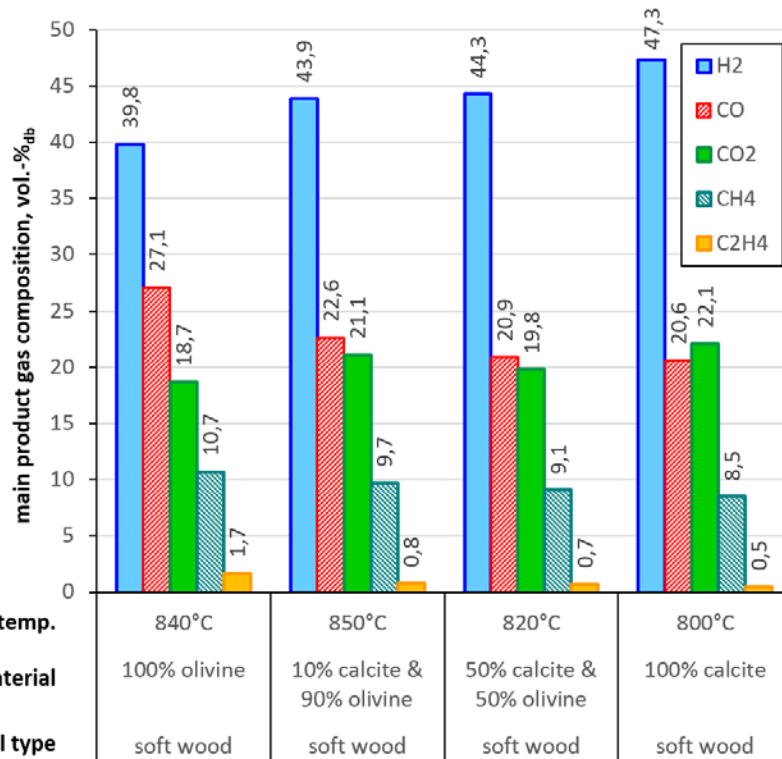
quarz



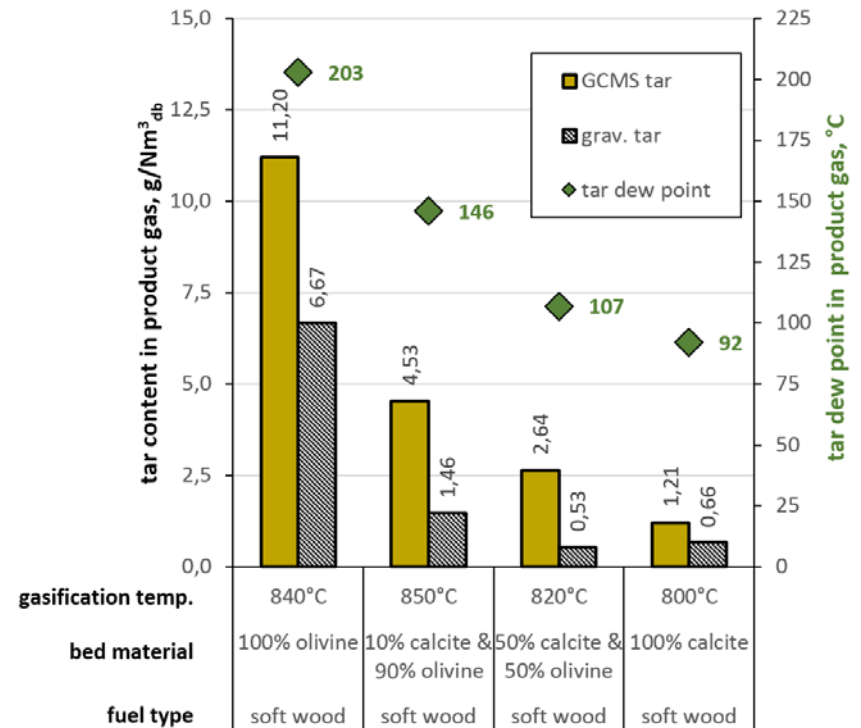
STEAM GASIFICATION

at temperatures $>750^{\circ}\text{C}$

Influence of different bed material mixtures:

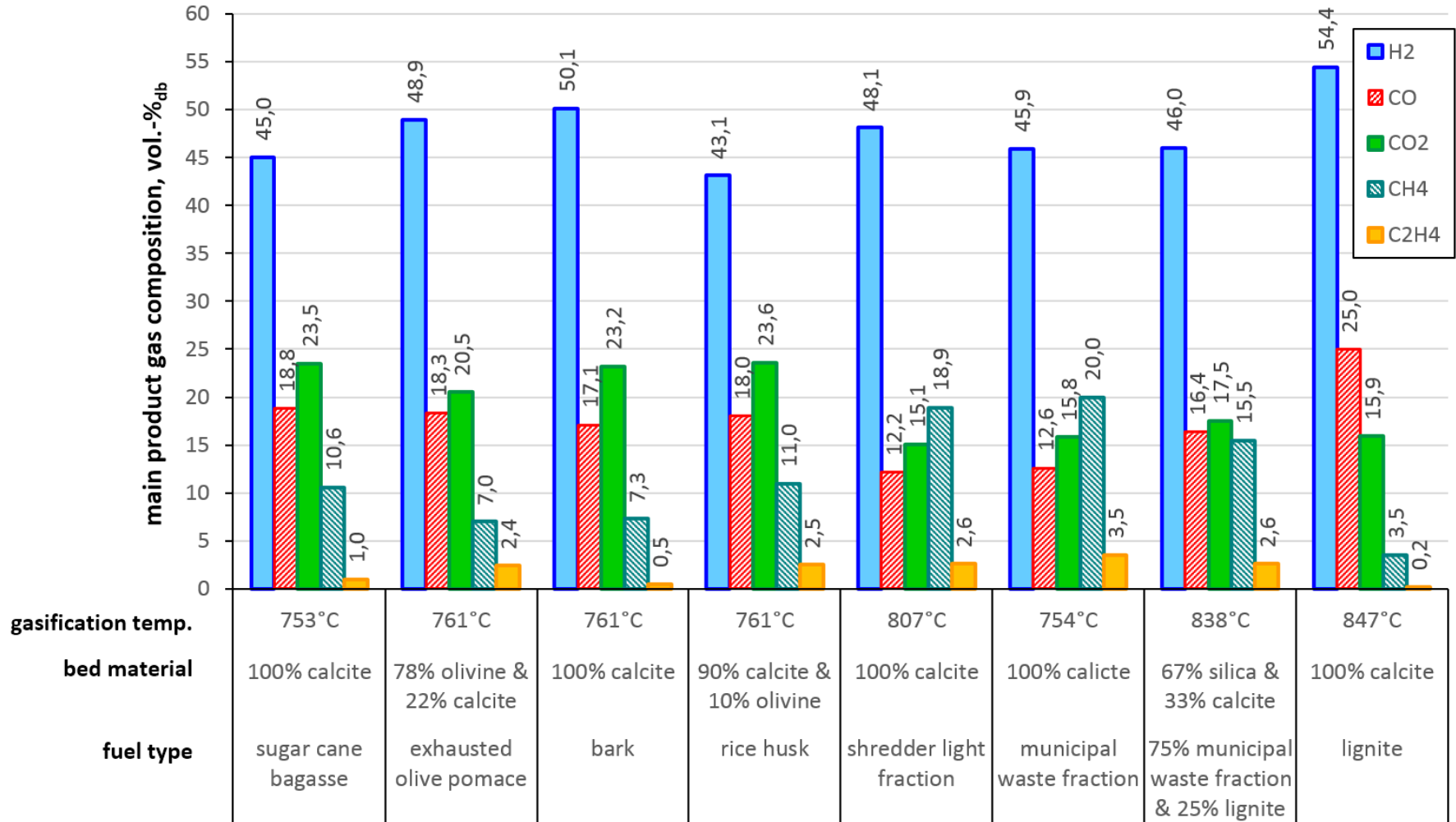


Main product gas components



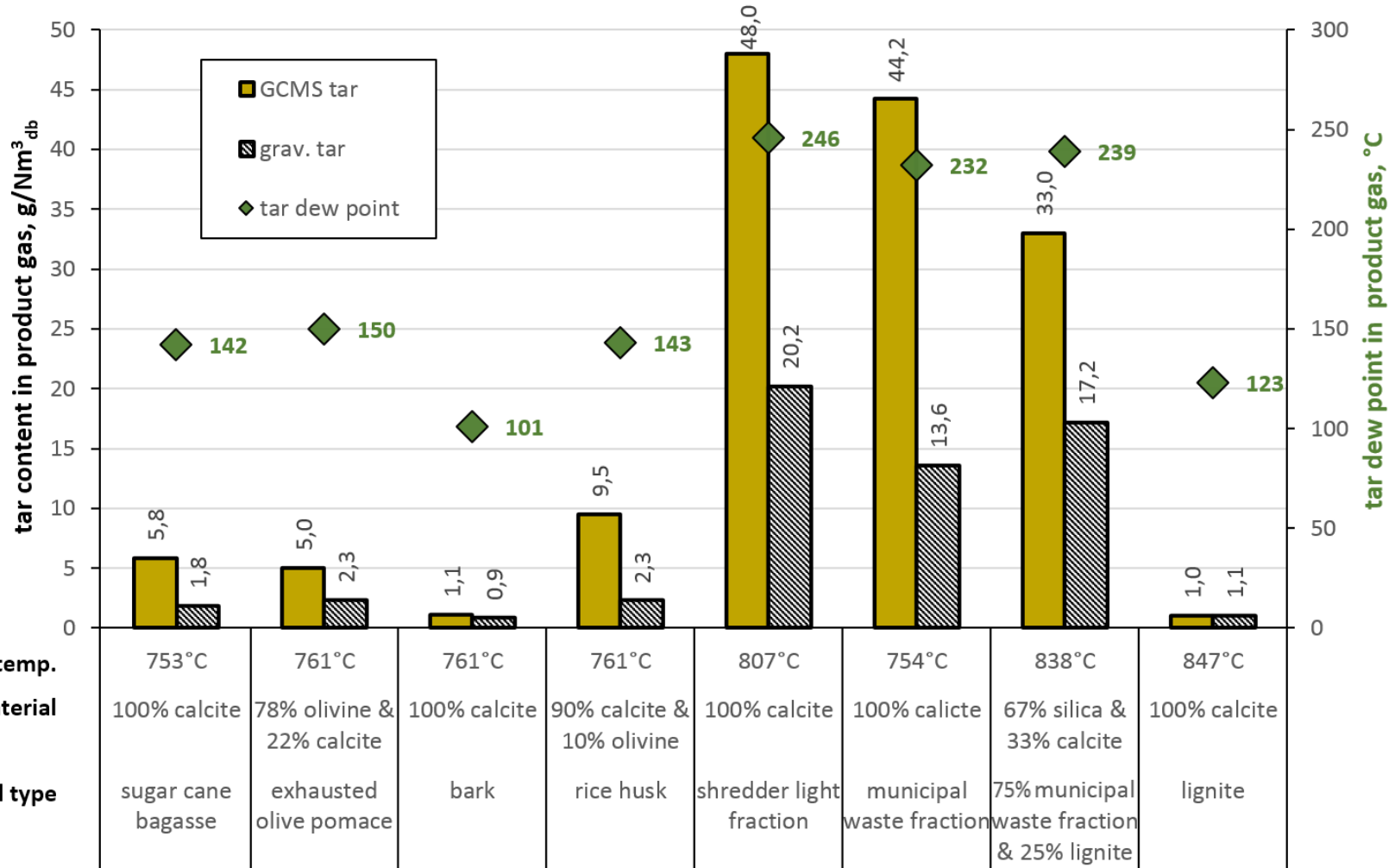
Tar content and dew point

Gasification of different fuels:



Main product gas components

Gasification of different fuels:

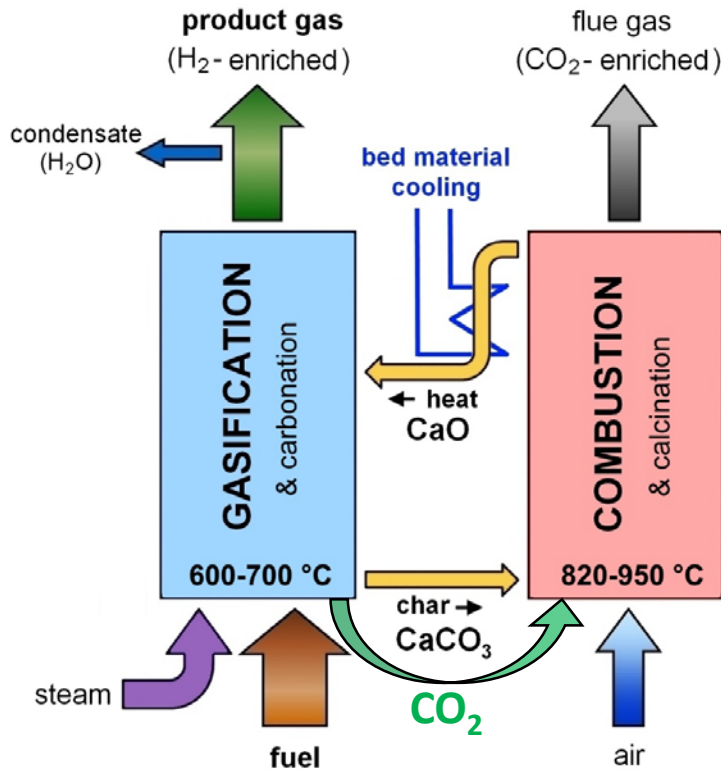


Tar content and dew point

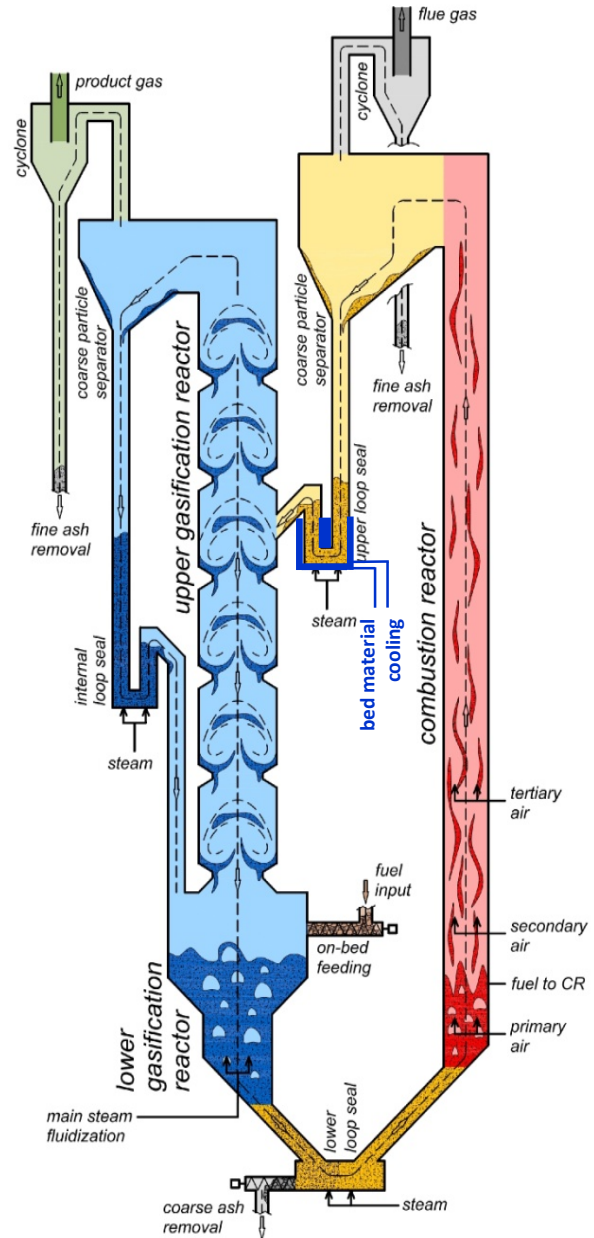
SORPTION ENHANCED REFORMING

at temperatures 620-680°C

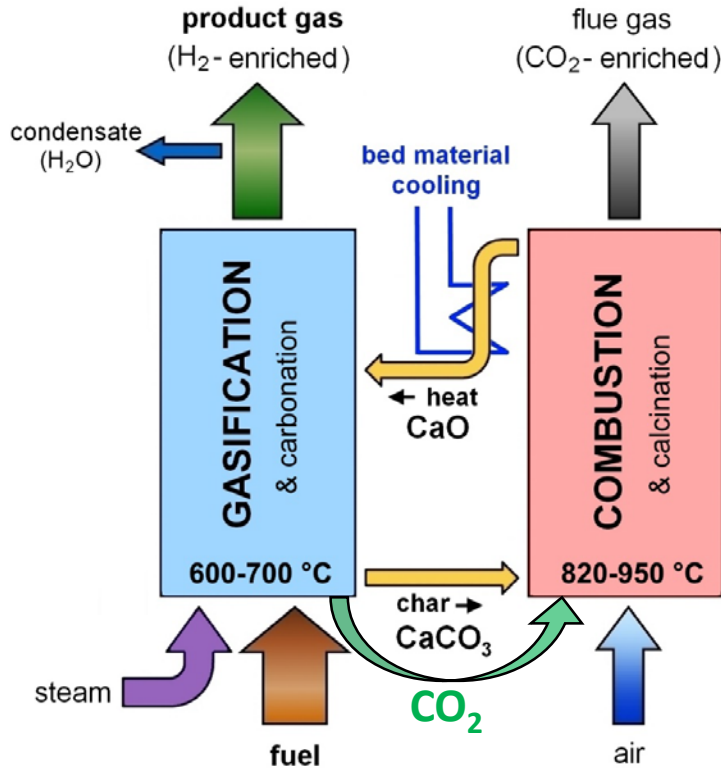
„Sorption Enhanced Reforming (SER)“ with Limestone/Calcite as Bed Material



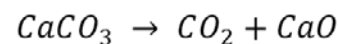
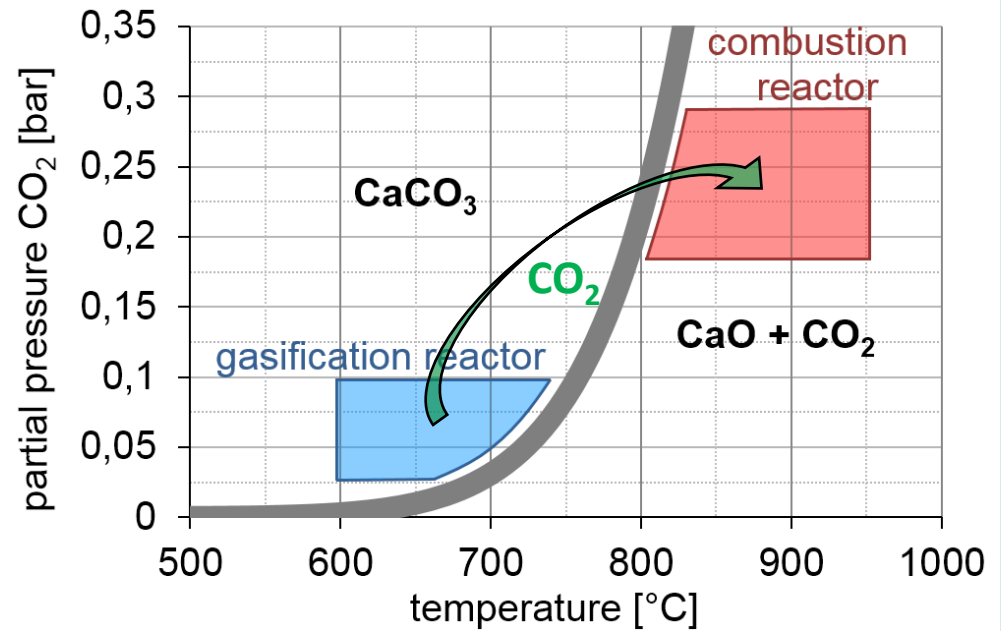
CaO / CaCO₃
as bed material:
heat and CO₂ carrier



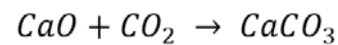
„Sorption Enhanced Reforming (SER)“ with Limestone/Calcite as Bed Material



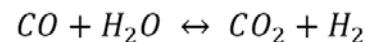
CaO / CaCO₃
as bed material:
heat and CO₂ carrier



$$\Delta H_R^{850} = +167 \text{ kJ/mol}$$

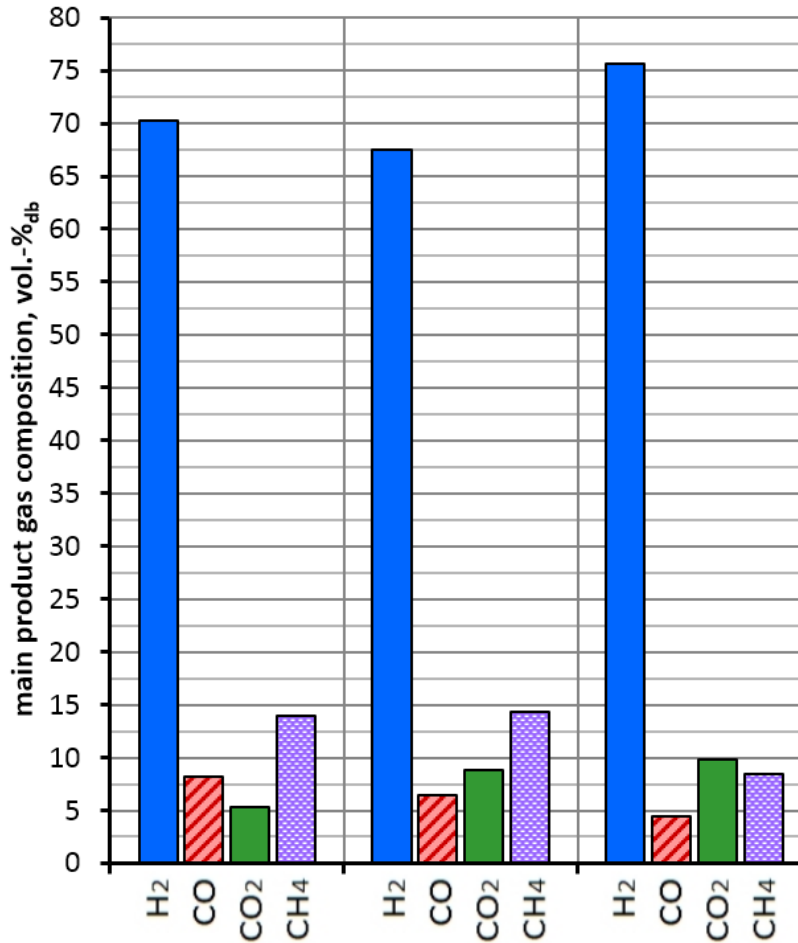
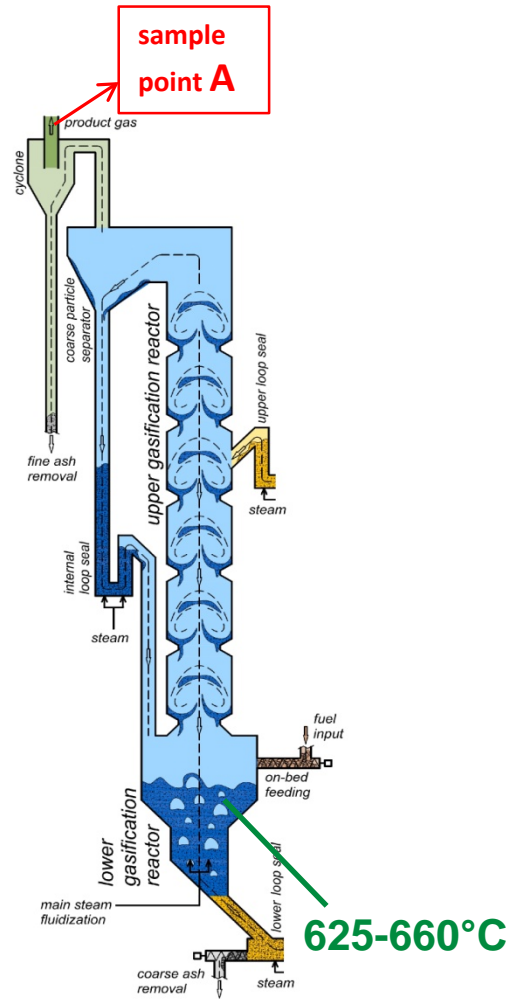


$$\Delta H_R^{650} = -170 \text{ kJ/mol}$$



$$\Delta H_R^{650} = -36 \text{ kJ/mol}$$

SER: Variation of Fuel Type



gasification temp. GR6

629°C

625°C

660°C

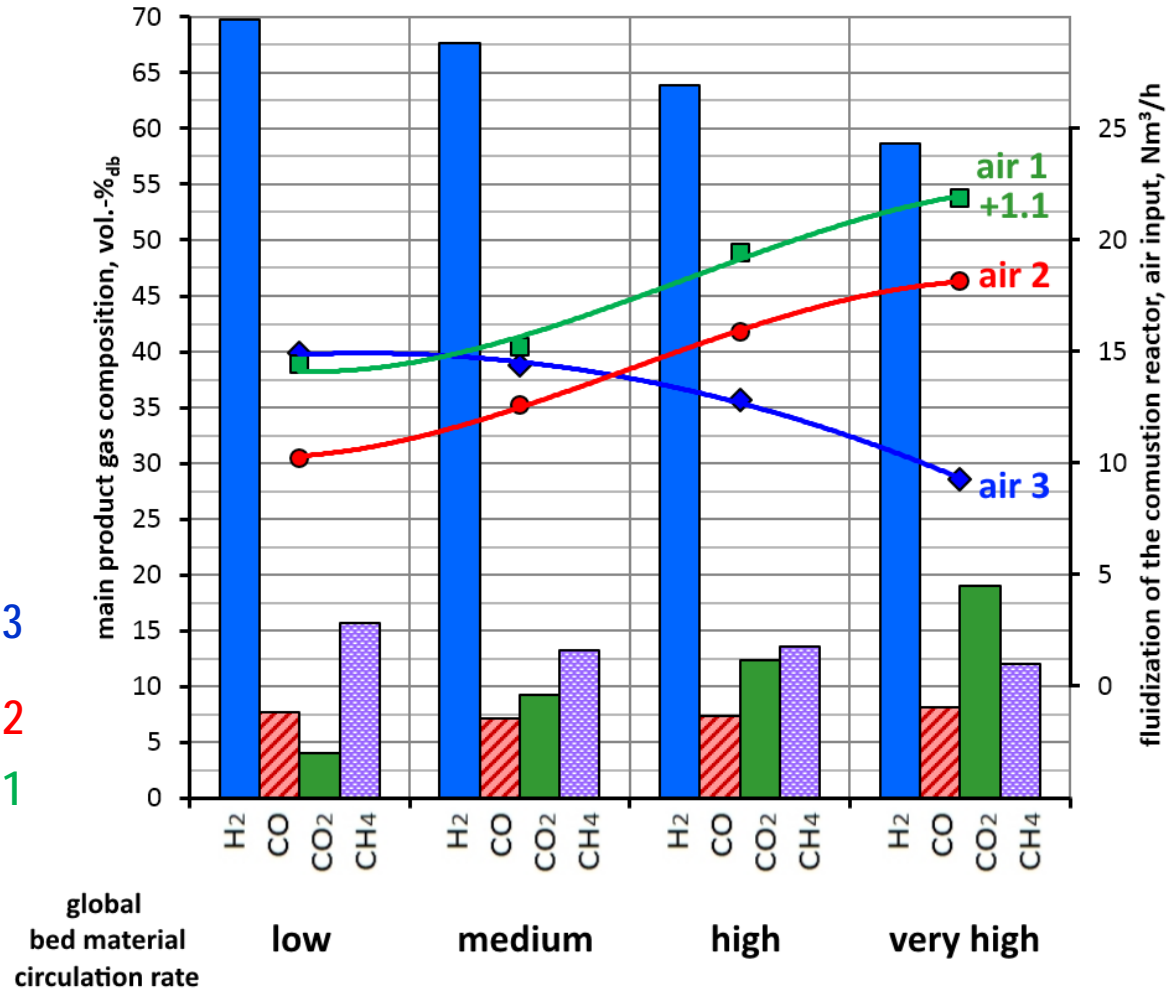
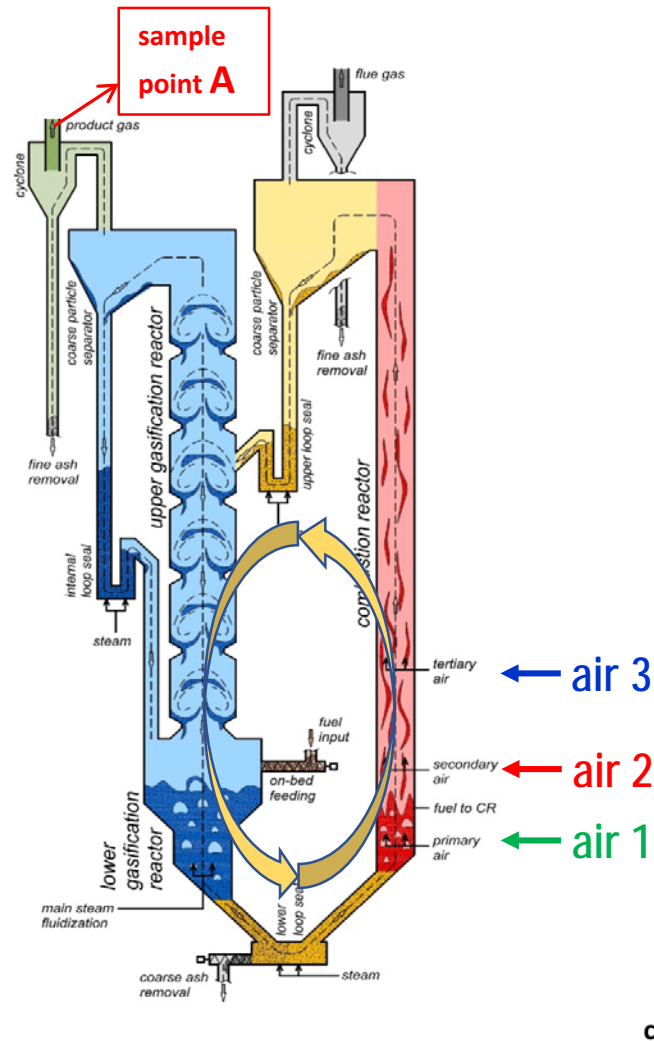
fuel type

soft wood

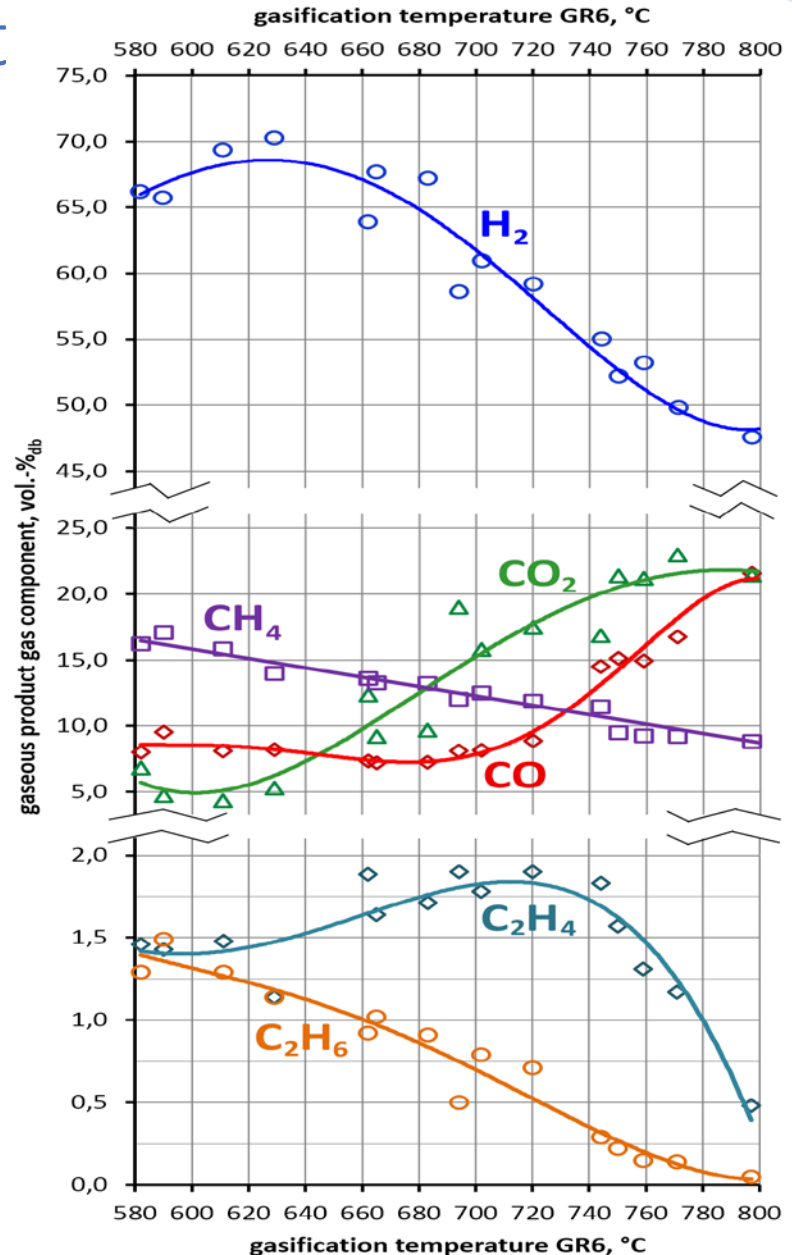
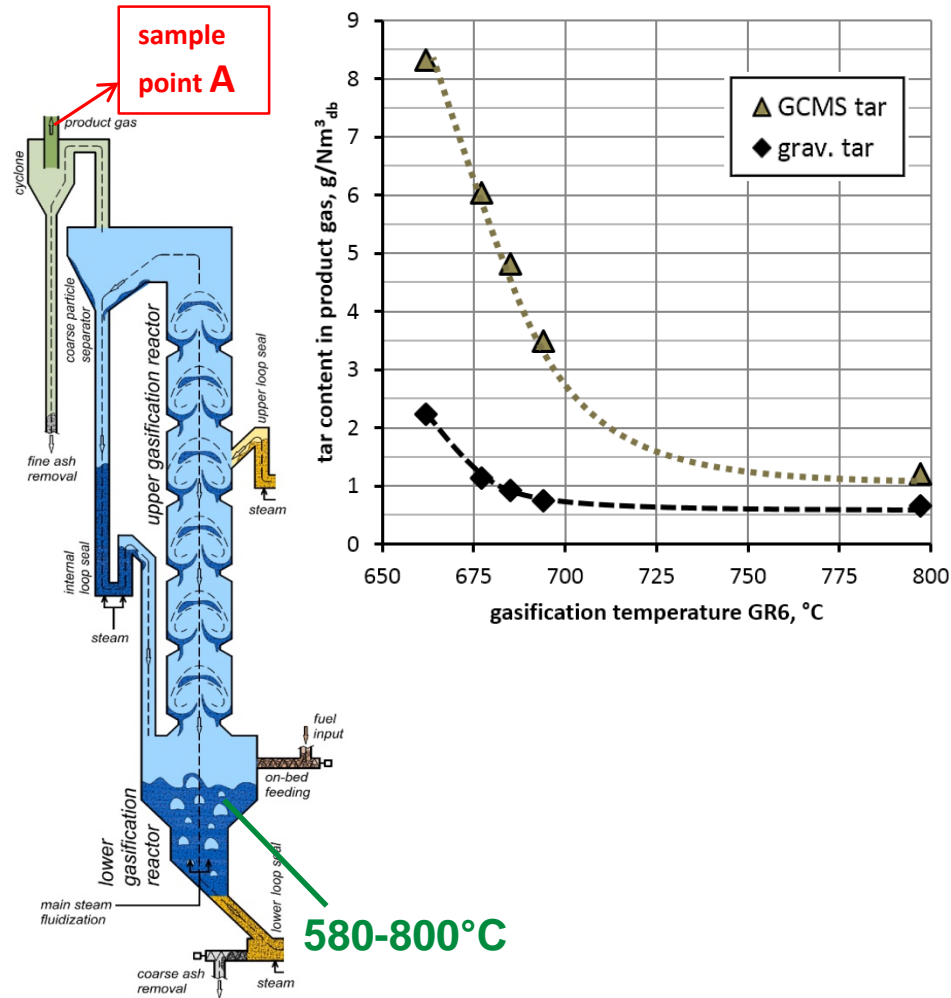
bark

lignite

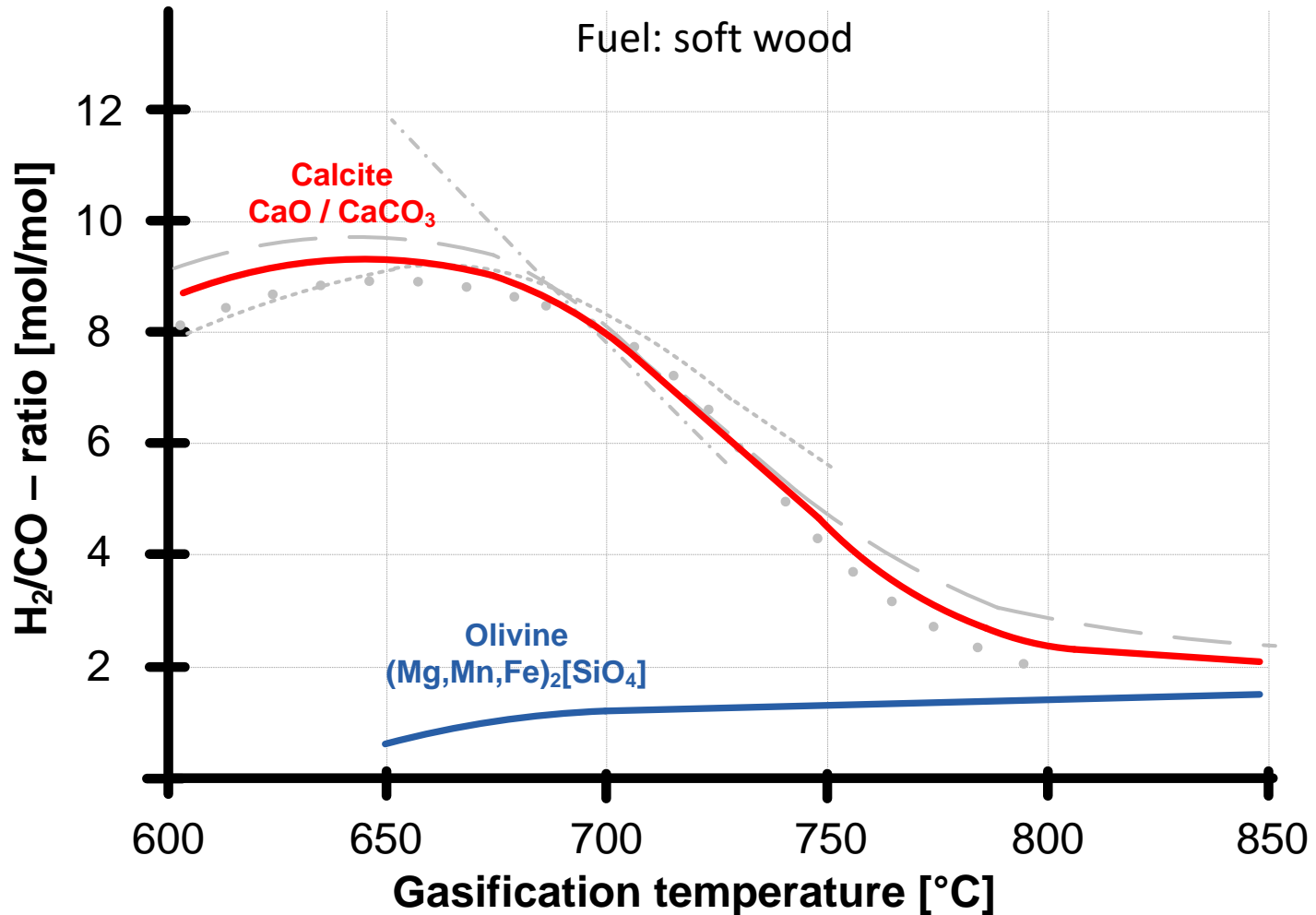
SER: Variation of Bed Material Circulation



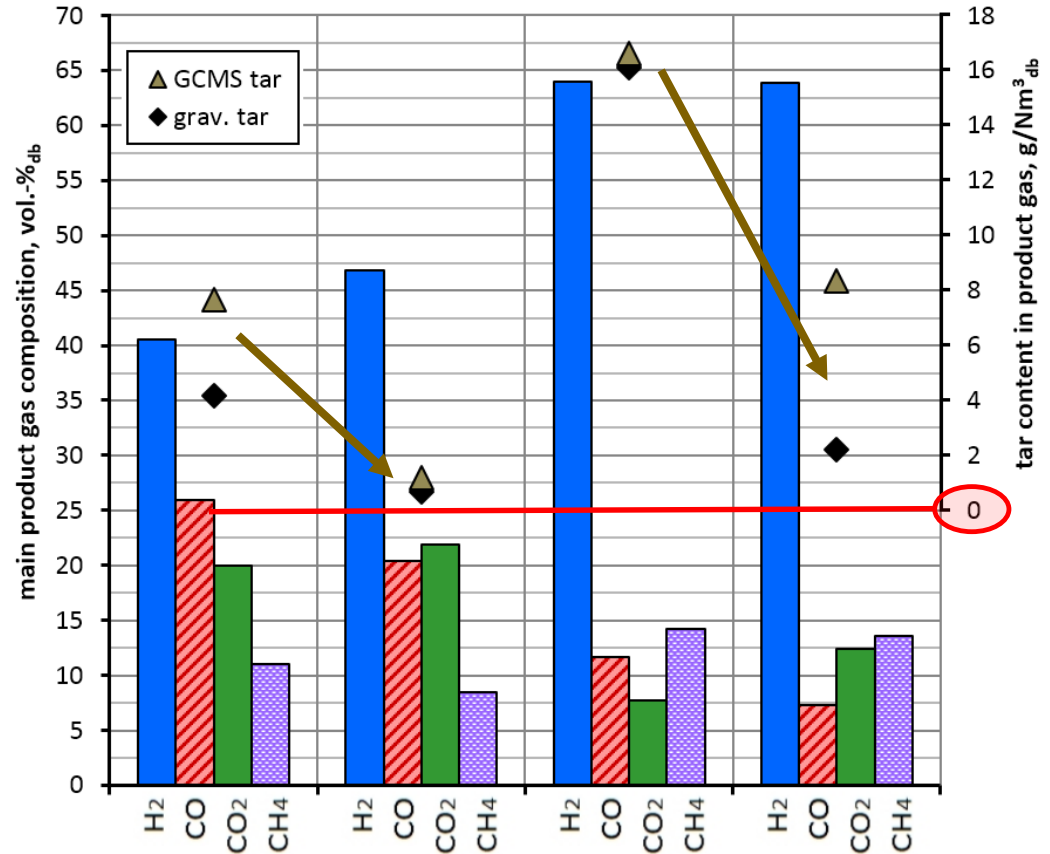
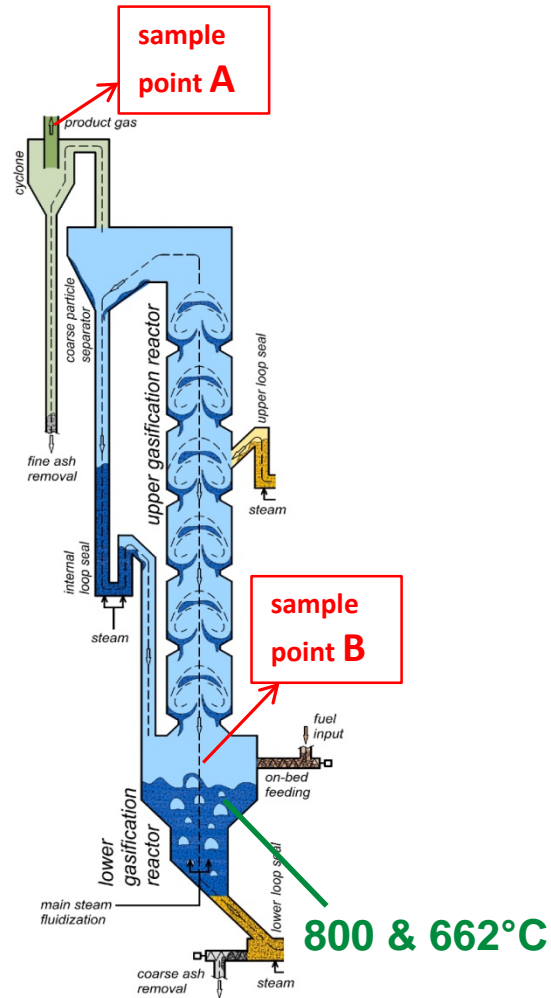
SER: Variation of temperat



Variation of the gasification temperature



Impact of Upper Gasification Reactor



sample point

B

A

B

A

gasification temp. GR6

800°C

662°C

dual fluidized bed process

conventional steam gasification

sorption enhanced reforming

Conclusion:

- Novel design: fuel and bed material flexible
- Low-cost fuels can be gasified
- Alternative, residual fuels increase requirements on the gas cleaning system significantly
- Hydrogen rich gas can be produced (SER)
- H₂/CO adjustment with the gasification process
- Novel separation system for soft bed materials

Outlook:

Research questions for the future:

- Impurities or valuable substances of different fuel types
- Where are the substances (product gas, fine ash, coarse ash, fly ash,...)
- Suitable gas cleaning processes

Thank you for your attention

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FFG

voestalpine

ONE STEP AHEAD.

Sources

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