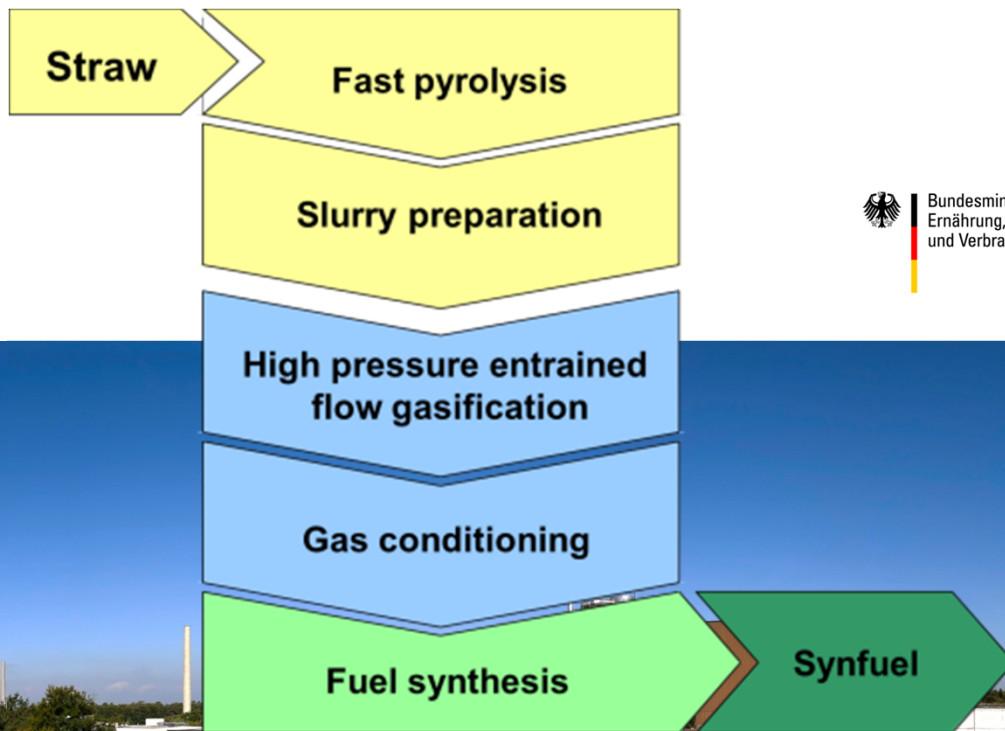


BtL – the bioliq[®] process

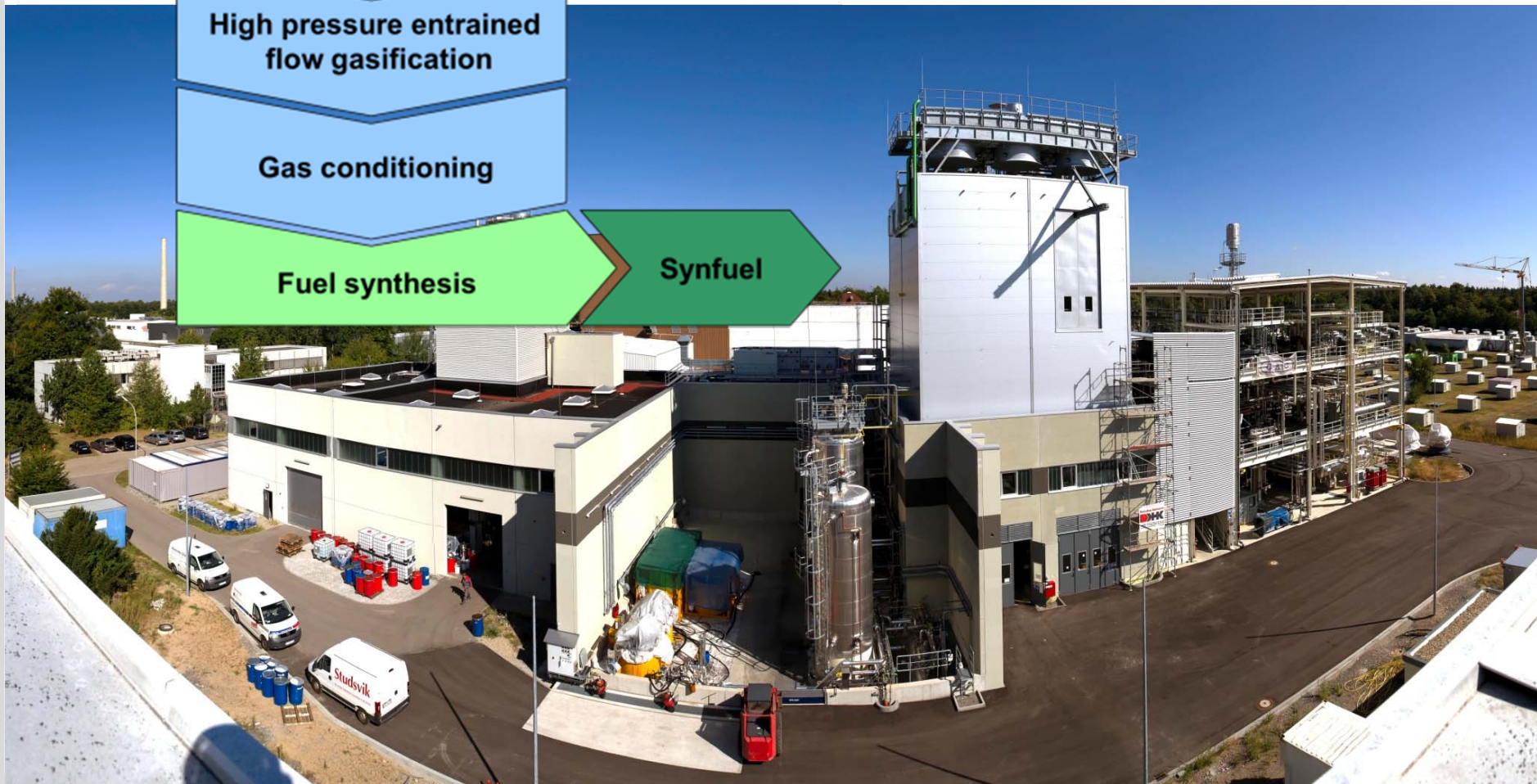
Thomas Kolb, Mark Eberhard

Engler-Bunte-Institut, Chemische Energieträger – Brennstofftechnologie, EBI ceb
Institut für Technische Chemie, Vergasungstechnologie, ITC vgt
DVGW Forschungsstelle am EBI, Gastechologie, DVGW gt





Bundesministerium für Ernährung, Landwirtschaft und Verbraucherschutz



The bioliq[®]-Process

Specific energy content [GJ/m³]

Regionally distributed biomass

Transportation distance

Straw 1,5



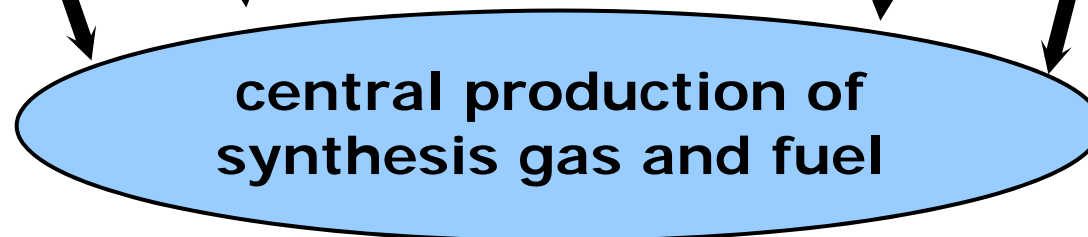
25 km

Slurry 15-25

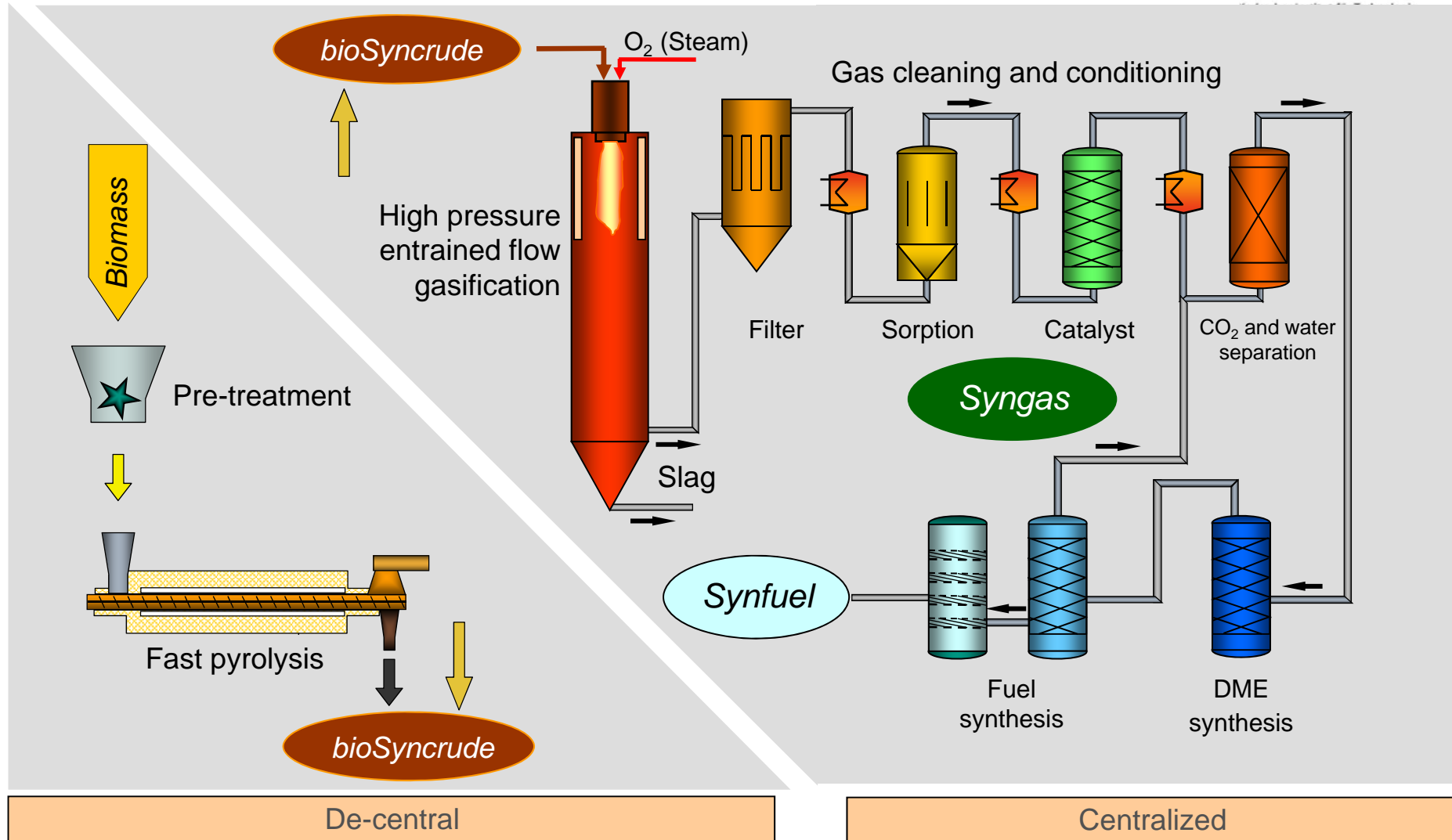


250 km

Fuel 36

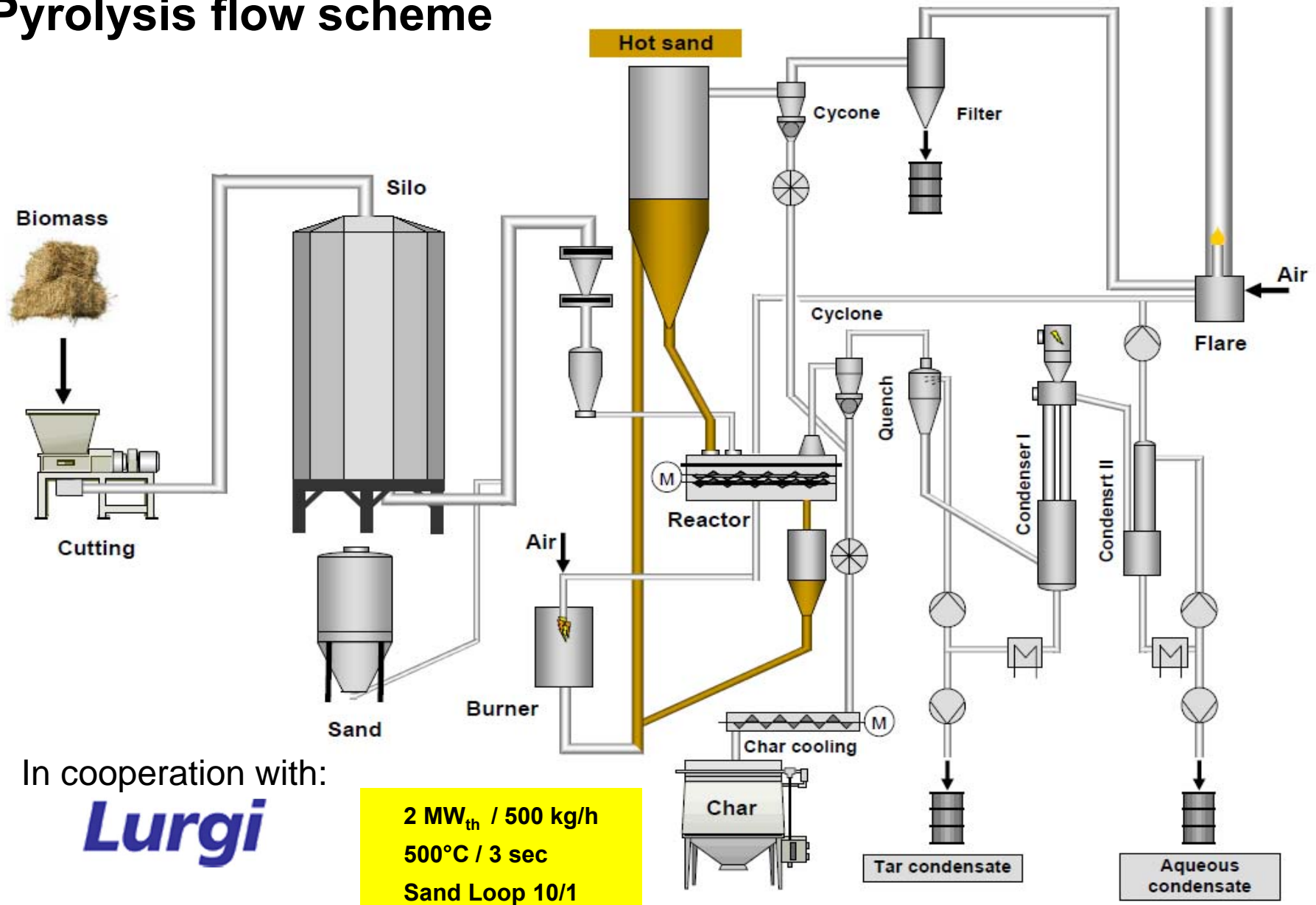


bioliq[®] process scheme



Source: Presentation of Dr. Dahmen, IKFT

Pyrolysis flow scheme



Fast Pyrolysis Pilot Plant

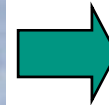
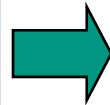
Biomass preparation



Fast pyrolysis



Pyrolysis product recovery

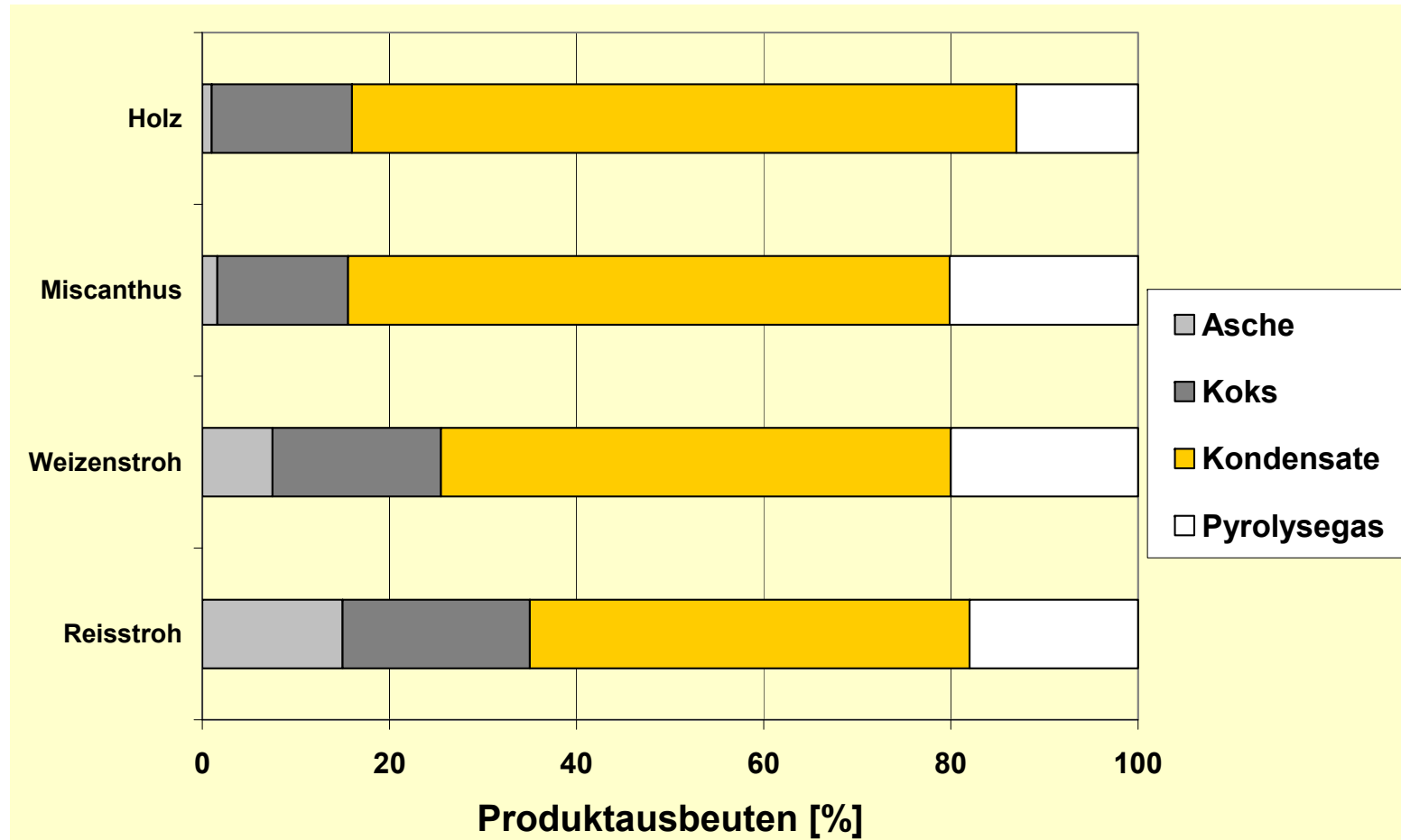


Feed stock storage



Biosyncrude preparation

Fast Pyrolysis of different Feed Stock /Lab Scale

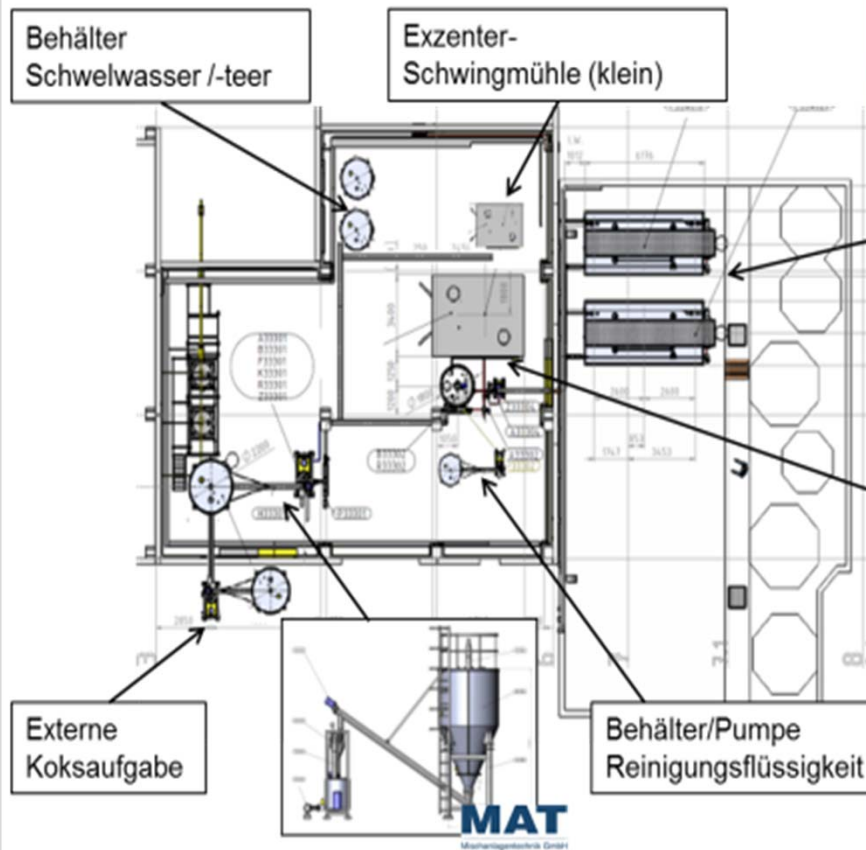


From lab scale experiment



BioSyncrude

Production / Storage



Slurry Specification

- 2 fractions organic & water
- solids up to 40 wt. %
- ash up to 10 wt. %
- organic acids (e.g. formic / acetic acid)
- alcohol (e.g. methanol)
- chloride up to 1 wt. %

- dynamic viscosity $50 \text{ mPas} < \eta < 5000 \text{ mPas}$
- density $1000 \text{ kg/m}^3 < \rho < 1500 \text{ kg/m}^3$
- Particle size $90\% < 100 \mu\text{m}$
- pH $2 < \text{pH} < 7$

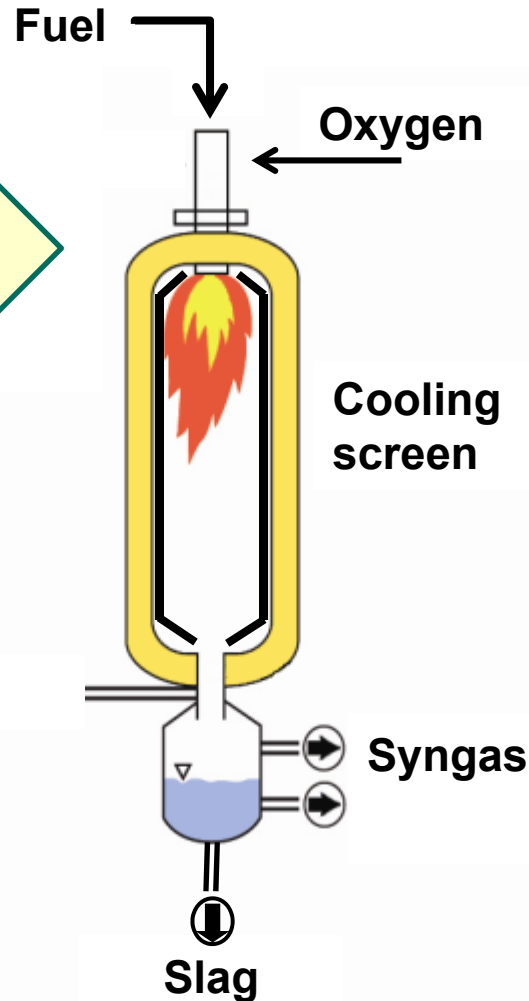


**Organic condensate
30% solids**

High Pressure Entrained Flow Gasification

➔ Fuel/ Load / Product – Flexibility

- Coal
- Residues
- **Biomass**
- Waste



- Flexibility
- Load / Product
- Efficiency

- heterogeneous
- high ash content
- flexibility

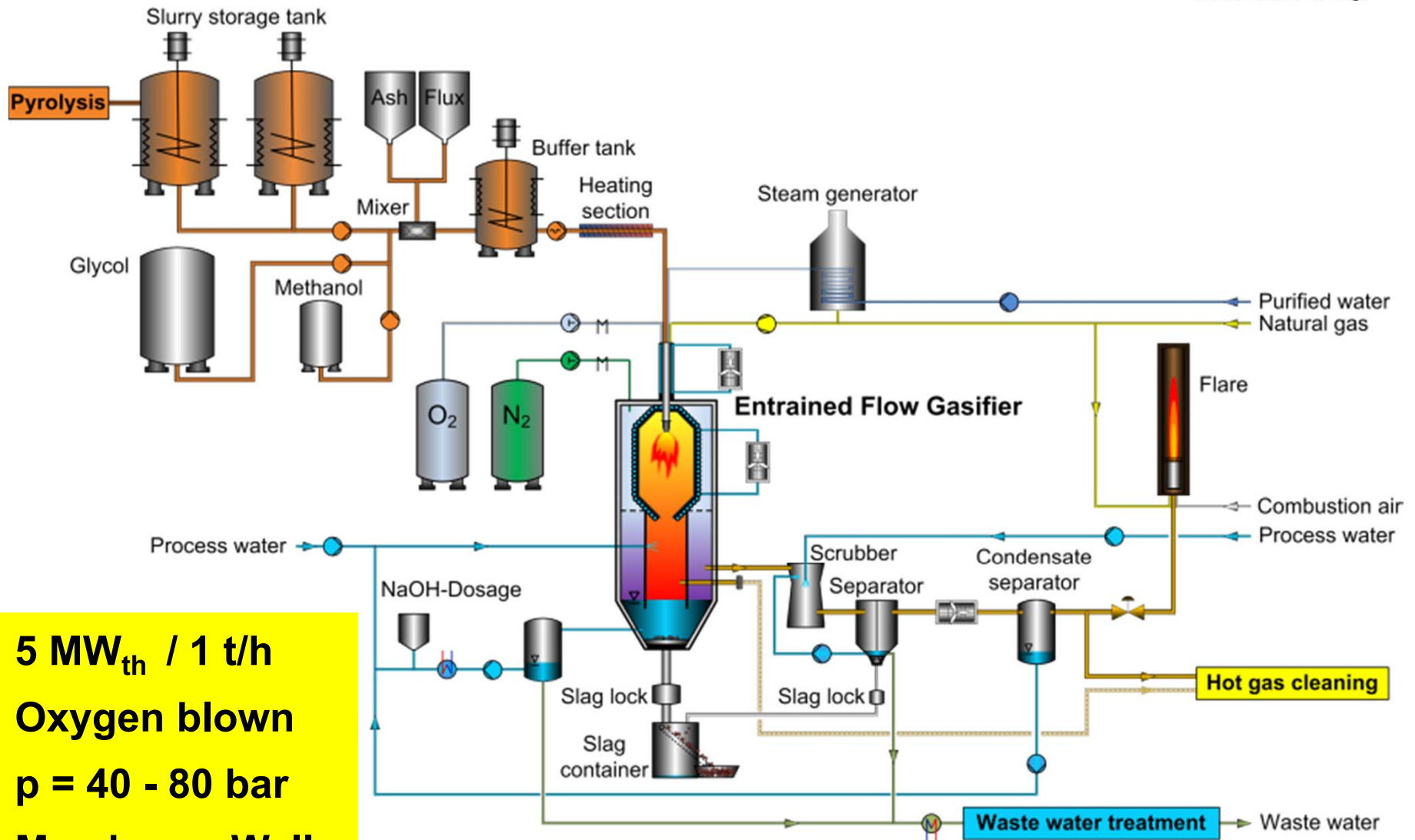
- Fuels, BtL
- Chemicals
- Hydrogen, H₂
- Electricity / Heat, IGCC

bioliq[®] Entrained Flow Gasifier

- Confirmation of Funding FNR / Sept. 2008
- Contract signed KIT-Lurgi / Dec. 2008
- Mechanical Completion / Oct. 2011
- Completion of Commissioning / July 2012
- First Flame / Aug. 2012
- Stable Operation with Liquid Fuel 80 bar / Dec. 2012
- Performance Test with Model Slurry / Jan 2013
- First Test Run July 2013



bioliq[®] Entrained Flow Gasifier



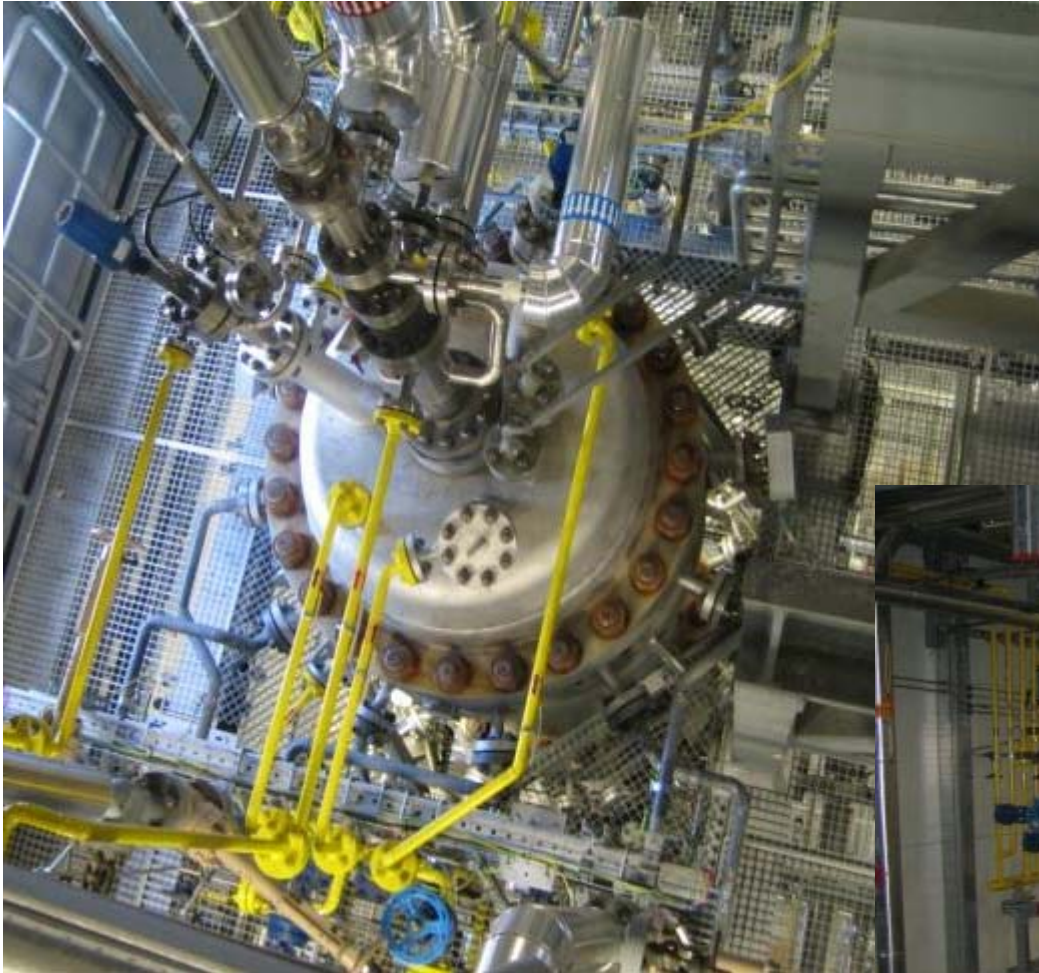
5 MW_{th} / 1 t/h
Oxygen blown
p = 40 - 80 bar
Membrane Wall

bioliq[®] II

Tankfarm & Slurry Pump



bioliq® EFG



Gasifier Top
40bar configuration

Quench upper
section

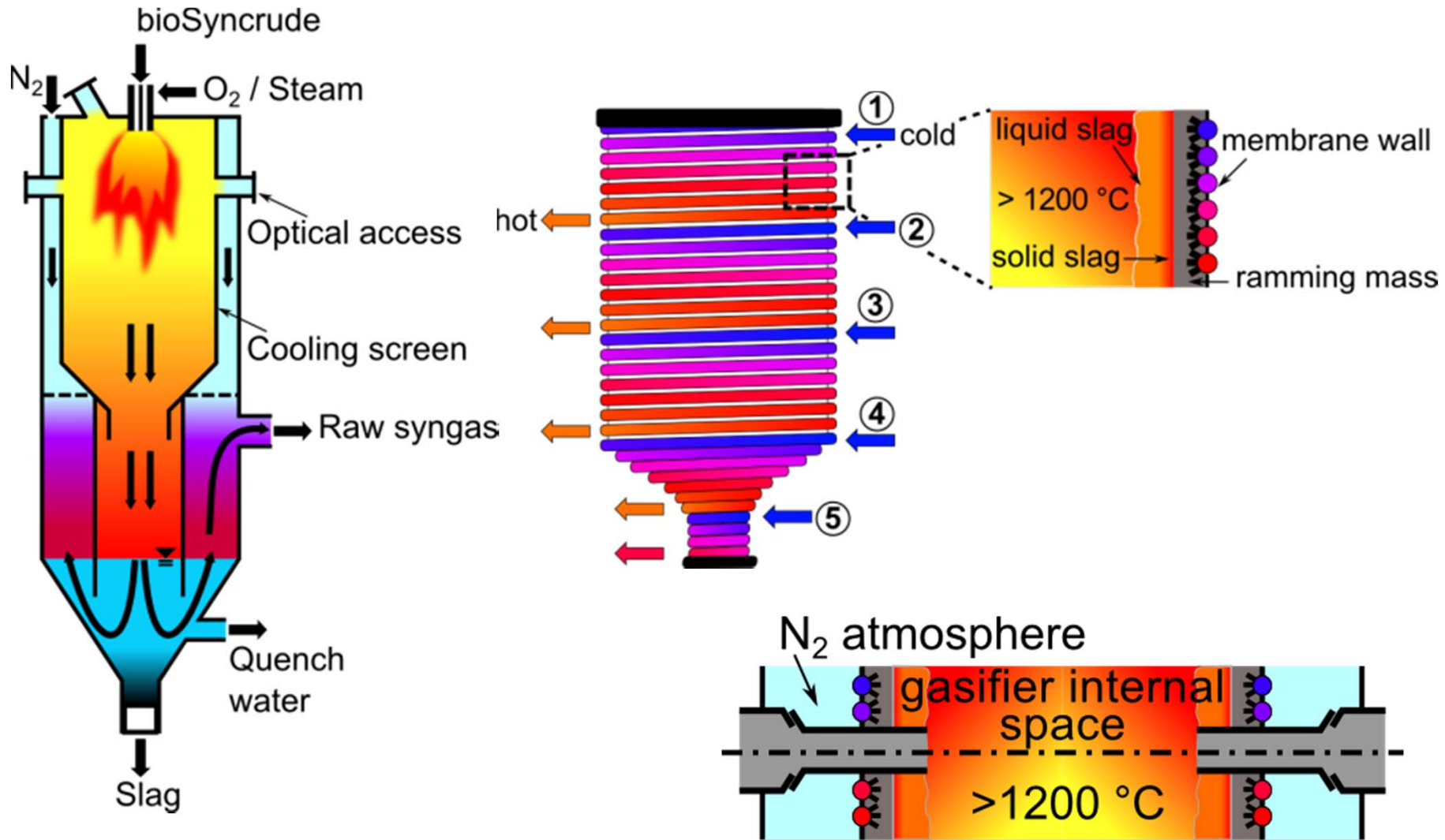


bioliq® II

Quench & Slag Handling



bioliq[®] Gasifier → Prozess Optimization



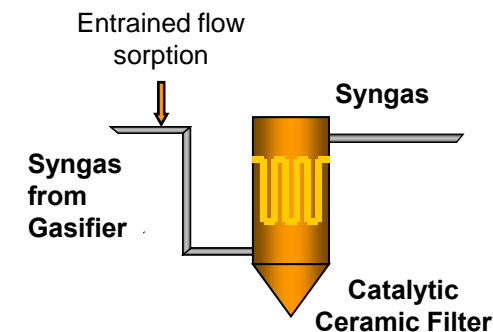
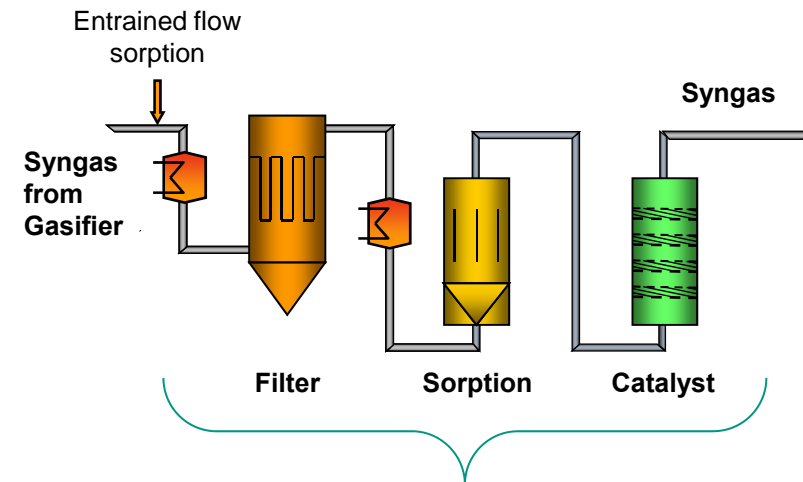
High Temperature - High Pressure (HTHP) Syngas Cleaning

- Compact horizontal ceramic filter for particle removal with CPP recleaning
- Dry sorption of sour gases (HCl, H₂S) and alkalines
- Catalytic conversion of organics and N-species (HCN, NH₃)
- CO₂ separation (optional)
- 700 m³/h STP synthesis gas (40 m³/h at 80 bar, 800 °C)

⇒ Energy Savings ca. 10% compared to state-of-the-art gas cleaning

⇒ Process Integration

⇒ Chemical Quench



bioliq[®] HTHP Syngas Cleaning



Nov 2013: End of commissioning phase

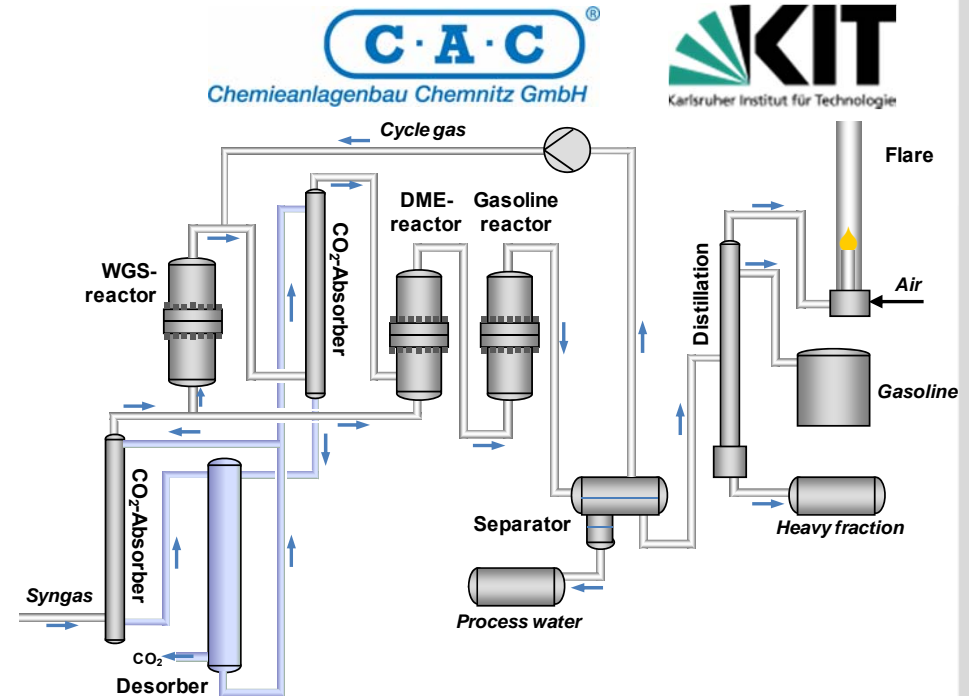
DME and Fuel Synthesis

DME-synthesis

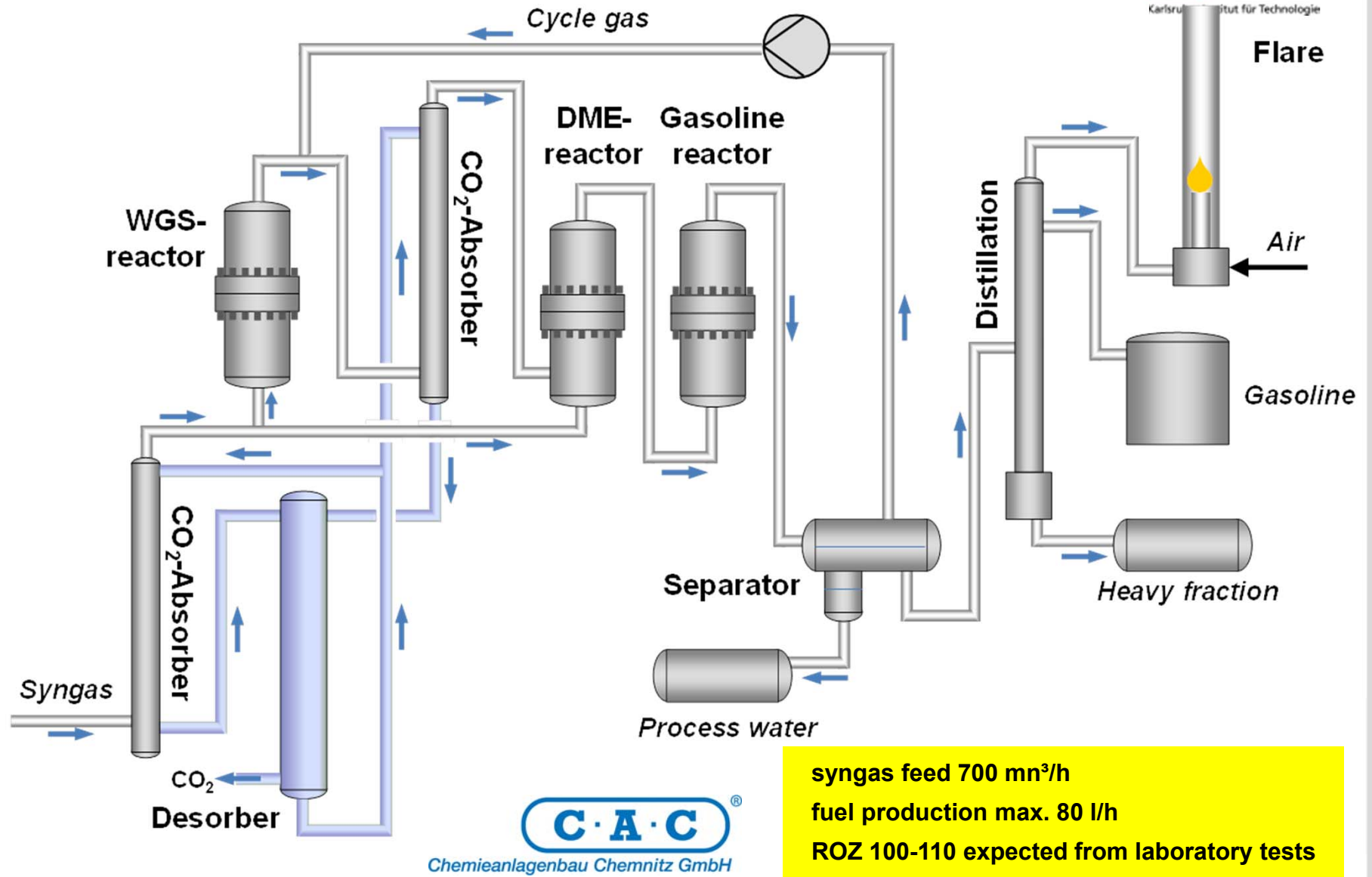
- One step DME synthesis
- Innovative isothermal reactor
- Temp. 250 °C, pressure 60 bar

DtG-synthesis

- Zeolithe catalyzed dehydratization, oligomerization and isomerization
- Temp. 350 - 450 °C, pressure 25 bar
- Recycling of unconverted gas
- Gasoline stabilization



Flow sheet Synthesis



Synthesis Pilot Plant

Performance Test June 2013
Acceptance July 2013



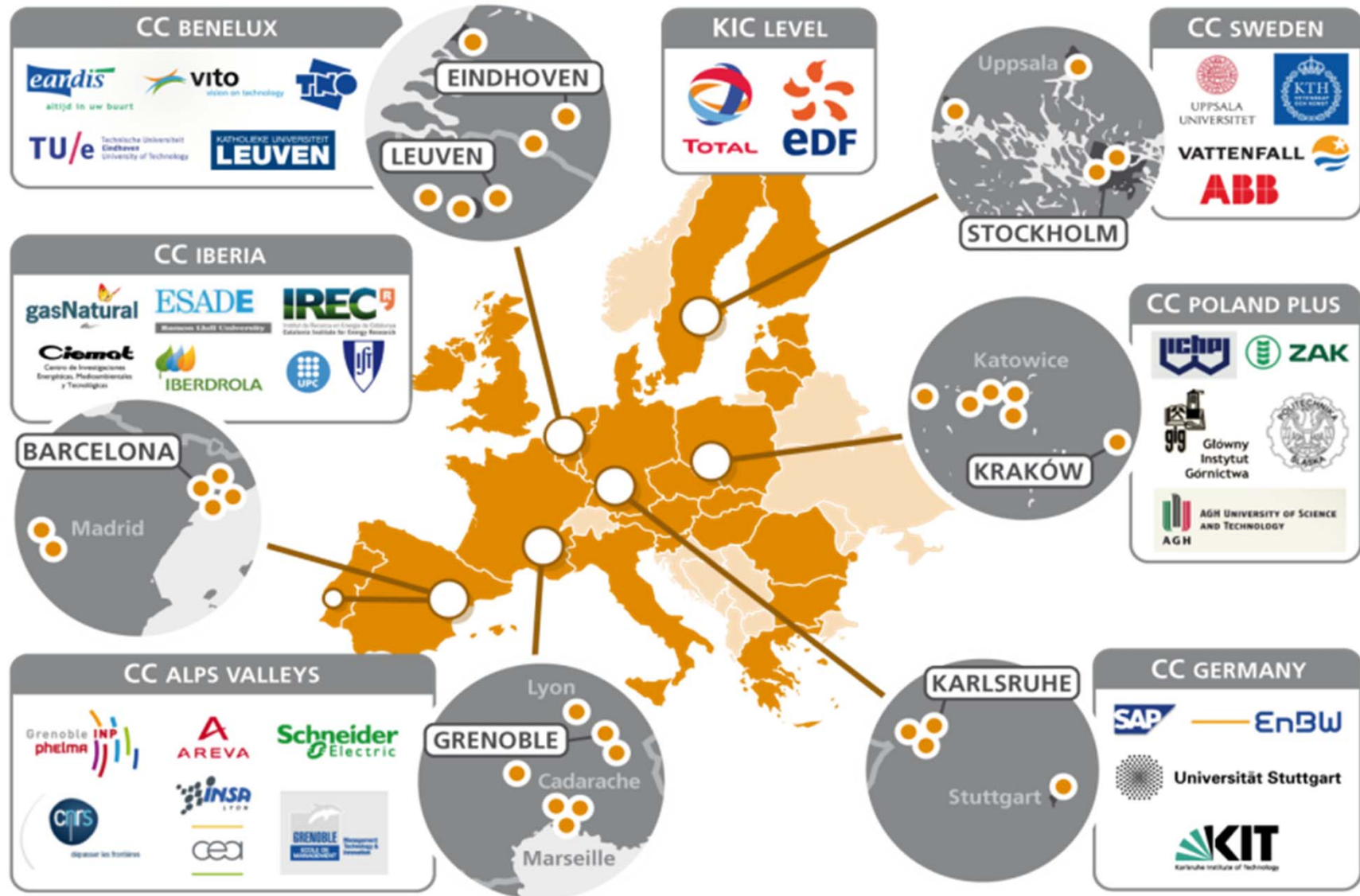
Helmholtz Virtual Institute for Gasification Technology

Towards Sustainable Energy Systems

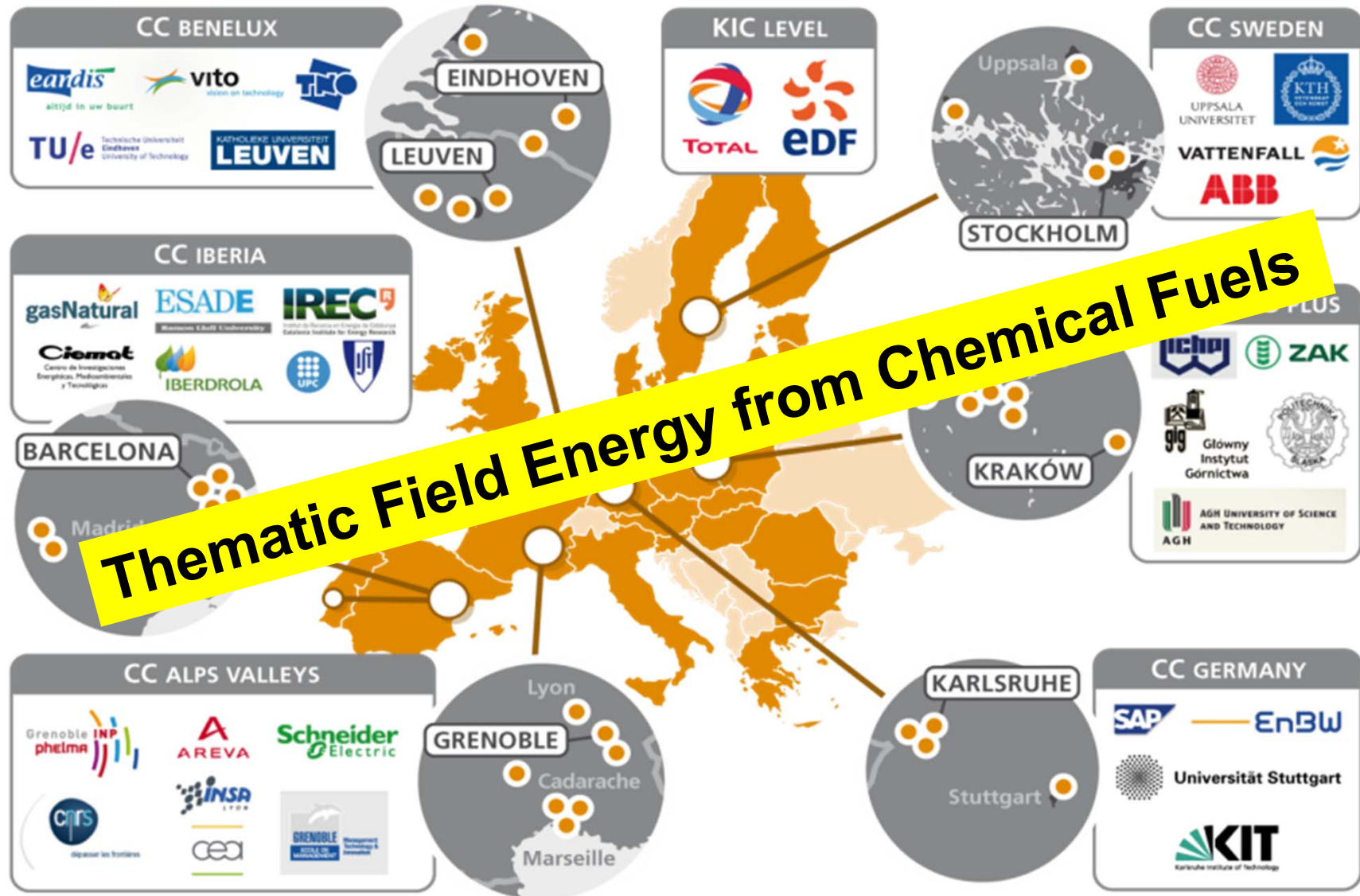
Thomas Kolb, Manfred Aigner, Reinhold Kneer, Michael Müller, Roman Weber



KIC InnoEnergy – Partners from 6 co-locations



KIC InnoEnergy – Partners from 6 co-locations





Lurgi



Chemieanlagenbau Chemnitz GmbH

