



Dual fluidized bed gasification for CHP and production of advanced biofuels

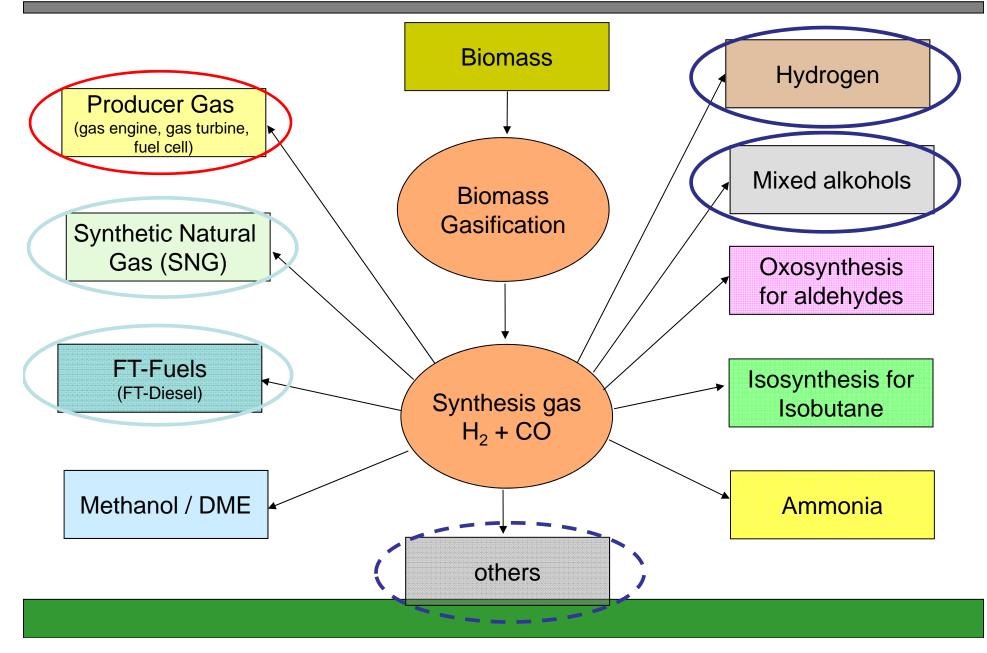
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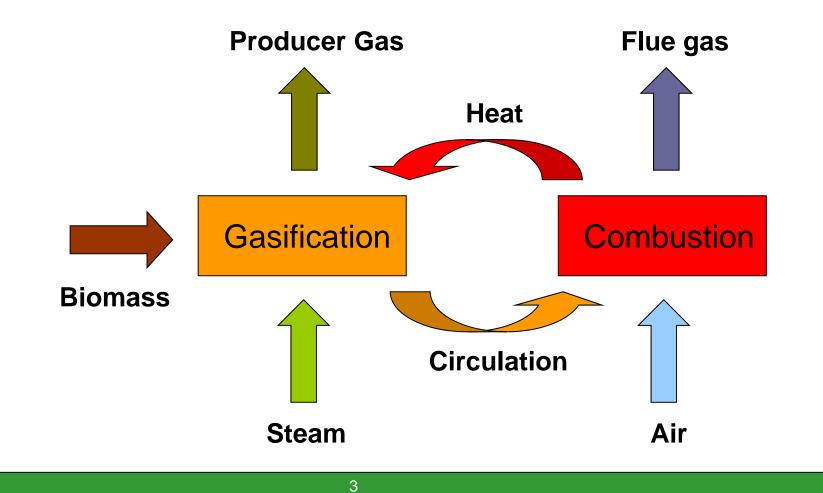
IEA Bioenergy Task33 Thermal Gasification of Biomass







Gasification Concept of Dual Fluid (FICFB)





Location	Usage / Product	Fuel / Product MW, MW	Start up	Supplier	Status
Güssing, AT	Gas engine	8.0 _{fuel} / 2.0 _{el}	2002	AE&E, Repotec	Operational
Oberwart, AT	Gas engine / ORC	8.5 _{fuel} / 2.8 _{el}	2008	Ortner Anlagenbau	Operational
Villach, AT	Gas engine	15 _{fuel} / 3.7 _{el}	2010	Ortner Anlagenbau	On hold
Senden/Ulm DE	Gas engine / ORC	14.7 _{fuel} / 5 _{el}	2011	Repotec	Operational
Burgeis, IT	Gas engine	2 _{fuel} / 0.5 _{el}	2012	Repotec	Commissioning
Göteborg, Sweden	BioSNG	32 _{fuel} /20 _{BioSNG}	2013	Metso/ Repotec	Commissioning



Biomasses tested in the pilot scale FICFB gasifier

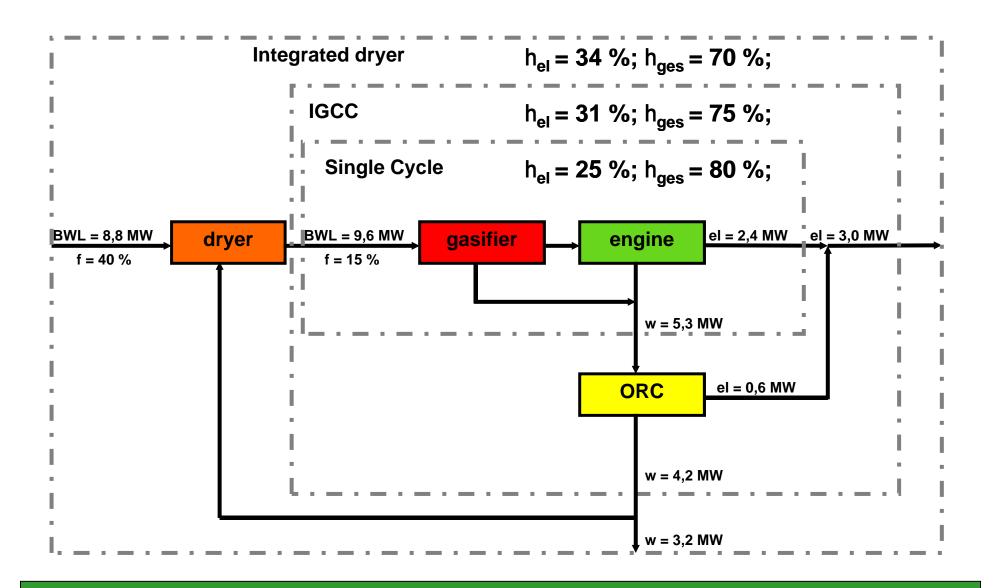
- Wood chips
- Wood pellets
- Saw dust (particle size)
- Coal (fixed carbon)

- Sewage sludge pellets (ash content)
- Animal residue (impurities)
- Straw (ash melting)
- Willow (energy crop)

All fuels can be used, if the ash melting point is above 1000°C as pure fuel and fixed carbon below 25%. Fuels with lower ash melting point or higher fixed carbon have to be used as mixture (e.g. 15% straw works well)

Case Study on CHP













BioH2-4Refineries

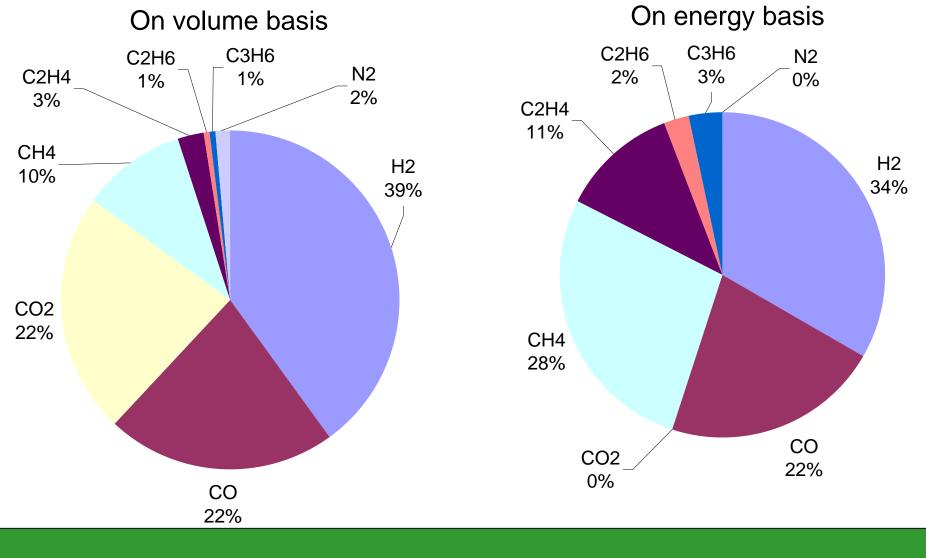
Economic evaluation of production of hydrogen for a refinery

- Coordination by OMV
- 50 MW fuel plant to replace fossil hydrogen
- Evaluation of the biomass resources available for such a plant
- Basic engineering of the gasifier as well as of all other sub units, including pipelines, utility systems, logistic needs
- Optimal use of by-products
- Economic evaluation





Gas composition at CHP Güssing







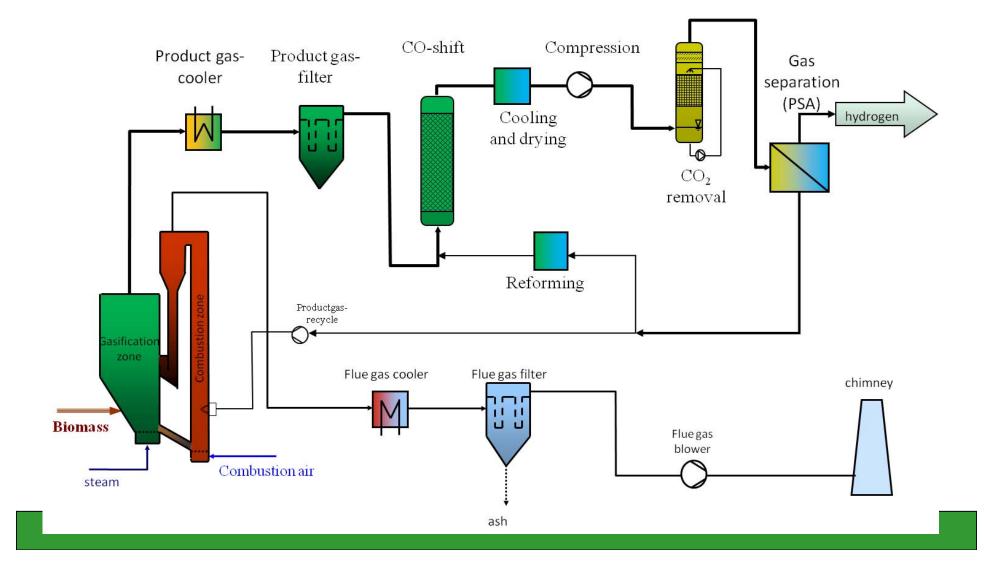
Options for gas conversions

- CO-shift
- Conversion of hydrocarbons
 - Reforming to H_2 and CO and recycle
 - Conversion to SNG
 - Conversion to electricity and heat
- Mass and Energy balances for all 3 cases were calculated
- Economics show, that reforming gives the highest overall value (at the frame conditions in Austria)





Simplified flow chart







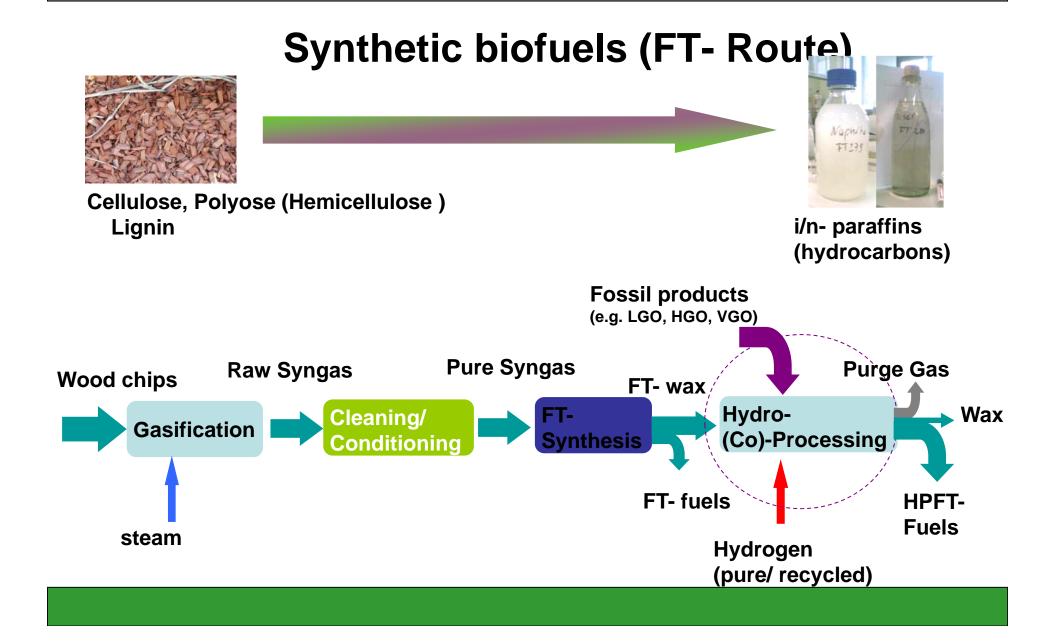
- Applied for NER300
- Technical diligence was good
- Economics due to high biomass price (110 €/t_{dry}) were the main reason to be on the 3rd place
- Project is on hold, but pilot plant is realised as slip stream in Güssing
- Future applications are evaluated together with gas industry





BIOMASS-TO-FISCHER-TROPSCH

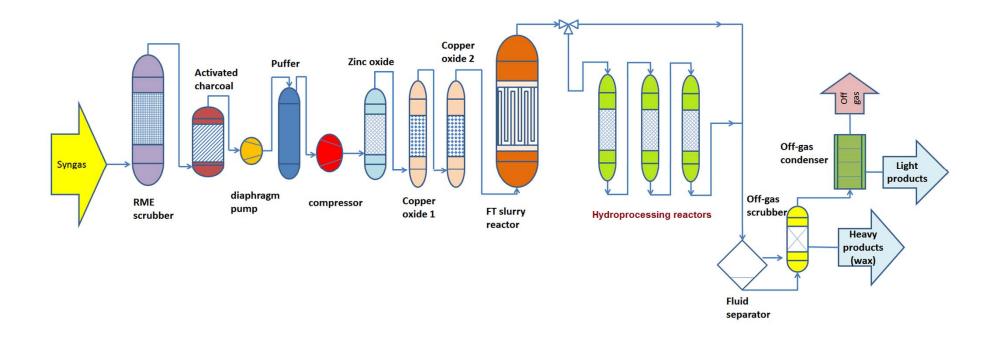






FT lab scale plant

bioenergy2020+



5-10kg/day of FT raw product

Slurry reactor, because of excellent heat transfer and easy scaling up

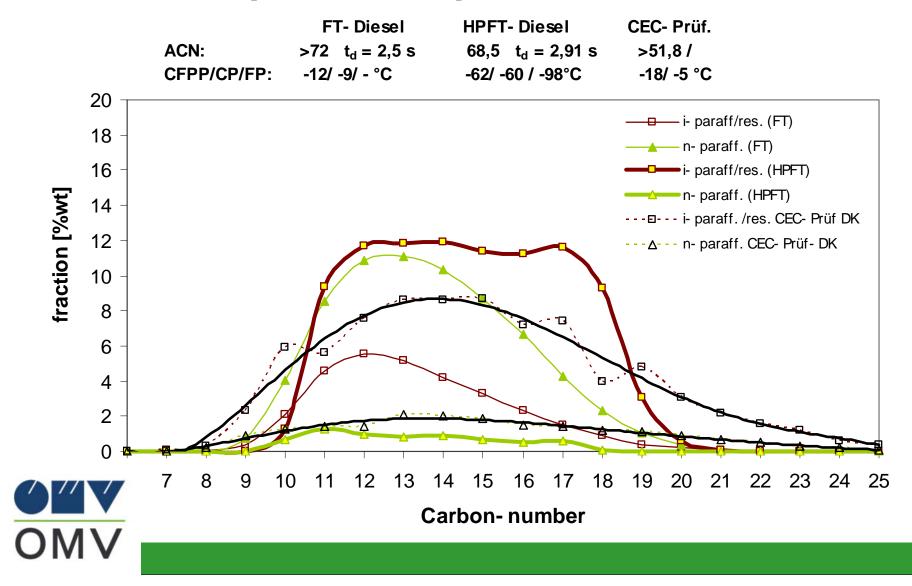
Gas treatment removes Sulphur to below 10ppb

Fully automatic





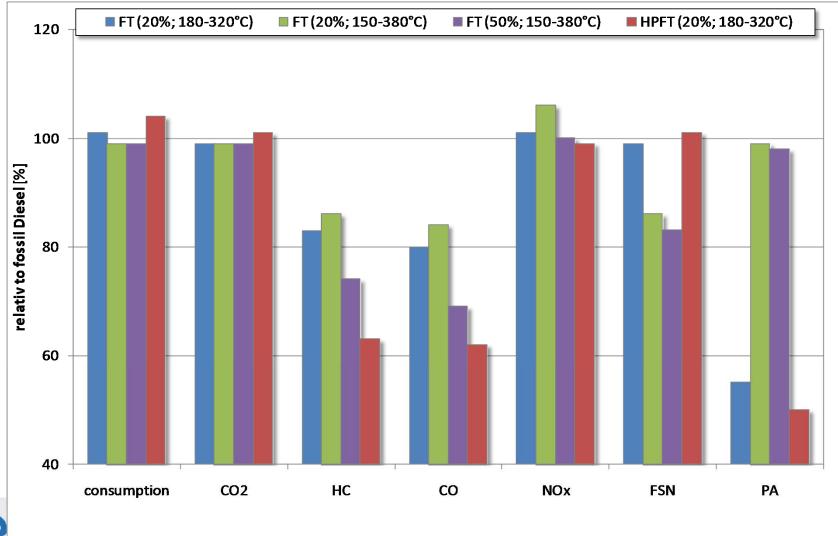
Comparison of produced FT Fuels







Results on engine tests with blends









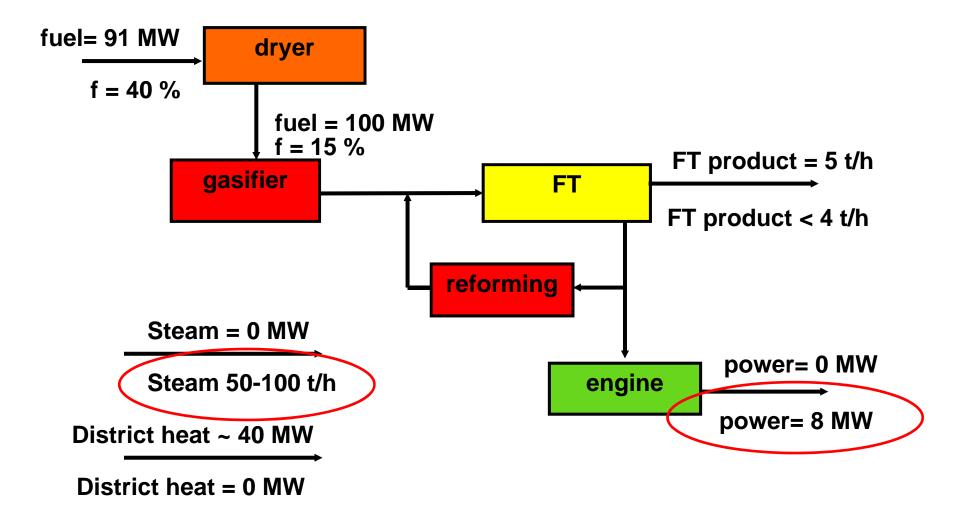
SGC Energia finished successfully their 1bpd demo





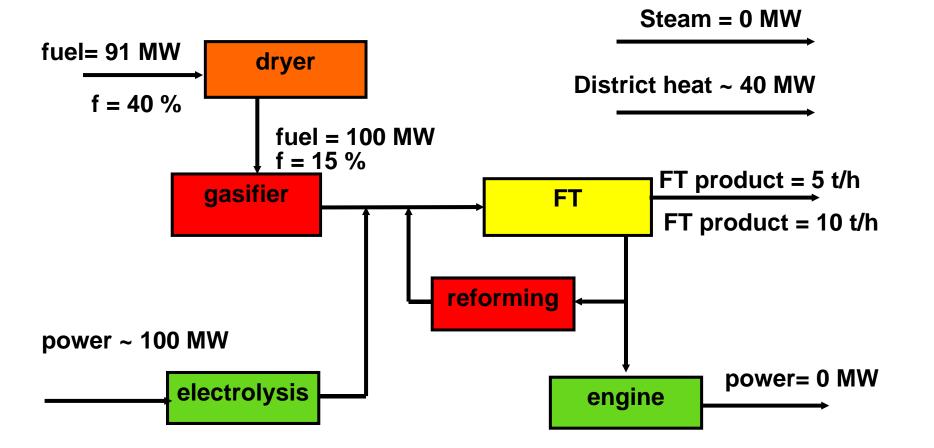
Cases for FT













- Successful scale up of a dual fluidized bed steam gasification system from laboratory to industrial scale (within 10 years)
- Several industrial plants available with
 - High electrical efficiency (> 30 % with combined gas engine and ORC-process)
 - No solid residues (only ash, carbon content <0,5 %)
 - No liquid condensates
 - European emission requirements are met
 - High availabilities (>90 %)
 - Three plants are already in operation (8-15 MW_{fuel})
- High potential for biofuels (BioSNG, BioFiT)
 - BioSNG, most suitable,
 - BioFiT, research ongoing, scale up to 1 bpd is ongoing
- Biomass CHP Güssing and now also Oberwart is optimal for research, as synthesis gas is available for 7000 hours per year





Information

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