

Biomass steam gasification - A platform for synthesis gas applications

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Team of R&D

Scientific partners



VIENNA UNIVERSITY OF TECHNOLOGY

Engineering (as example)



Operators (as example)





bioenergy2020





bioenergy2020+

Bioenergy 2020+ is a Competence Centre funded according to the rules of the COMET program from Austria

Start of the project in COMET Program: Foundation of company "bioenergy 2020+": Headquarter: Research locations: Additional research locations:

Budget per year: Funding: Personal:

Homepage

01st April 2008 29th January 2009 Graz Güssing, Wieselburg Pinkafeld, Tulln

4.5 Mio.€55%about 70 full time equivalents

http://www.bioenergy2020.eu/



Bioenergy 2020+ Vision

| State | of | scie | ence |
|-------|----|------|------|
| | | | |

Vision of BIOENERGY 2020+

Areal: Biomass combustion

conventional biomass fuels (wood fuels, straw)

modern biomass combustion technologies

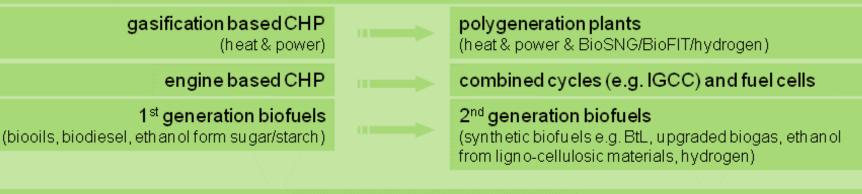
conventional CHP technologies

new biomass fuels (annual crops, short rotation plants, waste materials from the agricultural and the food in dustry, etc.)

next generation biomass combustion systems (towards zero emission technologies)

innovative small- and micro-scale CHP systems advanced highly efficient medium-scale systems

Areall: Biomass gasification, fermentation and liquid biofuels



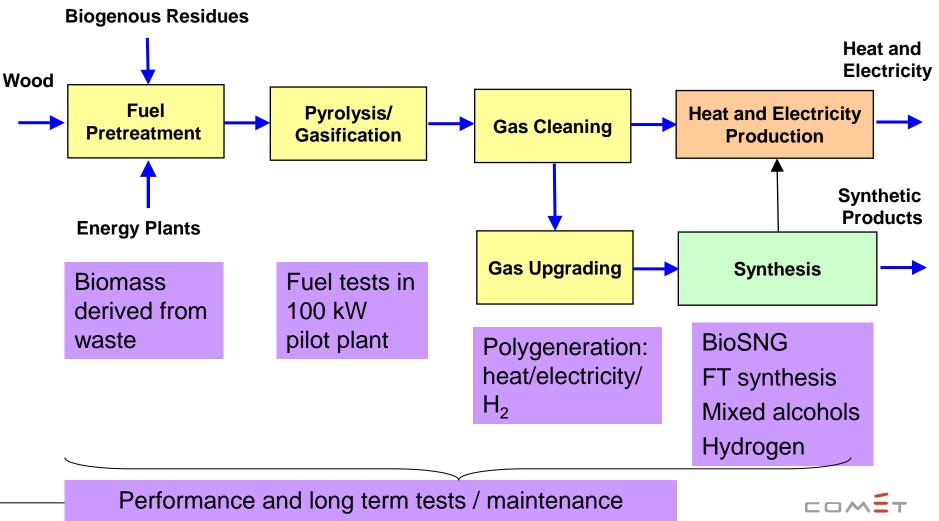
Area III: Modelling and simulation

single model development virtual biomass conversion plant



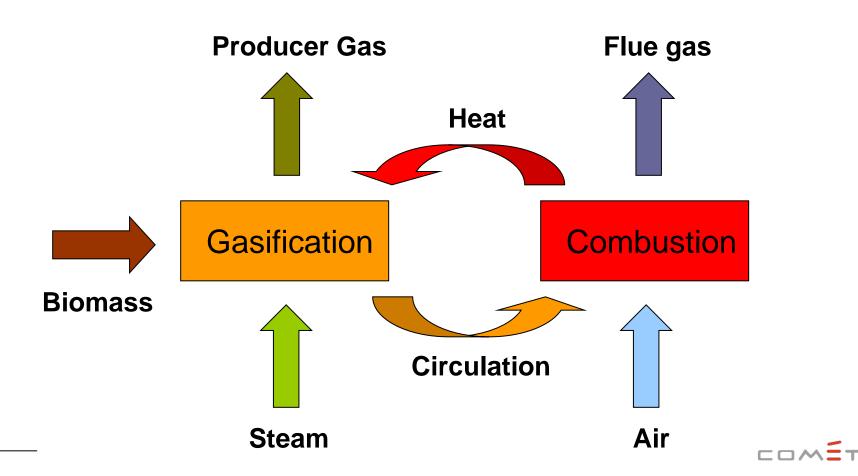
Research along the process chain

Optimisation of the whole chain



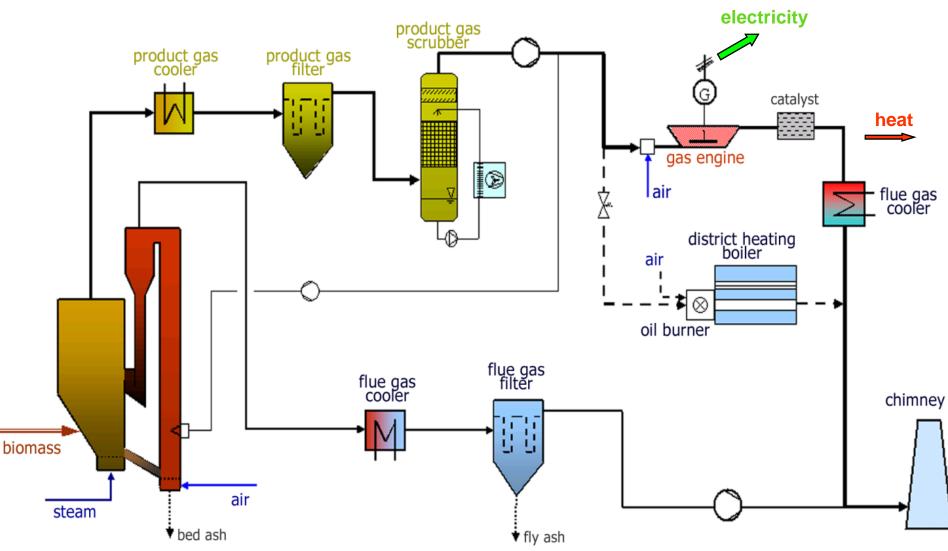








CHP-PLANT GÜSSING





Gas Composition (after gas cleaning)

| Main Components | | | | |
|-----------------|---|-------|--|--|
| H ₂ | % | 35-45 | | |
| СО | % | 20-25 | | |
| CH₄ | % | ~10 | | |
| CO ₂ | % | 20-25 | | |

| Minor Components | | | |
|--------------------------------|-------|-------|--|
| C_2H_4 | % | 2-3 | |
| C_2H_6 | % | ~0.5 | |
| C_3H_4 | % | ~0,4 | |
| O ₂ | % | < 0,1 | |
| N ₂ | % | 1-3 | |
| C ₆ H ₆ | g/m³ | ~8 | |
| C ₇ H ₈ | g/m³ | ~0,5 | |
| C ₁₀ H ₈ | g/m³ | ~2 | |
| TARS | mg/m³ | 20-30 | |

| Possible poisons | | | | |
|------------------|---------------------|----------|--|--|
| H ₂ S | mgS/Nm ³ | ~200 | | |
| Mercaptans | mgS/Nm ³ | ~30 | | |
| Thiophens | mgS/Nm ³ | ~7 | | |
| HCI | ppm | ~3 | | |
| NH3 | ppm | 500-1000 | | |
| Dust | mg/Nm ³ | < 20 | | |

H₂:CO = from 1.5:1 to 2:1





Commercial FICFB gasifiers

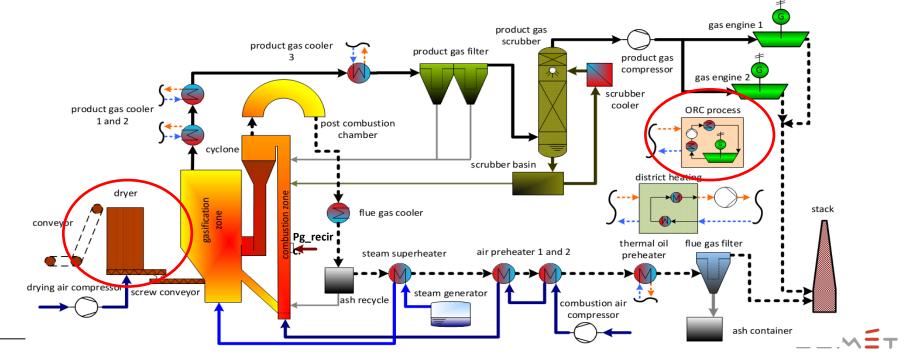
| Location | Usage / Product | Fuel / Product MW, MW | Start up | Supplier | Status |
|---------------------|--------------------------------------|--|----------|----------------------|-----------------------------------|
| Güssing, AT | Gas engine | 8.0 _{fuel} / 2.0 _{el} | 2002 | AE&E, Repotec | Operational |
| Oberwart, AT | Gas engine / ORC / H ₂ | 8.5 _{fuel} / 2.8 _{el} | 2008 | Ortner Anlagenbau | Operational |
| Villach, AT | Gas engine | 15 _{fuel} / 3.7 _{el} | 2010 | Ortner Anlagenbau | Operational |
| Klagenfurt, AT | Gas engine, BioSNG | 25 _{fuel} / 5.5 _{el} | ? | Ortner Anlagenbau | Planing |
| Senden/Ulm DE | Gas engine / ORC | 14 _{fuel} / 5 _{el} | 2011 | Repotec | Commissioning |
| Göteborg, Sweden | BioSNG | 32 _{fuel} /20 _{BioSNG} | ? | Metso/ Repotec | Construction |
| Vienna, OMV | Hydrogen | 50 _{fuel} /30 _{hydrogen} | ? | Repotec | Planing – decision end of 2012 |



FICFB Oberwart

- FICFB, gas engine, ORC
- 8.5 MWfuel, 2.8 MWel
- 17.000 t wood chips/year
- District heating distance 5.2 km

| Product gas composition | | | |
|-------------------------------|----------------|--|--|
| H ₂ 35 - 45 vol. % | | | |
| СО | 18 – 23 vol. % | | |
| CO ₂ | 20 – 24 vol. % | | |
| CH ₄ | 7 – 10 vol. % | | |
| C _x H _v | 1-3 vol. % | | |





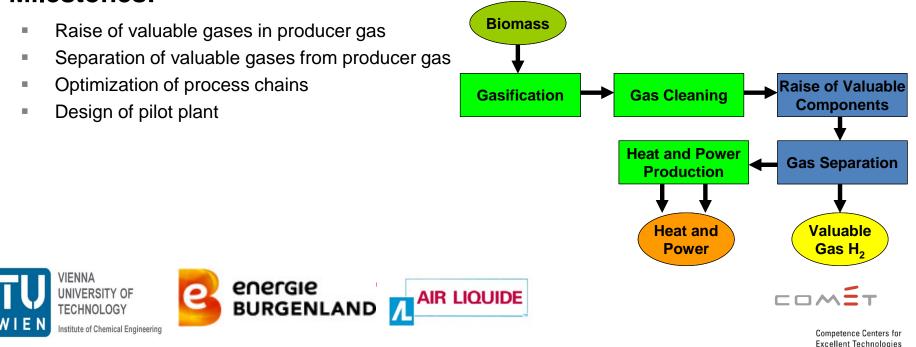
Polygeneration

Production of Valuable Gases, Electricity and Heat from Biofuels

Objective:

 Develop economic feasible process configurations for the production of valuable gases, heat and electricity by using polygeneration strategies.

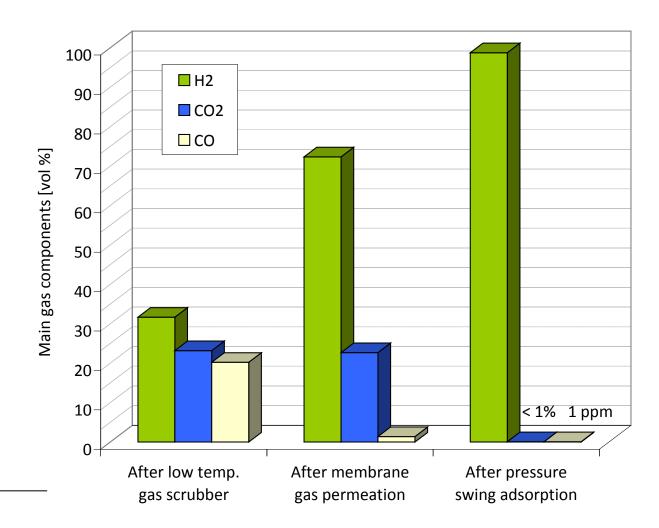
Milestones:







Polygeneration – Results



Hydrogen is used in a PEM fuel cell



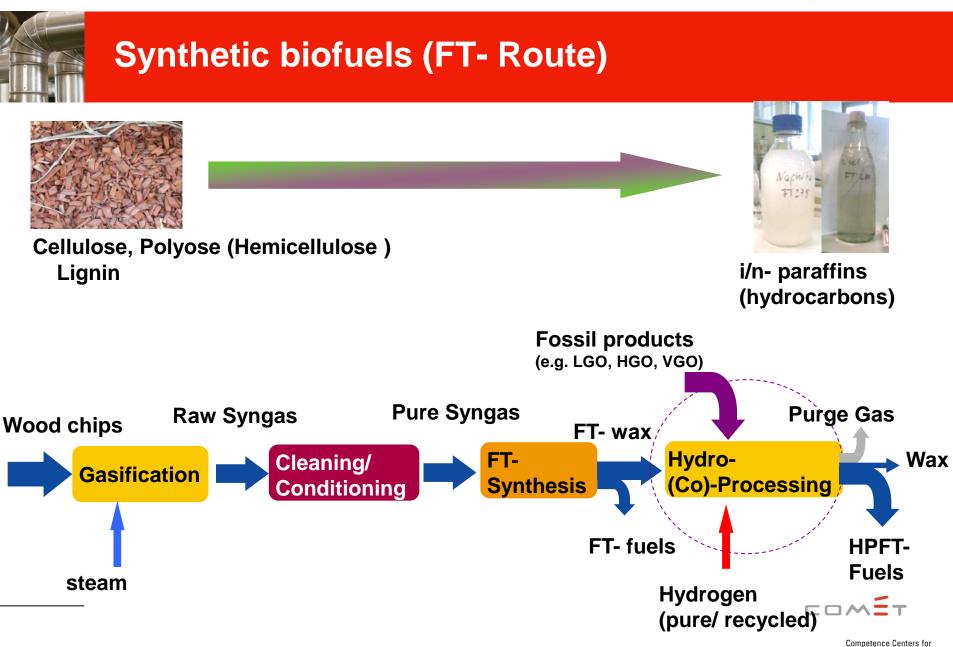




Biomass CHP Güssing



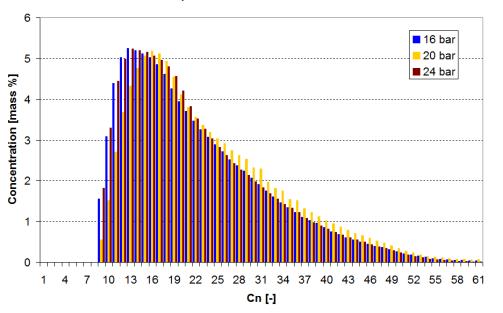




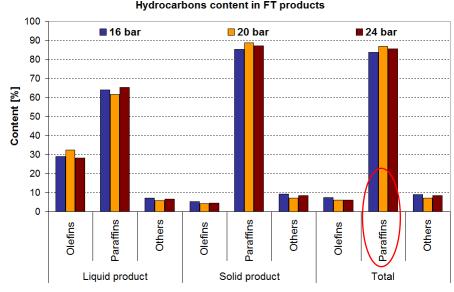
Excellent Technologies



Product distribution and Hydrocarbons content



The experimental carbon distribution









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Performances of FT synthesis

| Experiment | Pressure [bar] | CO conversion [%] | a value [-] | C ₅₊ selectivity [%] | Par/Ole ratio [-] | H ₂ /CO ratio [-] |
|------------|-------------------|-------------------------|----------------|------------------------------------|-------------------------|---------------------------------|
| 1 | 16 | 44.2 | 0.892 | 90.6 | 11.4 | 1.5 |
| 2 | 20 | 52.5 | 0.9 | 91.7 | 14.1 | 1.6 |
| 3 | 24 | 63.7 | 0.89 | 90.3 | 13.8 | 2.0 |
| | | | | | | |

UNIVERSITATEA





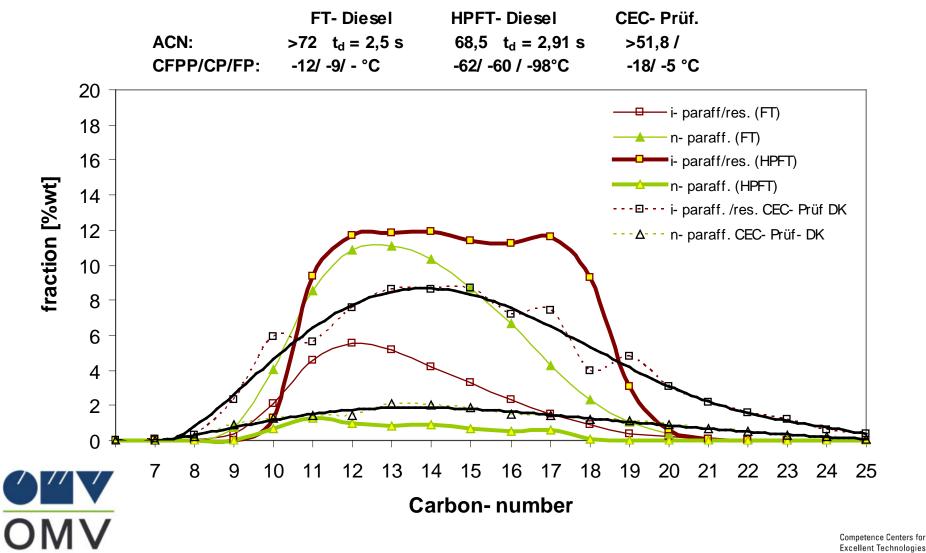
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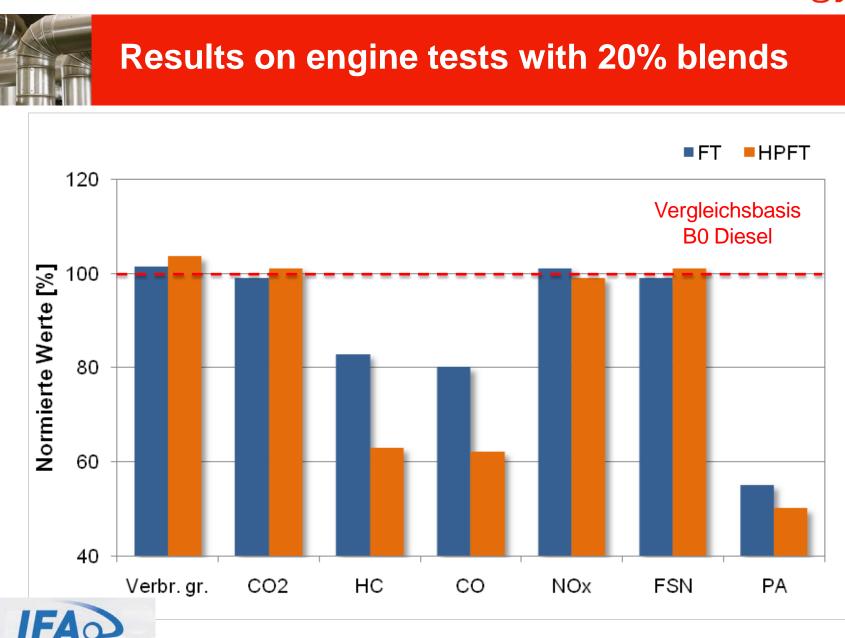


COMÉT



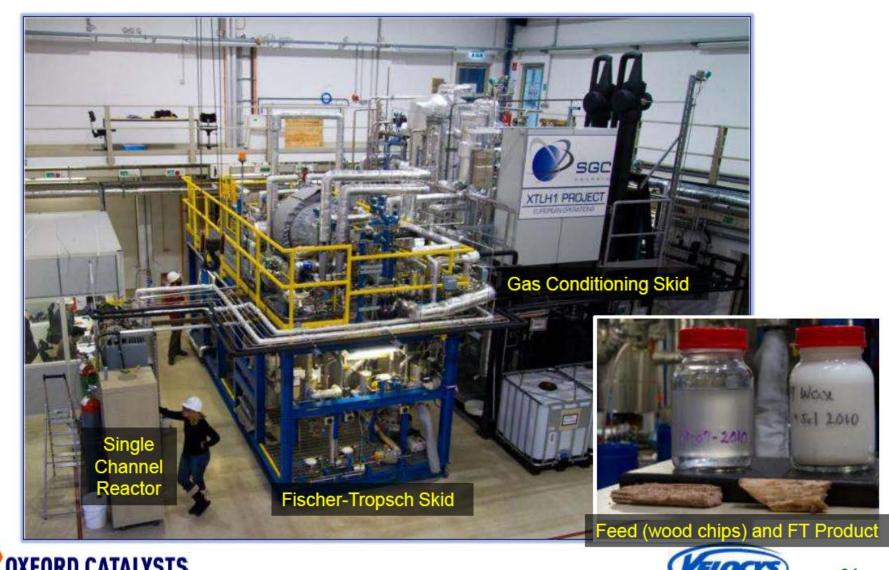
Comparison of produced FT Fuels





Institut für Fahrzeugantriebe & Automobiltechnik

SGC Energia finished successfully their 1 bpd demo

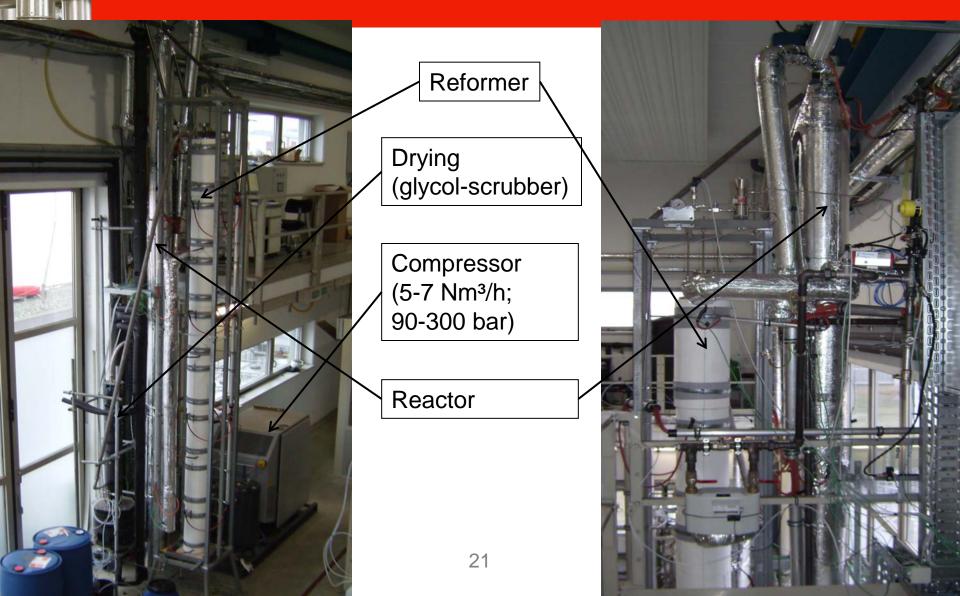




- Funded by "Klima und Energiefonds" and Bioenergy 2020+
- Aim is to get fundamental know how in the synthesis of mixed alcohols from biomass
- Main advantage is very simple gas cleaning, due to sulphur resistant catalyst



Actual status: first experiments are done



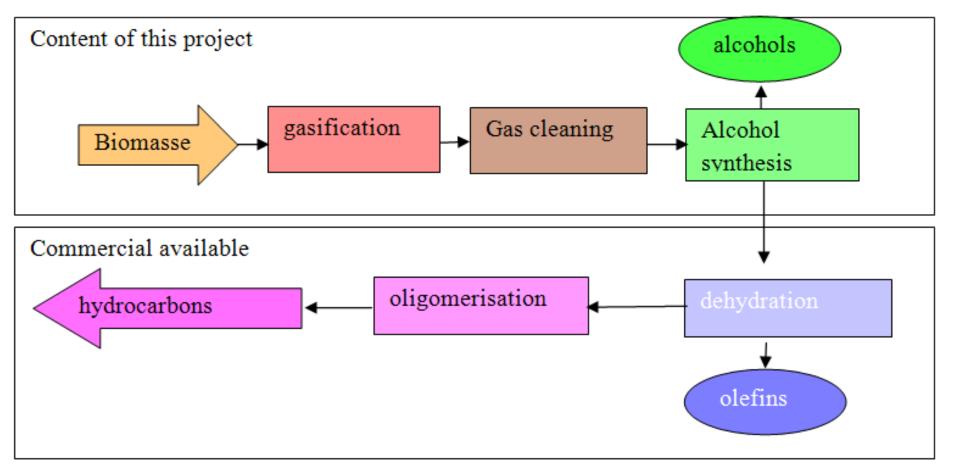


- The MoS based catalysts need about 50-100ppm of H₂S in the synthesis gas to keep the sulfidation status constant which is necessary for a constant activity. So a removal of sulphur is not necessary, which reduced the investment costs dramatically.
- These catalysts are not sensitive to CO₂ in the synthesis gas. Only for CO₂-contents above 30% a removal of CO₂ is necessary.
- Carbon deposits (coking) are normally no problem, also at H_2/CO ratios smaller than 2.
- Mainly linear alcohols are produced.











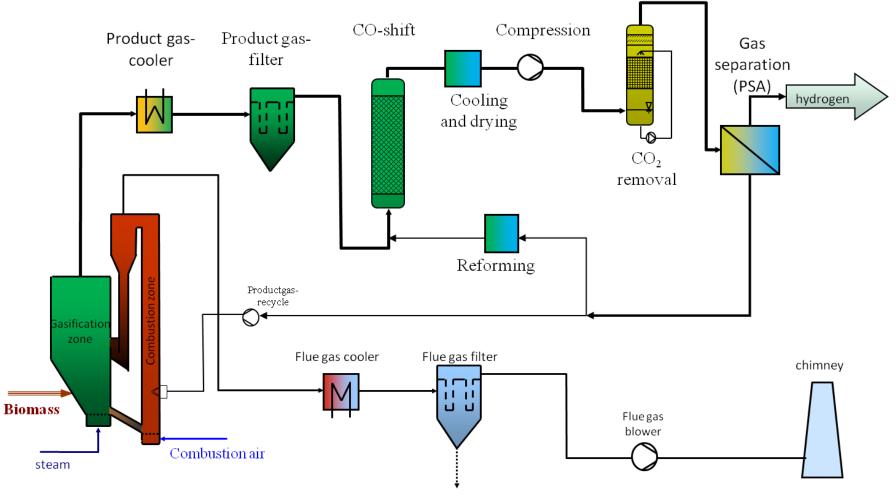
BioH2-4Refineries

Economic evaluation of production of hydrogen for a refinery

- Coordination by OMV
- 50 MW fuel plant to replace fossil hydrogen
- Evaluation of the biomass resources available for such a plant
- Basic engineering of the gasifier as well as of all other sub units, including pipelines, utility systems, logistic needs
- Optimal use of by-products
- Economic evaluation



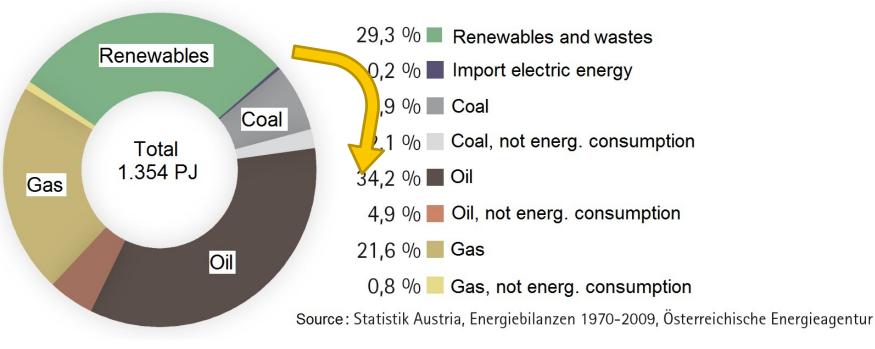
Simplified flow chart



Current Status and Outlook

- Successful scale up of a dual fluidized bed steam gasification system from laboratory to industrial scale (within 10 years)
- Industrial plant available with
 - High electrical efficiency (> 30 % with combined gas engine and ORCprocess)
 - No solid residues (only ash, carbon content <0,5 %)</p>
 - No liquid condensates
 - European emission requirements are met
 - High availabilities (>90 %)
 - Three plants are already in operation (8-15 MW_{fuel})
 - High potential for biofuels (BioSNG, BioFiT)
 - BioSNG, most suitable, 1 MW (100 m³/h BioSNG), demonstration plant is in operation (soon again)
 - BioFiT, research ongoing, scale up to 1 bpd is ongoing
- Biomass CHP Güssing optimal for research, as cheap synthesis gas is available for 7000 hours per year

Future



More info at http://www.ficfb.at http://www.vt.tuwien.ac.at http://www.bioenergy2020.eu





Conversion of wind and photovoltaic to transportation fuels

