

Techno-economic and Market Analysis of Pathways from Syngas to Fuels and Chemicals



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Objective

Assess the economics of producing fuels and chemicals from biomass-derived synthesis gas.

- Process economics based on literature (consistent TEA assumptions)
- Perform more rigorous TEA on promising pathways
 - Biochemical conversion of syngas to ethanol and higher alcohols
 - o Ethanol and higher alcohols to infrastructure-compatible hydrocarbons
- Simple product market analyses

What can we do with syngas?

Analysis Approach

- Simplified TEA model
- Inputs from literature sources
 - Feedstock rate and properties (heating value)
 - Product yields
 - Operating costs (variable & fixed)
 - Capital costs
- Common scaling assumptions
 - Capital scaling exponents
 - Economies of scale for fixed operating costs
- Operating and financing assumptions for nth plant and pioneer plant
- Minimum Product Selling Price

literature values → average, standard deviation & 90% confidence intervals

nth Plant Assumptions

Parameter	Value
Basis year for analysis	2011
Feedstock processing capacity	2,000 Dry Tonnes / SD
Feedstock cost (woody biomass)	\$75 / Dry Ton (€21.60 / MWh)
Debt / equity for plant financing	60% / 40%
Internal rate of return (after-tax) for equity financing	10%
Annual interest rate and term for debt financing	8% / 10 years
Total income tax rate	35%
Plant life	30 years
Plant depreciation schedule	7-year IRS MACRS MACRS = Modified Accelerated Cost Recovery System
Reliability of operations / on-stream factor	0.90
Site development costs	4% of ISBL Installed Capital
Working capital	5% of Fixed Capital Investment
Indirect costs for capital project	60% of Total Direct Costs
Capital equipment capacity scaling exponent	0.70

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Pioneer Plant Assumptions

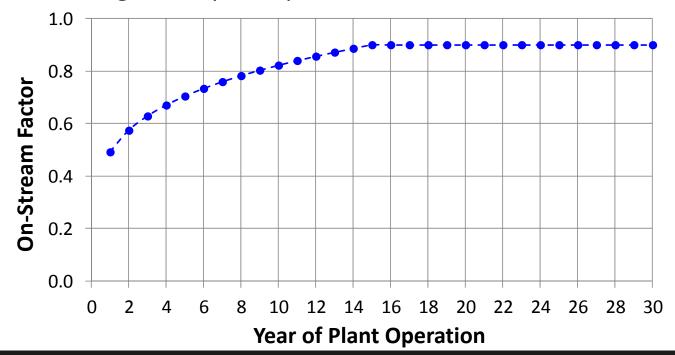
- Internal Rate of Return (IRR): 10% 25%
- Capital Costs:

Pioneer Plant Escalation ~ 210% of nth Plant Estimates (Merrow et al, Rand, 1981)

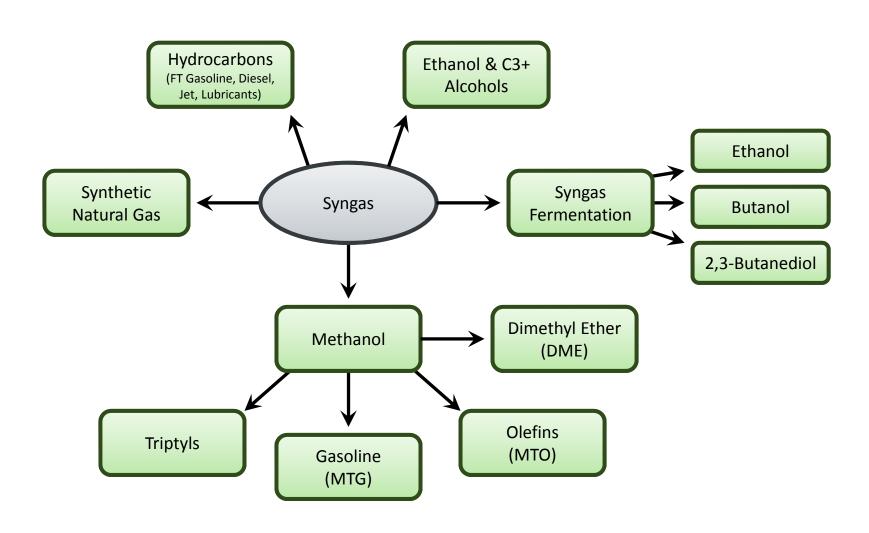
• Reliability of Operations / On-Stream Factor:

Initial value of 0.5 (Merrow et al, Rand, 1981)

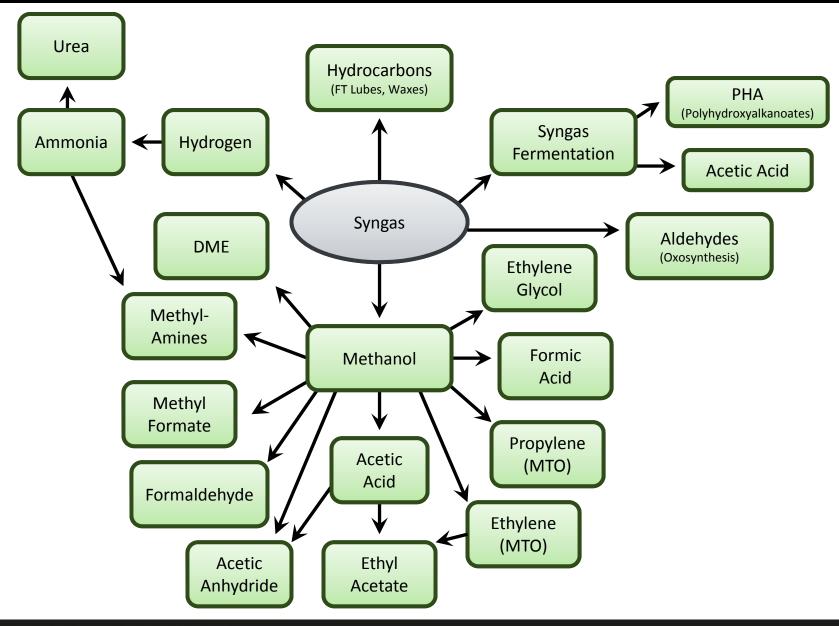
Increasing to 0.9 per experience curve (Heinen, SRI Consulting, 2001)



Fuel Pathways Explored



Chemical Pathways Explored



Major Pathway Categories Explored

- Synthetic Natural Gas via Methanation of Syngas
- Ethanol
 - Catalytic Mixed Alcohol Synthesis
 - Syngas Fermentation *
- Hydrocarbons
 - Fischer-Tropsch
 - Methanol to Naphtha Hydrocarbons
 - Ethanol & Higher Alcohols to Hydrocarbons *
- **Hydrogen** via Steam Reforming, WGS & Purification
- Methanol via Catalytic Methanol Synthesis

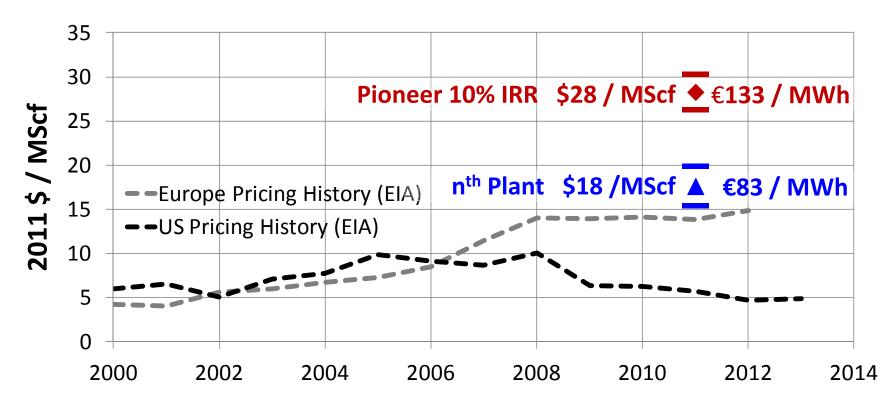
^{*} Pathways explored by NREL through Aspen modeling and rigorous TEA.

Synthetic Natural Gas

Methanation of Syngas

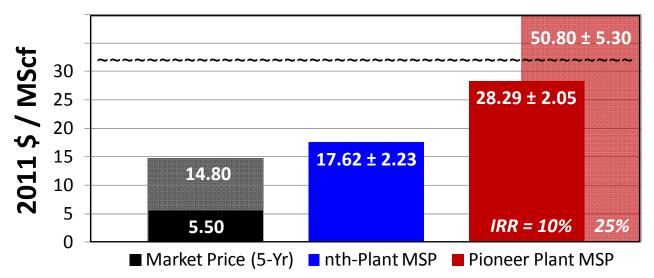
Synthetic Natural Gas

Process	Sources	Min. Selling Price Range (\$ / MScf)		
Syngas to SNG via	McKeough & Kurkela, 2007 Mozaffarian et al, 2004	n th Plant	16.52 – 19.13	
methanation van der Drift et al, 2005	Pioneer 10% IRR	27.07 – 29.52		
		Pioneer 25% IRR	47.50 - 53.97	



Synthetic Natural Gas

Techno-economic Analysis



Market Analysis		U.S.	Europe
Average Product Yield	Scf / Ton	11,440	11,440
Consumption (EIA, 2012)	Scf / Year	25.5T	19.0T
10% of Natural Gas Market	Scf / Year	2.55T	1.90T
Equivalent Biomass Consumption	MMTon / Year	223	165
Equivalent Biorefineries (2,000 To	nne / Day)	310	230

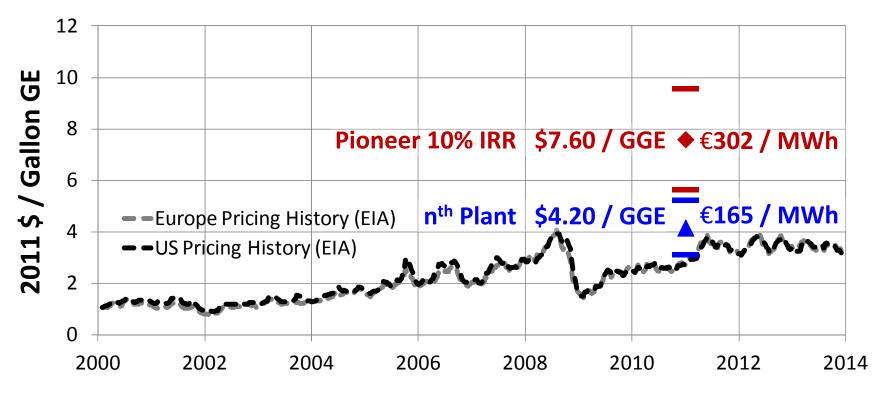
Ethanol

- Catalytic Mixed Alcohol Synthesis
- Syngas Fermentation *

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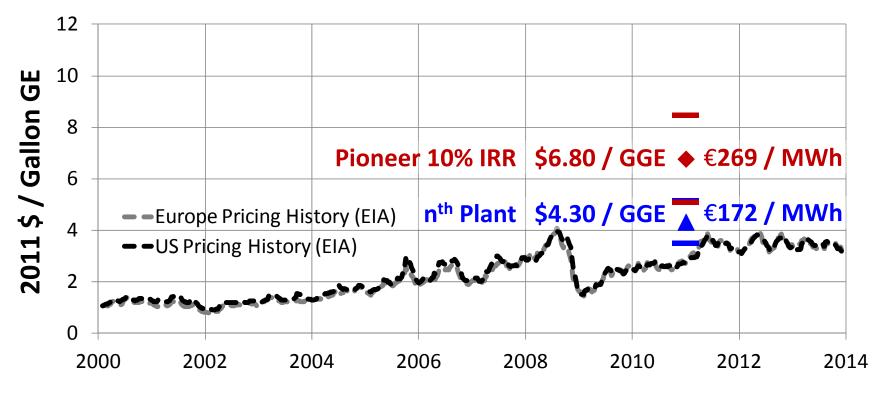
Ethanol via Mixed Alcohol Synthesis

Process	Sources	Min. Selling Price Range (\$ / Gal GE)		
Syngas to ethanol	Dutta et al, 2011 Dutta & Phillips, 2009	n th Plant	2.87 – 4.83	
via catalytic mixed alcohol synthesis Dutta & Philips, 2009 Dutta et al, 2010 He & Zhang, 2011 Villanueva Perales et al, 2011	Pioneer 10% IRR	5.34 - 9.08		
	Pioneer 25% IRR	10.66 - 18.15		



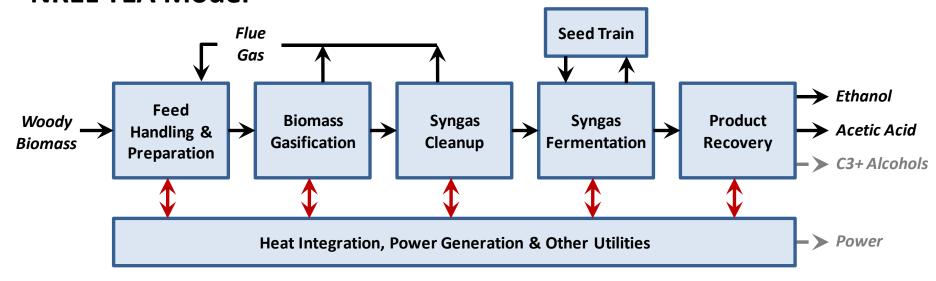
Ethanol via Syngas Fermentation

Process	Sources	Min. Selling Price Range (\$ / Gal GE		
Ethanol via syngas	Putsche,1999 van Kasteren & Verbene, 2005	n th Plant	3.67 – 5.08	
fermentation Piccolo & Bezzo, 2007	Pioneer 10% IRR	5.77 – 8.50		
		Pioneer 25% IRR	8.92 - 16.12	



Ethanol via Syngas Fermentation

NREL TEA Model

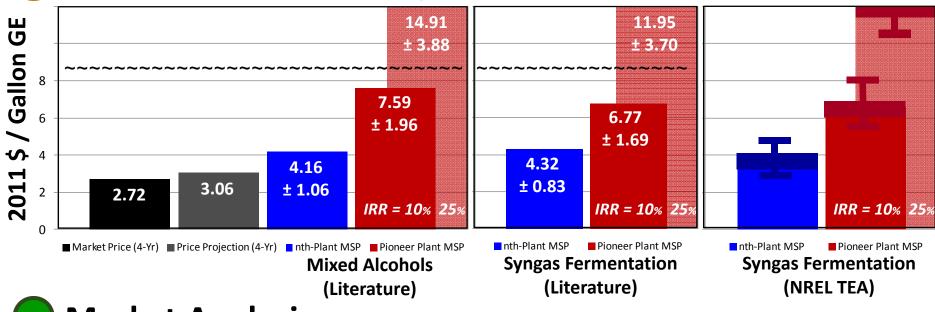


- Design Report NREL/TP-5100-51400 utilized as basis through clean compressed syngas from biomass.
- Yield structures based on publications from LanzaTech & INEOS Bio.
- Capital costs for fermenters, seed train and cell recovery developed by Harris Group Inc.

Ethanol



Techno-economic Analysis





Equivalent Biorefineries (2,000 Tor	100	80	
Equivalent Biomass Consumption	MMTon / Year	76	60
50% of Fuel Ethanol Market	Gallons / Year	6.5B	5.0T
Consumption (EIA, 2013)	Gallons / Year	13.0B	10.0T
Average Product Yield	Gallons / Ton	85	85

Europe

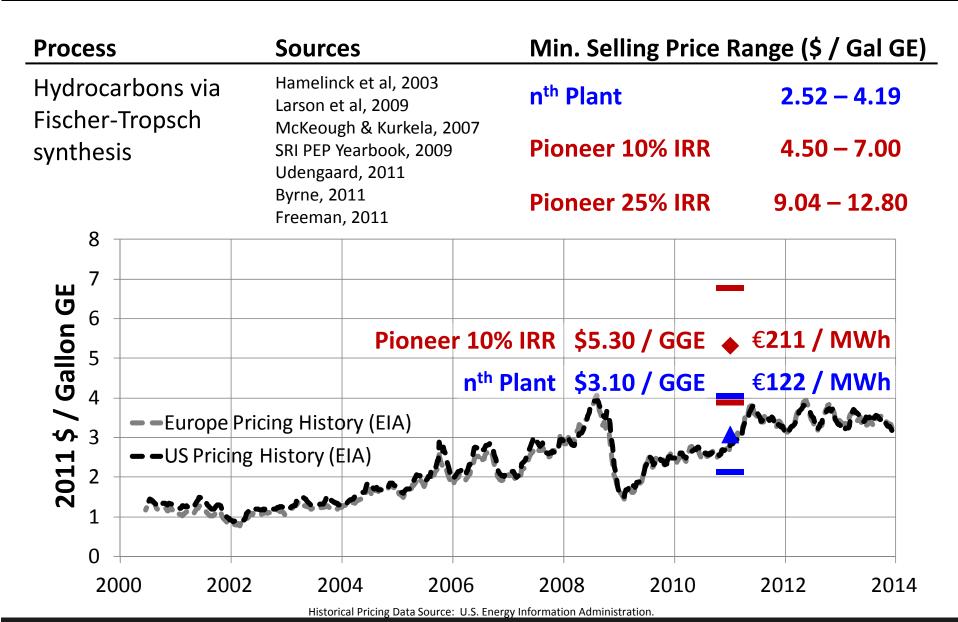
U.S.

Hydrocarbons

- Fischer-Tropsch
- Methanol to Naphtha Hydrocarbons
- Ethanol & Higher Alcohols to Hydrocarbons *

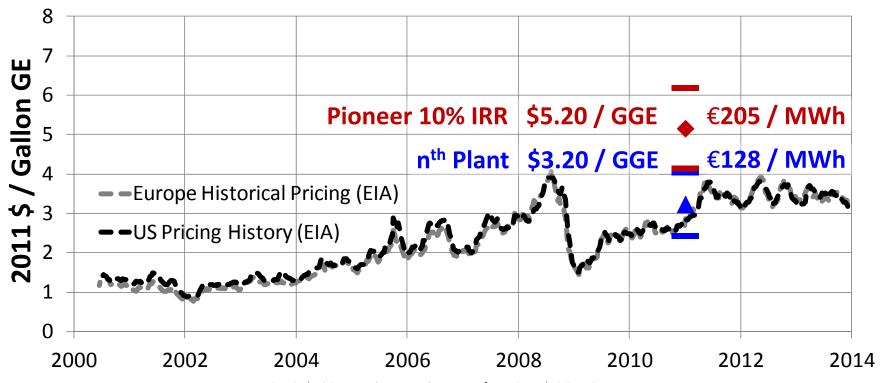
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Fischer-Tropsch Hydrocarbons



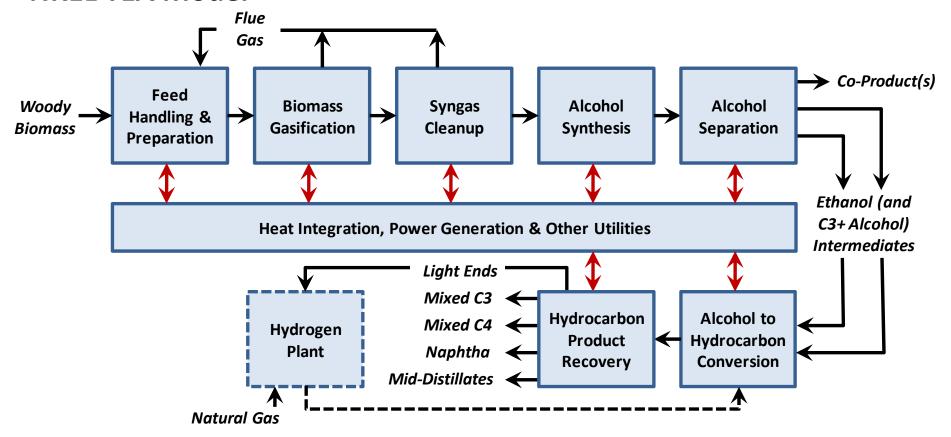
Methanol to Hydrocarbons

Process	Sources	Min. Selling Price Range (\$ / Gal GE)		
Hydrocarbons via	Phillips et al, 2011 Hindman, 2010	n th Plant	2.61 – 3.84	
methanol synthesis SRI PEP Report 191A, 1999 and methanol Udengaard, 2011	Pioneer 10% IRR	4.42 – 6.12		
conversion	Jones & Zhu, 2009 Ahn et al, 2009	Pioneer 25% IRR	8.22 - 10.79	



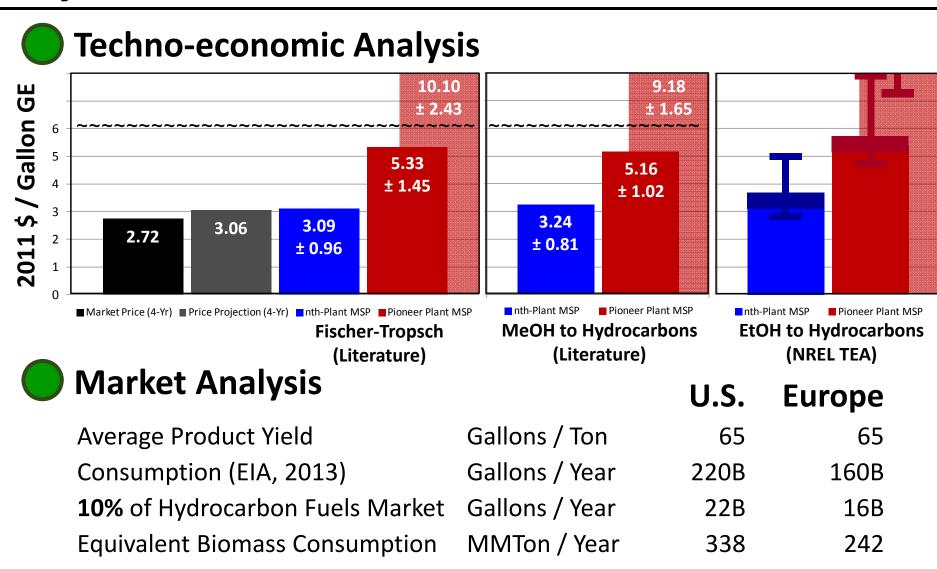
Ethanol & Higher Alcohols to Hydrocarbons

NREL TEA Model



- Ethanol (and higher alcohol) intermediates for hydrocarbon fuel production.
- Eliminates constraints of renewable ethanol blend limits.
- Technology development taking place in academia, national labs and industry.

Hydrocarbon Fuels



Equivalent Biorefineries (2,000 Tonne / Day)

310

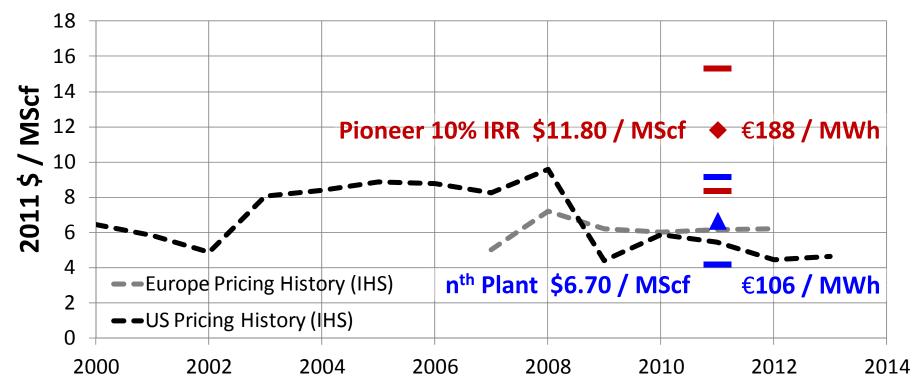
440

Hydrogen

• Steam reforming, water-gas shift & purification

Hydrogen

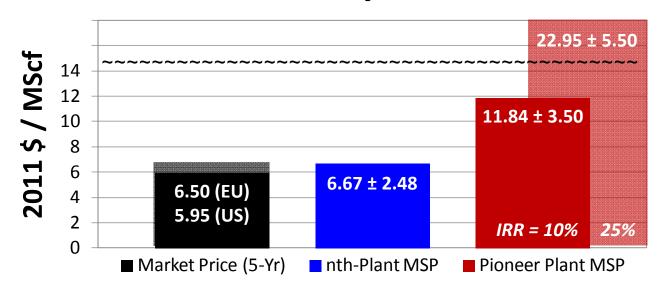
Process	Sources	Min. Selling Price Range (\$ / MScf)		
Syngas to H ₂ via	Spath et al, 2005 McKeough & Kurkela, 2003	n th Plant	5.33 - 8.84	
steam reforming,	Williams et al, 1995	Pioneer 10% IRR	9.87 – 14.82	
water-gas shift &	Hamelinck & Faaij, 2001			
purification		Pioneer 25% IRR	19.80 – 27.60	



Historical Pricing Data Source: SRI / IHS CEH Marketing Research Reports. Projected values based on ratios to EIA natural gas projections.

Hydrogen

Techno-economic Analysis



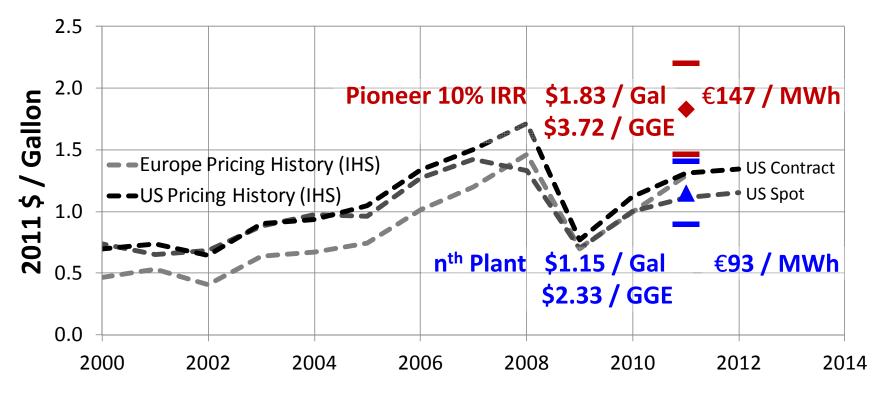
Market Analysis		U.S.	Europe
Average Product Yield	SCF / Ton	37,500	37,500
Consumption (EIA, 2013)	SCF / Year	4.1T	3.2T
10% of HydrogenMarket	SCF / Year	0.41T	0.32T
Equivalent Biomass Consumption	MMTon / Year	11	8.5
Equivalent Biorefineries (2,000 To	nne / Day)	14	11

Methanol

Catalytic Methanol Synthesis

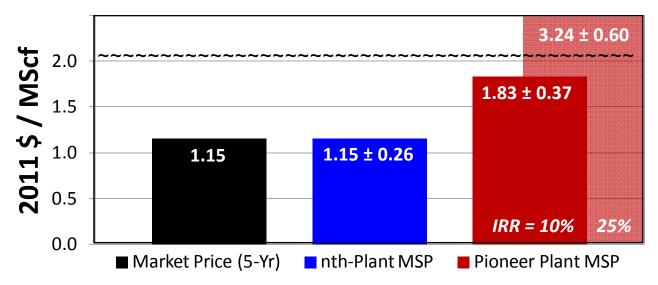
Methanol

Process	Sources	Min. Selling Price Range (\$ / Gal)		Min. Selling Price Range (\$ /	
Syngas to methanol	Tarud & Phillips, 2011 McKeough & Kurkela, 2007	n th Plant	0.96 - 1.32		
via catalytic synthesis	SRI PEP Yearbook, 2009 Williams et al, 1995	Pioneer 10% IRR	1.54 – 2.03		
	Hamelinck & Faaij, 2001	Pioneer 25% IRR	2.82 - 3.71		



Methanol as Chemical Intermediate

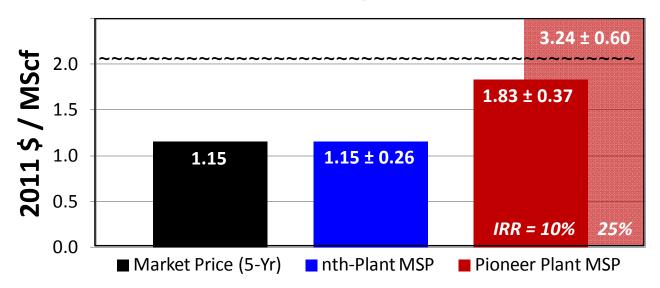
Techno-economic Analysis



Market Analysis		U.S.	Europe
Average Product Yield	Gallons / Ton	170	170
Consumption (IHS)	Gallons / Year	1.9B	2.2B
10% of Methanol Market	Gallons / Year	0.19B	0.22B
Equivalent Biomass Consumption	MMTon / Year	1.1	1.3
Equivalent Biorefineries (2,000 To	nne / Day)	1.4	1.6

Methanol as Fuel Intermediate

Techno-economic Analysis



Market Analysis		U.S.	Europe
Average Product Yield	Gallons / Ton	65	65
Consumption (EIA, 2013)	Gallons / Year	220B	160B
10% of Hydrocarbon Fuels Market	Gallons / Year	22B	16B
Equivalent Biomass Consumption	MMTon / Year	338	242
Equivalent Biorefineries (2,000 Tonne / Day)		440	310

Conclusions

- Hydrocarbon, ethanol and methanol economics can be competitive for nth-plant.
- Pioneer plant economics are challenged overall.
- Market capacities do not constrain bio-product pathways in major hydrocarbon fuel markets (natural gas, petroleum fuels).
- With fixed ethanol blend limit, cellulosic pathways and grainderived product will compete for limited market.
- Market capacities for methanol-derived chemicals are constraining.
- Syngas fermentation is potentially competitive, depending on
 CO / H₂ conversion to product(s).
- Methanol and ethanol are attractive intermediates for production of infrastructure-compatible hydrocarbons.

Future Work

- Apply simplified TEA and market analysis on emerging pathways to identify economic feasibility in early stages of development.
- Explore opportunities to improve Pioneer Plant economics
 - Biomass co-feeding opportunities (NG-Biomass to Liquids)
 - Utilizing inexpensive feedstocks
 - High-value co-products
 - RIN credits
- Evaluate infrastructure hurdle for methanol economy

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- NREL Biorefinery Analysis and Thermochemical Platform Teams

References

For a complete list of references utilized in this analysis, please contact Mike Talmadge (michael.talmadge@nrel.gov / 303-275-4632)