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IMAGINEERING  
NATURE

# Bio-Acetate production via dual fluidized bed syngas fermentation

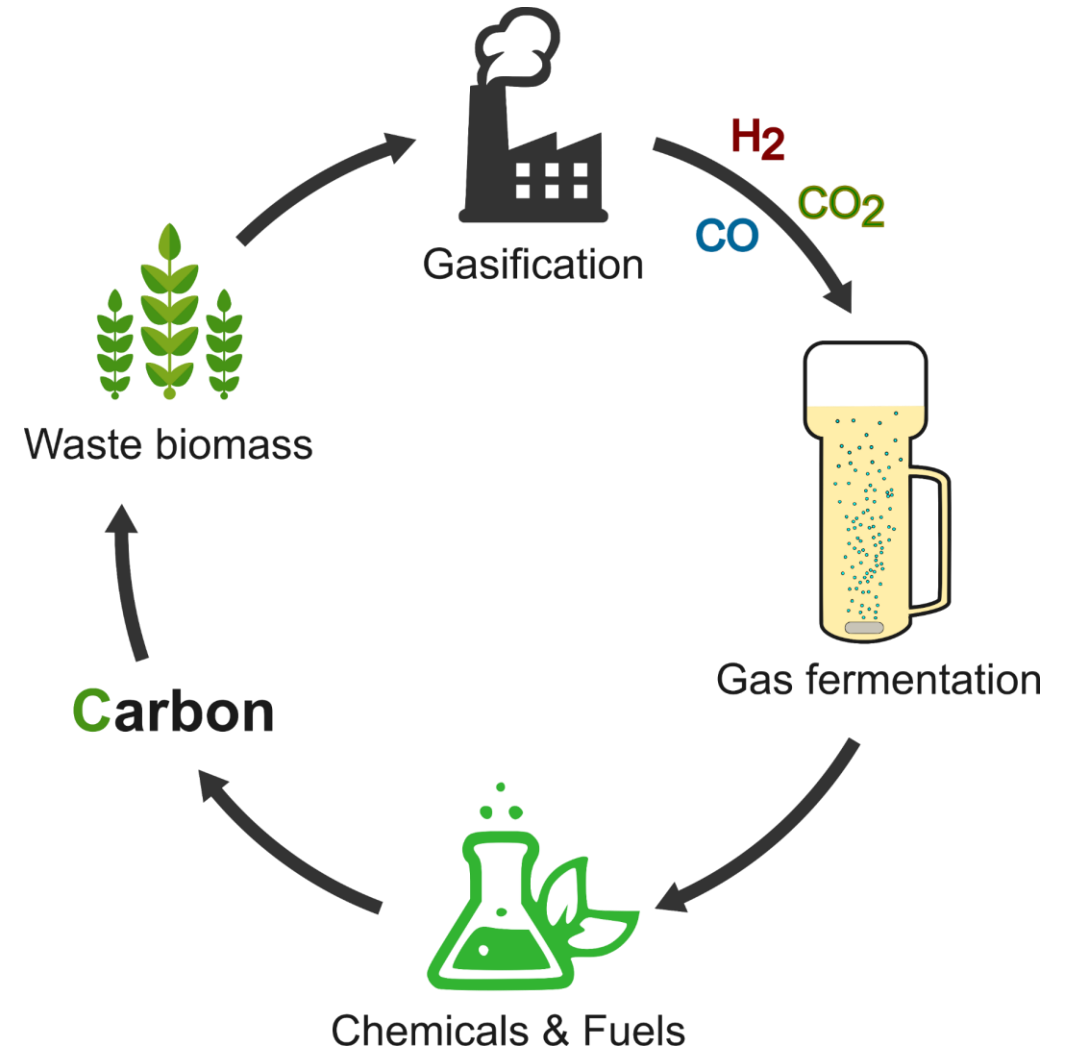
IEA Task 33 Workshop Gasification and Chemicals



# The circular carbon bioeconomy based on biomass

- **Gasification** of lignocellulosic (waste) biomass
  - Dual fluidized bed (DFB) gasification to produce product gas/syngas
  
- **Gas fermentation** to produce chemicals & fuels
  - Bubble column reactor with *Thermoanaerobacter kivui* to produce **acetate** (lactate\*)

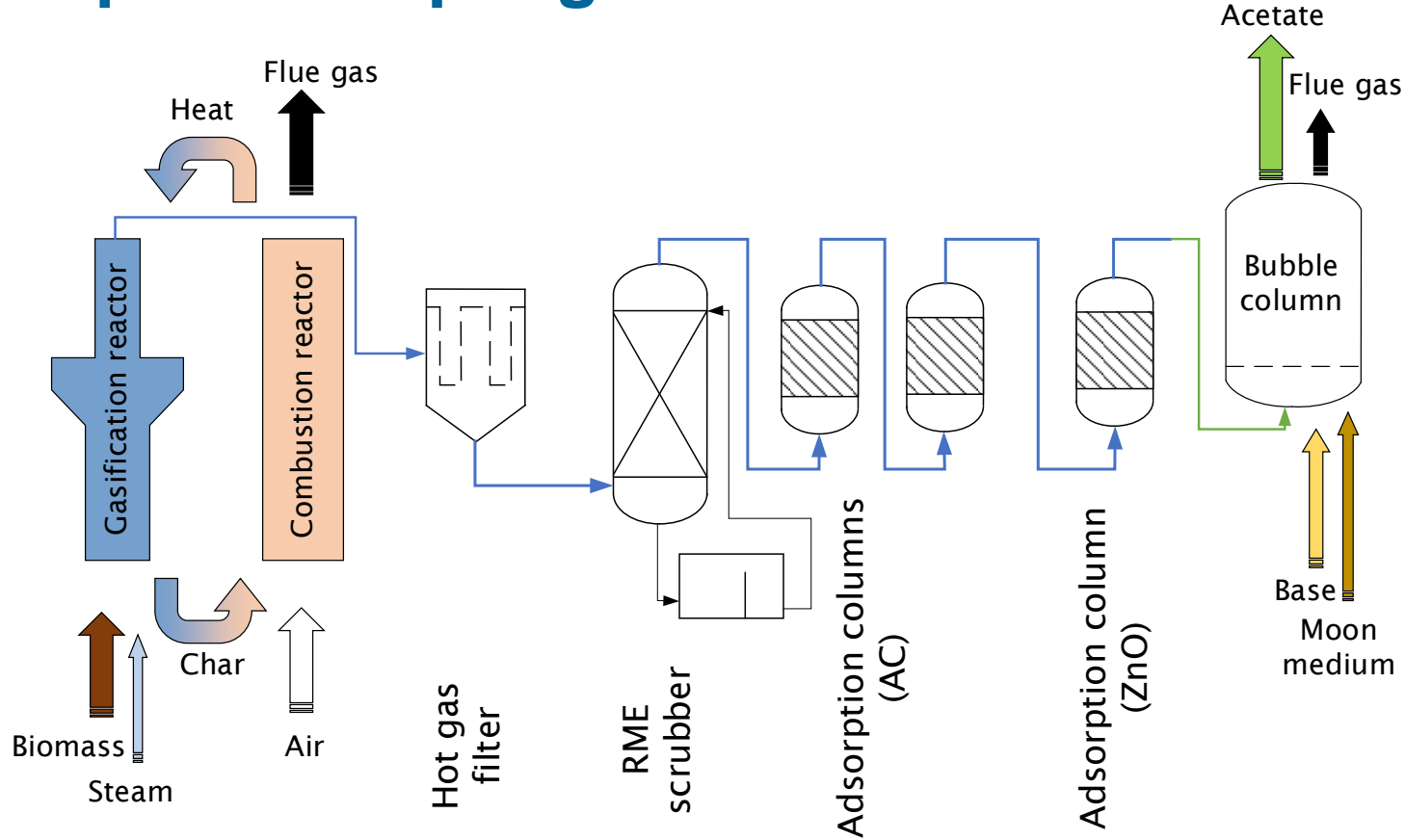
\*currently investigated



Proof of concept: coupling “real” DFB product gas with gas fermentation to produce acetate

- Characterize *T. kivui* physiology/metabolism
- (Re)adaptation of *T. kivui* to CO
- Show acetate production with synthetic gas and parameter testing
- Show resilience to product gas impurities and integration possibilities

# Concept for coupling



DFB steam gasification



Gas cleaning

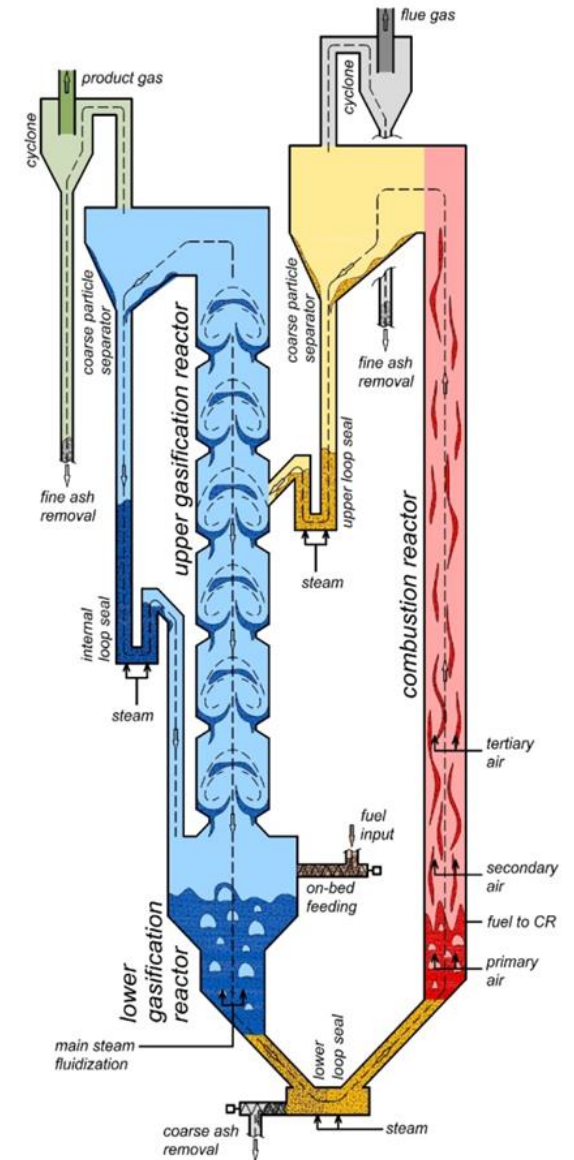
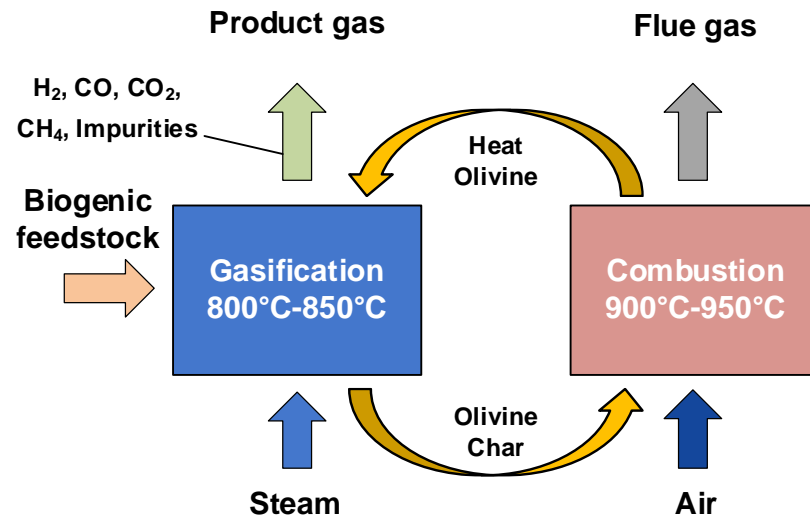


Fermentation

Steiner et al. 2024, in preparation

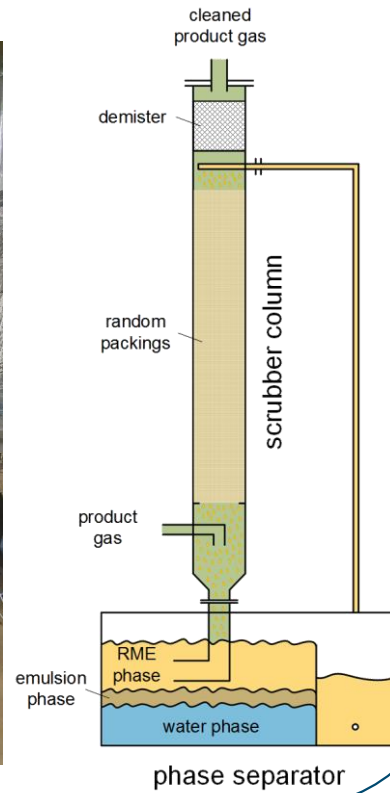
# Dual fluidized bed gasification

- 100 kW<sub>th</sub> advanced DFB pilot plant at TU Wien
- Two inter-connected fluidized beds
- Bed material circulation provides heat
- Nearly N<sub>2</sub>-free product gas (PG)
- Advanced design for enhanced gas-solid contact & soft bed materials



Absorption & condensation of

- Tar compounds
- Water-soluble substances ( $\text{NH}_3$ ,  $\text{HCl}$ , ...)

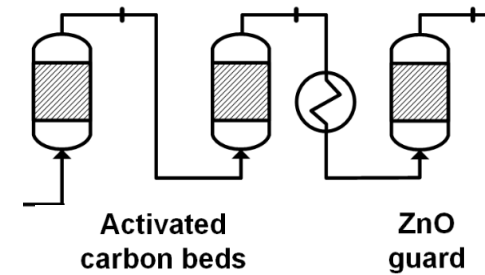


Biodiesel scrubber

Activated carbon beds & zinc oxide

Adsorption of

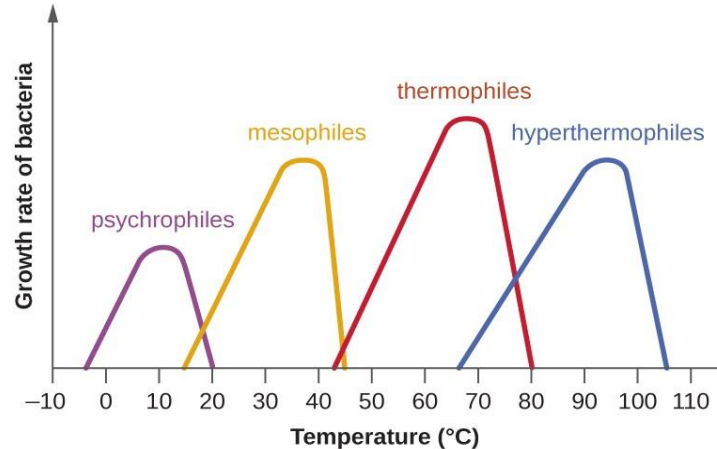
- Hydrocarbons & tar compounds (BTX, naphthalene)
- Sulfur compounds





- „Emerging“ technology
- Mass transfer critical for an economic operation of gas fermentation
- Anaerobic bacteria (acetogenes) suitable for syngas fermentation
- Robust biocatalysts with high tolerance
- High carbon and energy efficiency

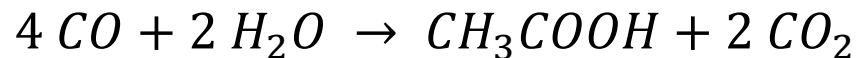
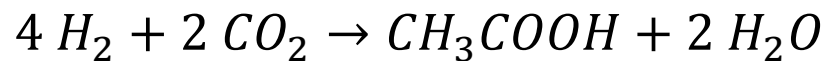
- *T. kivui* is a thermophilic acetogenic bacteria
  - growth at ~70°C
  - low cooling costs
  - high growth rates



20 liter bubble column gas fermentation reactor at TU Wien

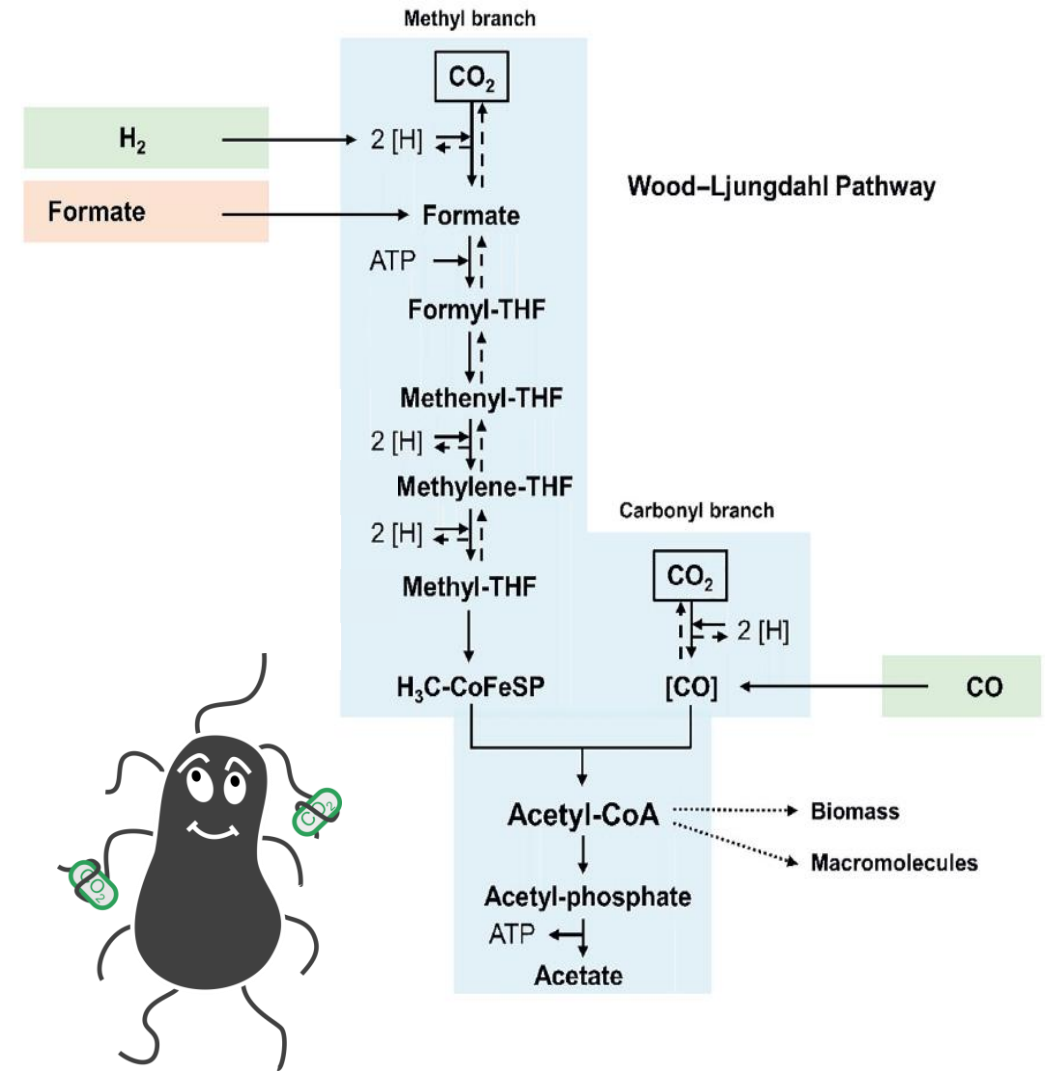


- Thermophilic acetogen ( $T_{opt} = 66\text{ °C}$ )
- Fast growth on  $H_2/CO_2$  [1]
- Sole CO utilization as carbon and energy source after adaptation [2]
- CO energetically more favorable than  $CO_2$
- Syngas: co-utilization of  $CO_2$ ,  $H_2$  and CO
- Mineral medium without yeast extract or vitamins [1]
- Wood-Ljungdahl pathway



[1] Leigh et al., 1981, Archives of Microbiology, <https://doi.org/10.1007/BF00414697>

[2] Weghoff and Müller, 2016, Applied and Environmental Microbiology, <https://doi.org/10.1128/AEM.00122-16>



Modified from: Müller, 2019, Trends in Biotechnology, <https://doi.org/10.1016/j.tibtech.2019.05.008>



1

Bottled gas + Serum bottle

- Fundamental survival
- Adaptation

2

Bottled gas + continuous culture

- Acetate production
- Parameter testing

3

100 kW DFB pilot plant +  
20 l bubble column reactor

- Coupling with “real” product gas
- proof of concept

4

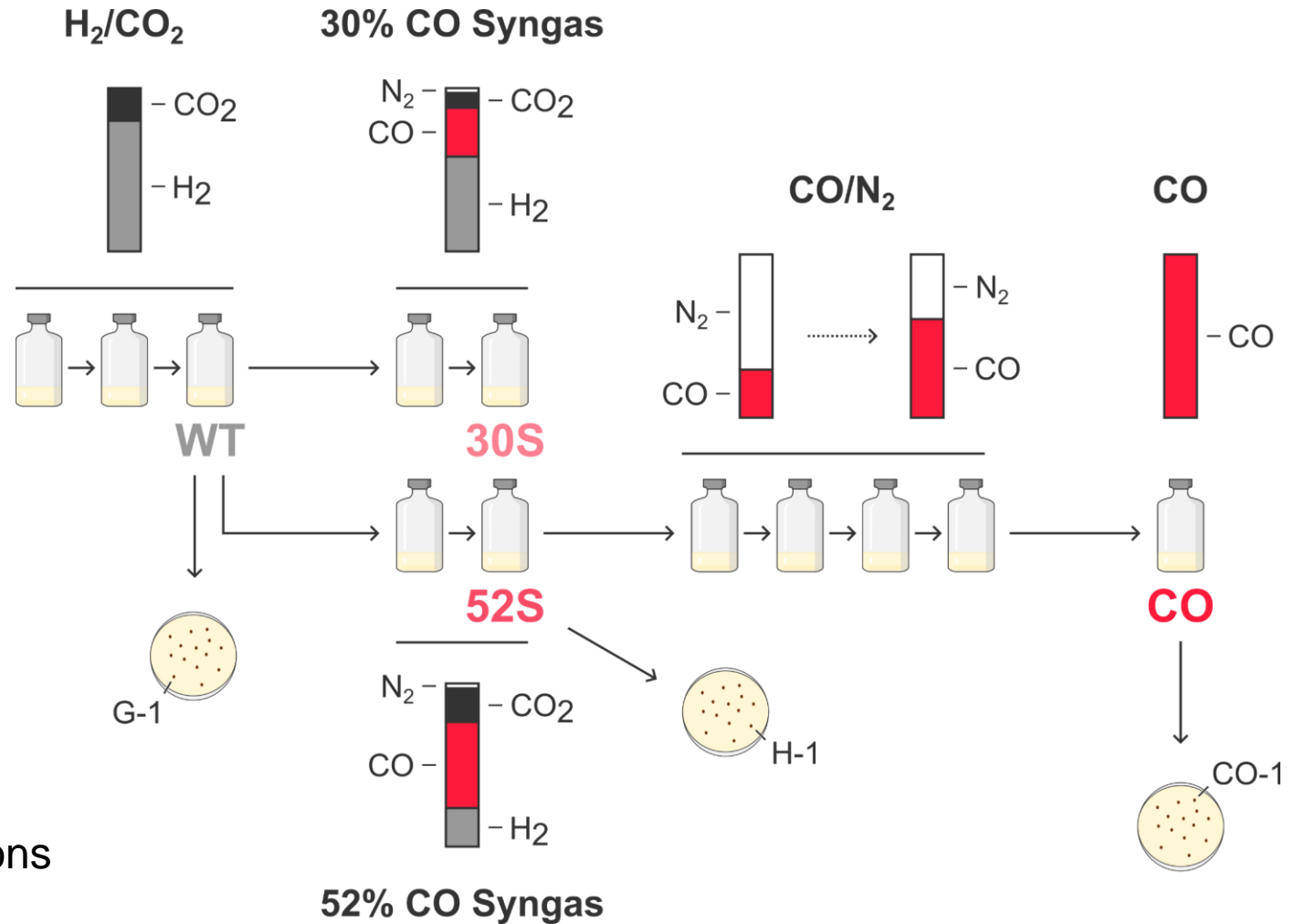
Bottled gas + Serum bottle

- Impurity tests

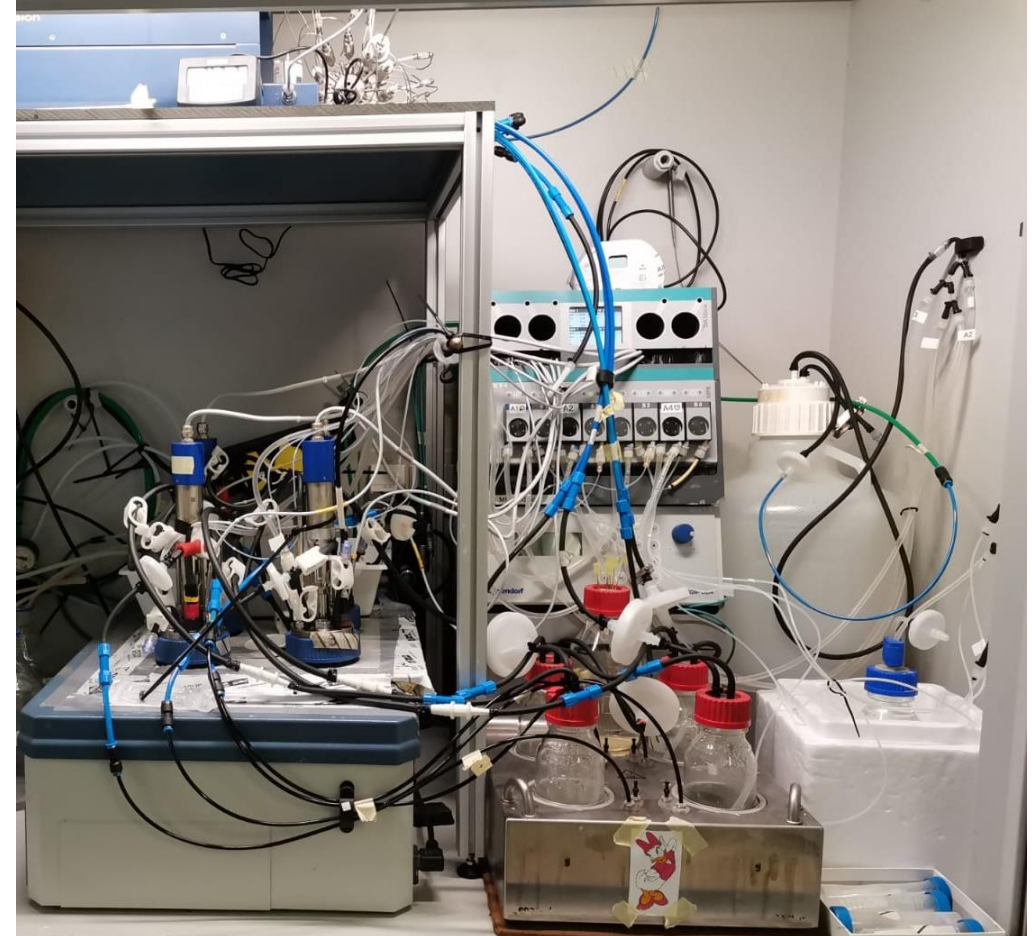
→ **Quick adaptation:**  
from H<sub>2</sub>/CO<sub>2</sub> to 100% CO  
in ~31 generations

→ **Fast growth on CO:**  
growth rates of 0.20-0.25  
h<sup>-1</sup> of *T. kivui* CO-1

adaptable to various syngas compositions

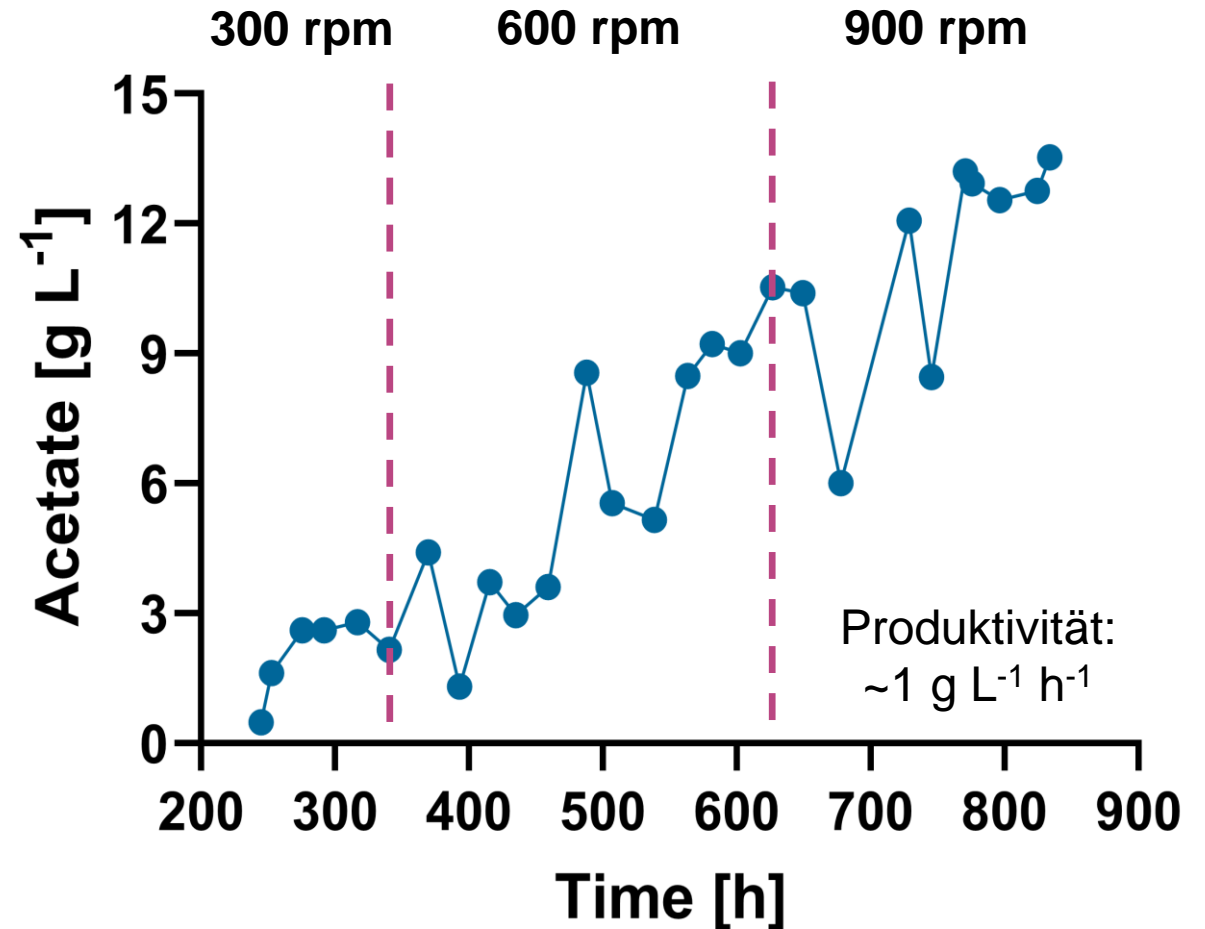


- 4x 200 mL parallel bioreactor system (DASBOX, Eppendorf)
- Continuous gas and liquid feeding (gas at 0.0633 vvm)
- Syngas composition: CO:H<sub>2</sub>:CO<sub>2</sub> 52:24:21
- Dilution rate: 0.075 h<sup>-1</sup>
- T = 66°C
- pH = 6.4

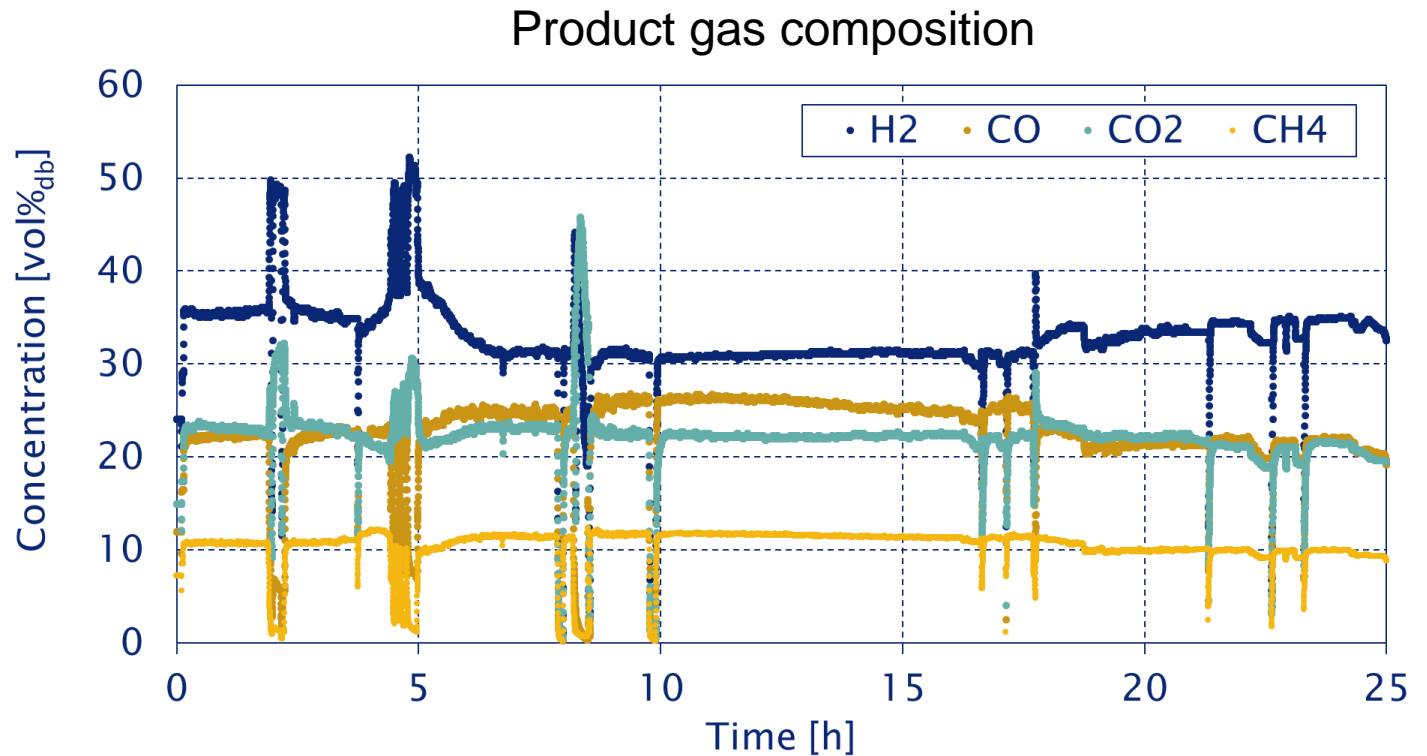




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  - Syngas composition: CO:H<sub>2</sub>:CO<sub>2</sub> 52:24:21
  - Dilution rate: 0.075 h<sup>-1</sup>
  - T = 66°C
  - pH = 6.4
- 
- 818 h of continuous growth and acetate production
  - Growth rate: 0.0766 h<sup>-1</sup>
  - Acetate productivity: 0.9527 g/l/h



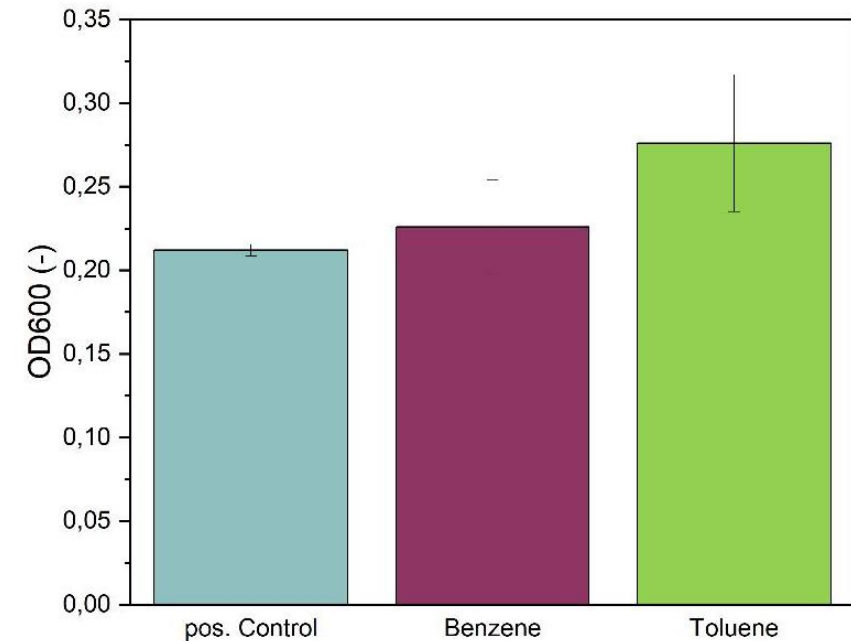
- Gasification of softwood pellets (~48 h)
- 25 h of coupled syngas fermentation
  - Bacteria growth rate:  
0.102 h<sup>-1</sup> (at 0.075 vvm)
  - Acetate productivity:  
0.083 g/l/h (at 0.075 vvm)
- Survival of bacteria (low enough oxygen contamination)
- Successful acetate production
- Productivity limited due to mass transfer limitations ( $k_L a$  value) of bubble column reactor



Could we use product gas downstream the biodiesel scrubber without activated carbon?

Typical impurities downstream of the biodiesel scrubber

Impurity	Concentration
Benzene	4000 ppm
Toluene	4000 ppm
H <sub>2</sub> S	25 ppm



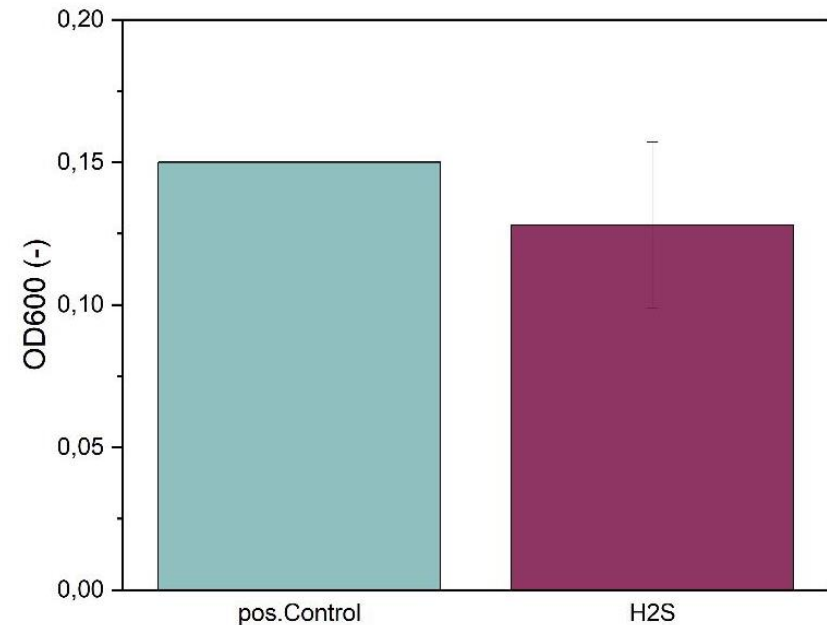


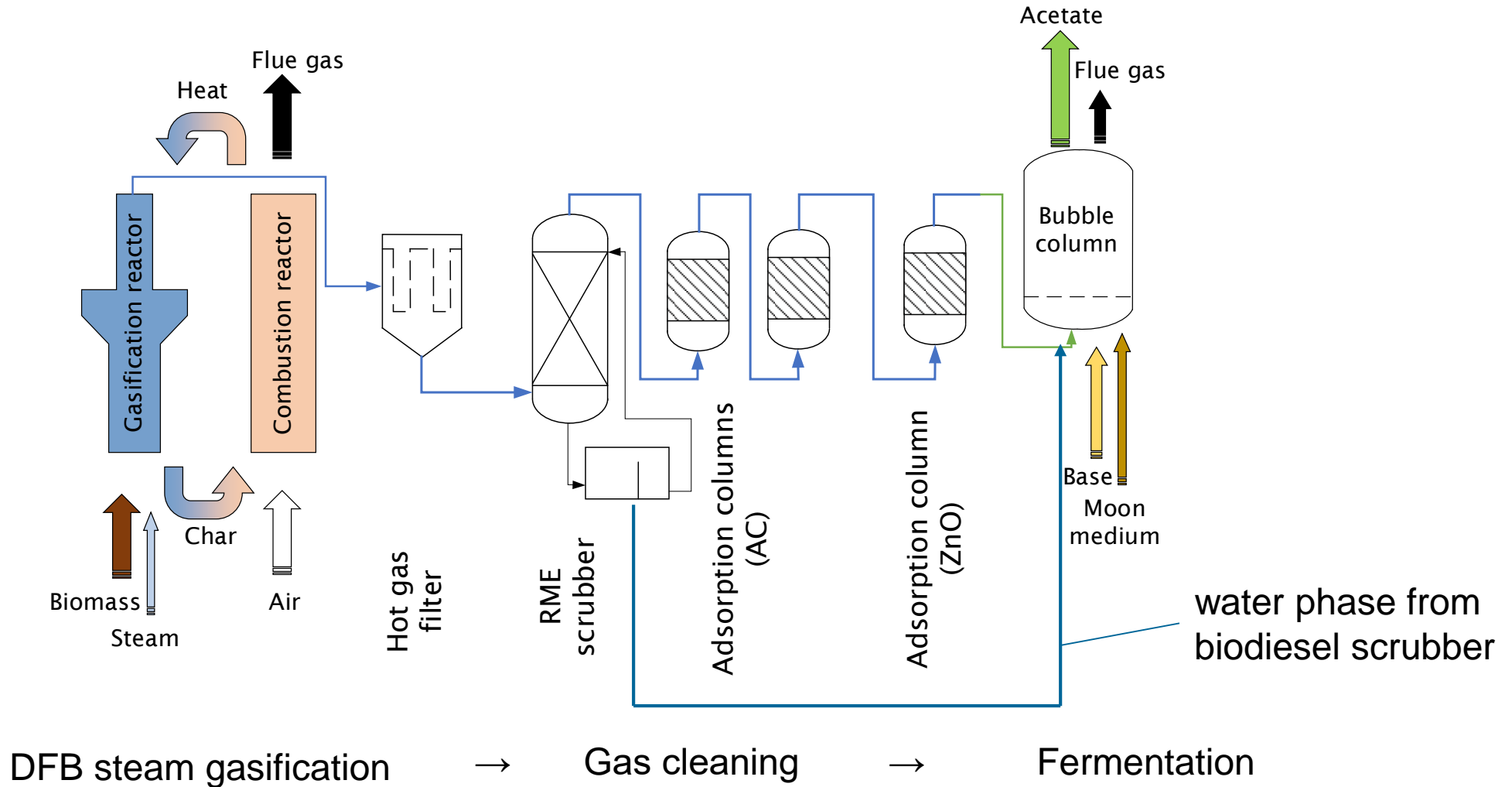
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Typical impurities downstream of the biodiesel scrubber

Impurity	Concentration
Benzene	4000 ppm
Toluene	4000 ppm
H <sub>2</sub> S	25 ppm

→ Use of product gas after RME scrubber conceivable





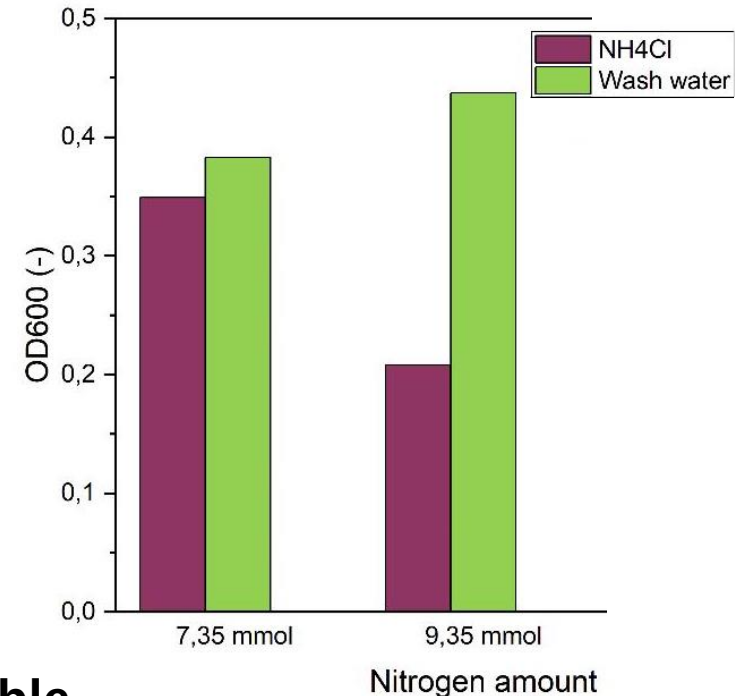
Steiner et al. 2024, in preparation

Could we use product gas downstream the biodiesel scrubber without activated carbon?

Typical impurities downstream of the biodiesel scrubber

Impurity	Concentration
Benzene	4000 ppm
Toluene	4000 ppm
H <sub>2</sub> S	25 ppm
Condensate*	unknown

\*From phase separator; Contains NH<sub>3</sub>, Phenol, Cyanate, Cyanide...



→ Use of water phase from biodiesel scrubber conceivable

Already tested and published for yeast production as well: <https://doi.org/10.3389/fbioe.2023.1179269>





## Biotechnology

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**Fuel and Energy  
System  
Engineering**



**CIRCE<sup>o</sup>**

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