

# Making small scale chemical production work

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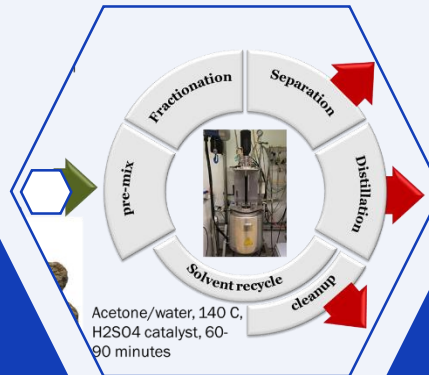


# Agenda



1. TNO and fuel development
2. Setting the scene
3. Explaining indirect gasification
4. Quick scan on the economics
5. Future outlook for MeOH production
6. Conclusions

# TNO and fuel development



Fabiola™ a pathway to 2<sup>nd</sup> generation sugars and furanic fuel components

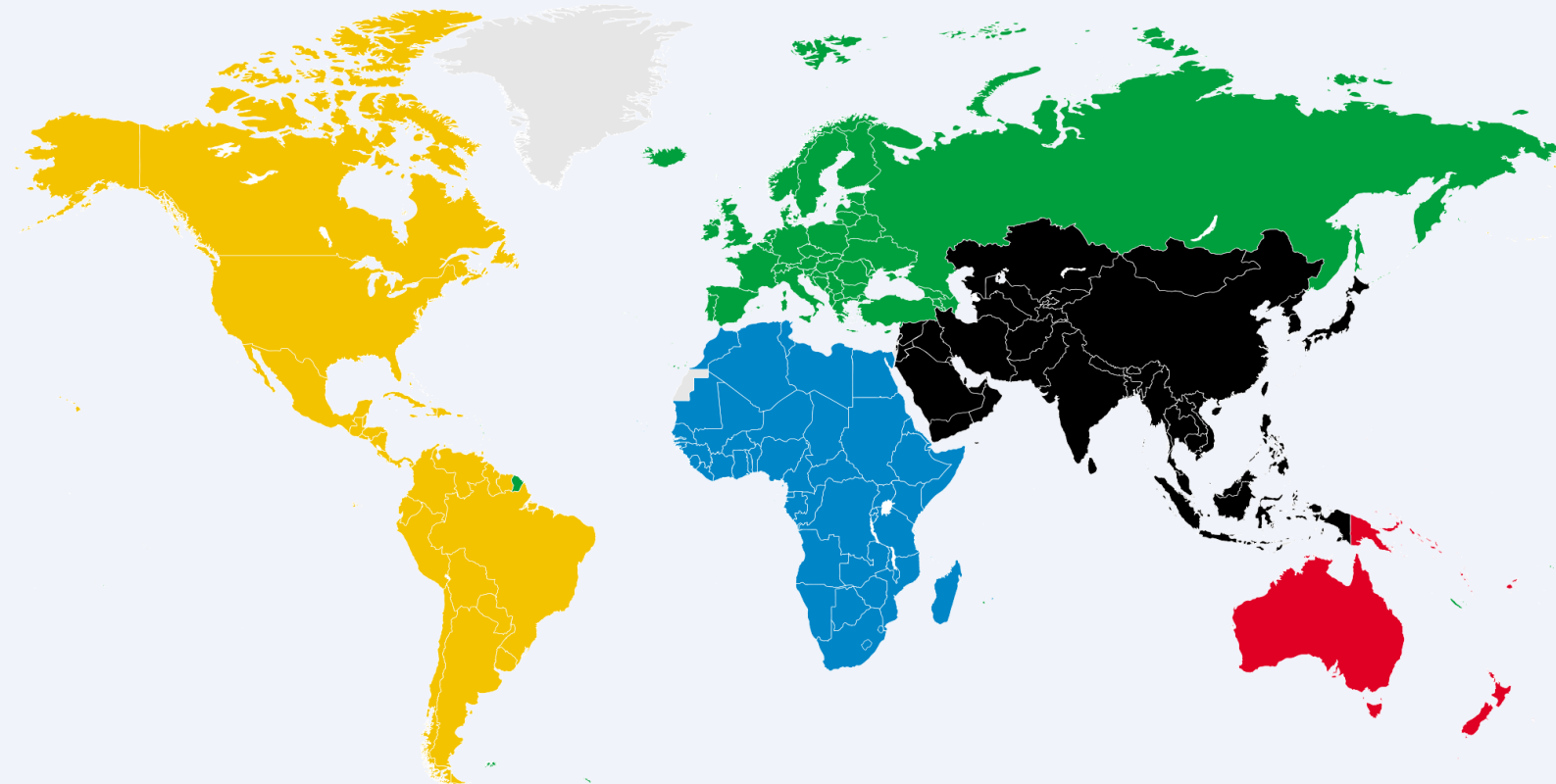
Indirect Gasification as a low cost, medium scale, pathway to MeOH

SEDMES technology for the conversion of synthesis gas (ratio agnostic) into r-DME

Hydro Thermal Upgrading converting wet organic reisdues into biocrude (55\$/barrel)



# Setting the scene



FB techn + oxygen Large  
EF + torrefaction Large  
Indirect approach Medium

Enerkem (2x) – Canada stopped  
+ under construction  
Fulcrum – USA stopped  
KEW – UK operation  
GoBiGas – Sweden stopped  
Enerkem – Spain announced  
Gidara – Netherlands  
RWE – Netherlands  
Salamandre – France  
BioTFuel – France  
ABSL - UK

# Three approaches towards gasification for fuel production



## Entrained flow gasification

Entrained flow gasification is characterized by high temperatures, small particles and oxygen usage, aiming to produce syngas.

- RWE – Furec
- BioTFuel
- SkyFuelH<sub>2</sub>
- Torrgas (not an exact fit)



## Direct gasification

Direct gasification is characterized by fuel flexible, limited in scale, typical fluidized bed technology and oxygen usage, aiming to produce syngas.

- Enerkem
- Gidara
- ABSL – Swindon
- KEW



## Indirect gasification

Indirect gasification is characterized by fuel flexible, semi-limited in scale, typical fluidized bed technology and **no** oxygen usage, aiming towards SNG production.

- Engie - Salamandre
- GoBiGas
- **TNO → MILENA**

Most direct approaches lead to syngas, subsequently used for H<sub>2</sub>, MeOH or SAF production

Indirect approaches, focussed on CH<sub>4</sub> production



# Syngas production is done in high temperature gasifiers!

*Can an indirect gasifier be used for syngas production and if so, what would be the best approach?*



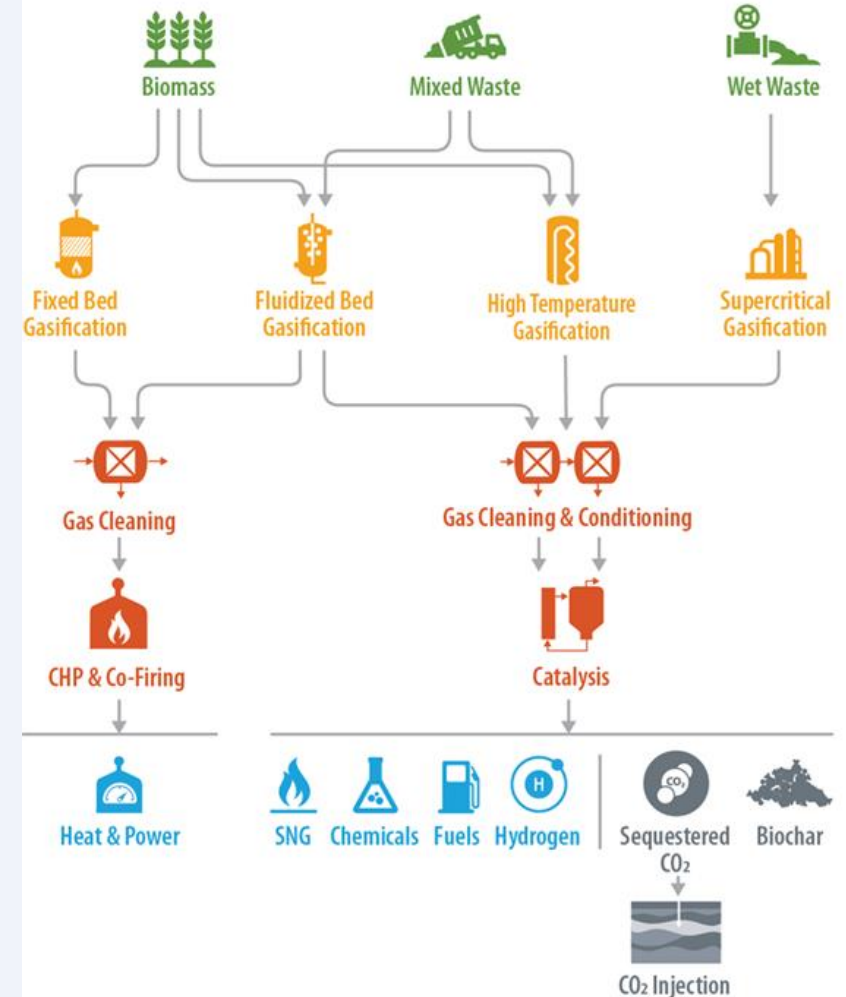


# Applications based on gasification

- Heat and Power (CHP)
- Green Gas (SNG/RNG)
- Chemicals (overlaps with fuels)
- Liquid fuels (MeOH, DME, LPG, FT)
- Hydrogen (with CCS)

Large amount of different applications, since the technology utilizes a syngas intermediate.

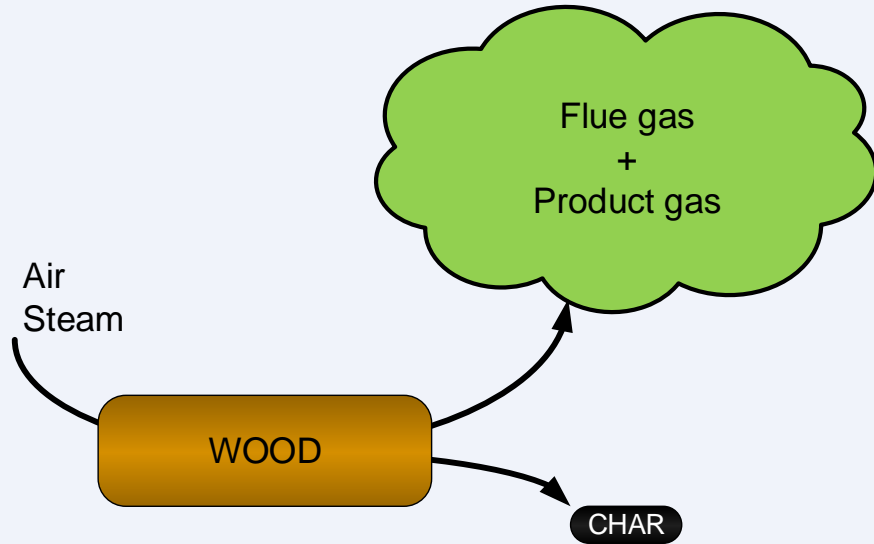
Even more technology options for the gasification itself



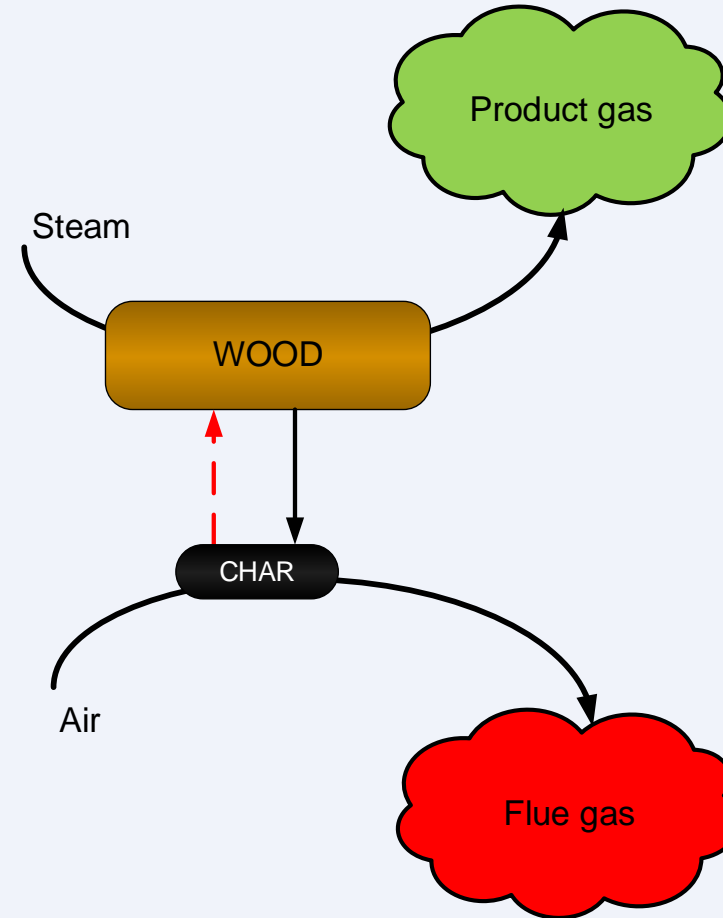


# Direct vs. Indirect gasification

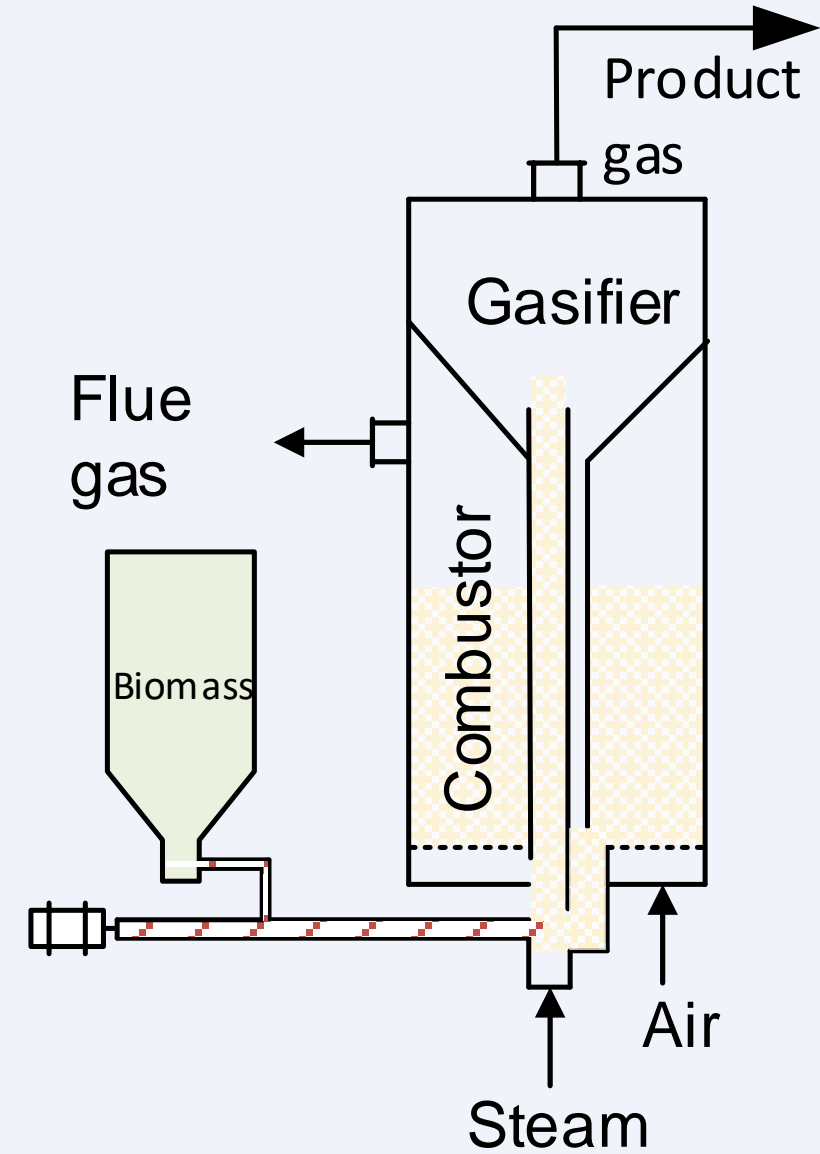
Direct gasification



Indirect gasification

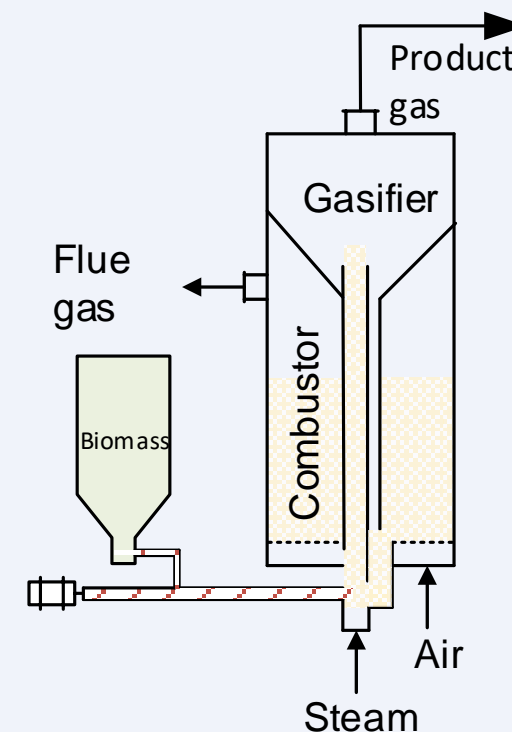


# Indirect gasifier - MILENA



# Indirect gasifier – MILENA

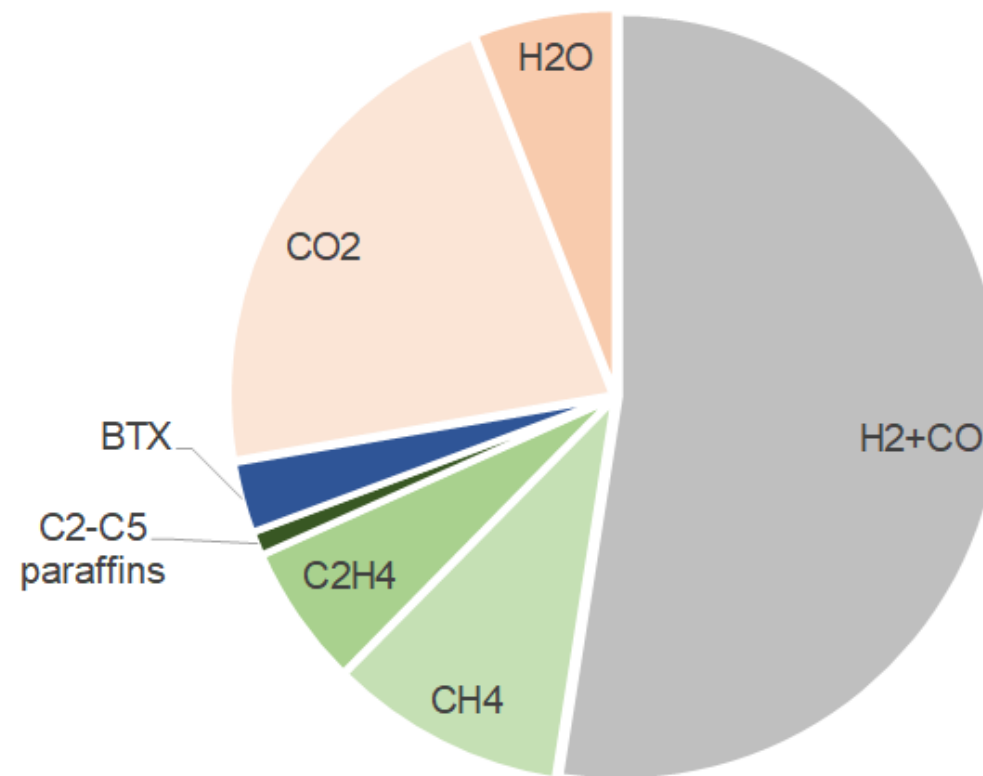
Characteristic	Description
Feedstock flow	6 kg/h max
Feedstock type (range)	biomass – RDF – plastic waste
Supply gases	N <sub>2</sub> , CO <sub>2</sub> , Air, Steam
Trace gases	Argon and Neon
Heating	Externally traced up to 900°C
Operating T	550 – 850 °C
Operating P	Atmospheric
Analysis	Product and flue gas





# Features of indirect gasification

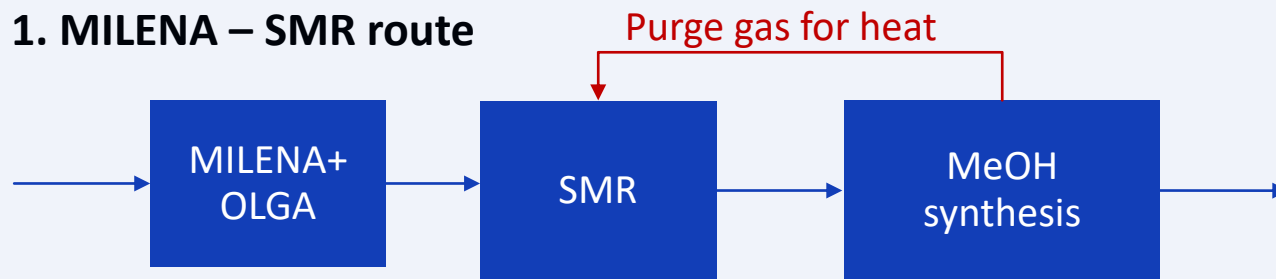
- + Complete feedstock conversion
- + High feedstock flexibility
- + Lower temperature levels in comparison to other syngas platforms
- + No oxygen required
- + Scalable, but economically interesting starting at small capacity (50 ktpa input)
- ? Not a direct route to syngas



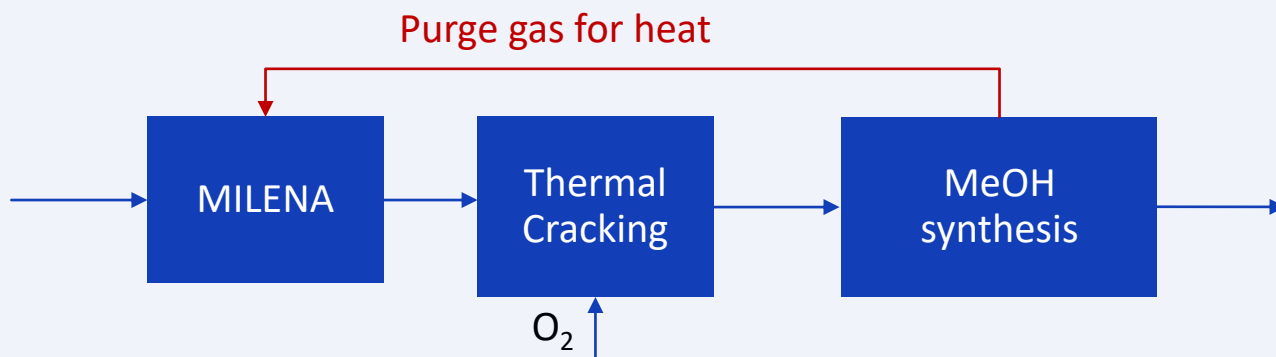
# Quick scan on the economics

- Biomass is extremely heterogeneous, scattered and has a different cost price compared to fossil → Scale will be limited
- Comparison of two pathways based on indirect gasification
- Based on first reasonable scale of 30 MWth input (~ 50 kton/y demolition wood feedstock)

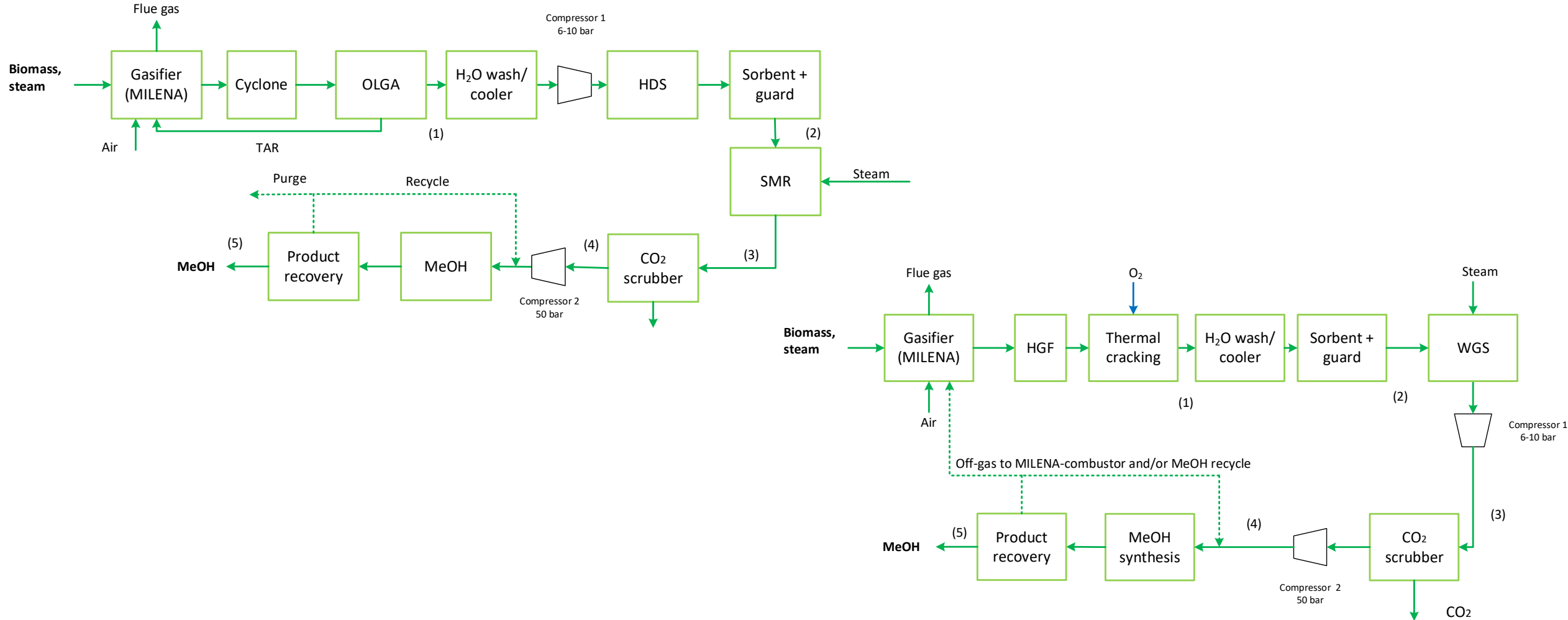
## 1. MILENA – SMR route



## 2. MILENA – Thermal cracking route

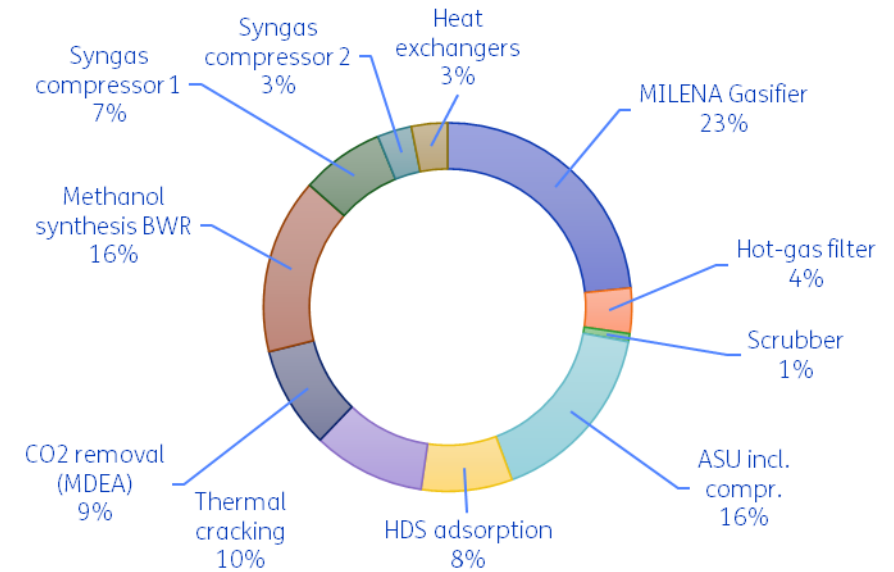
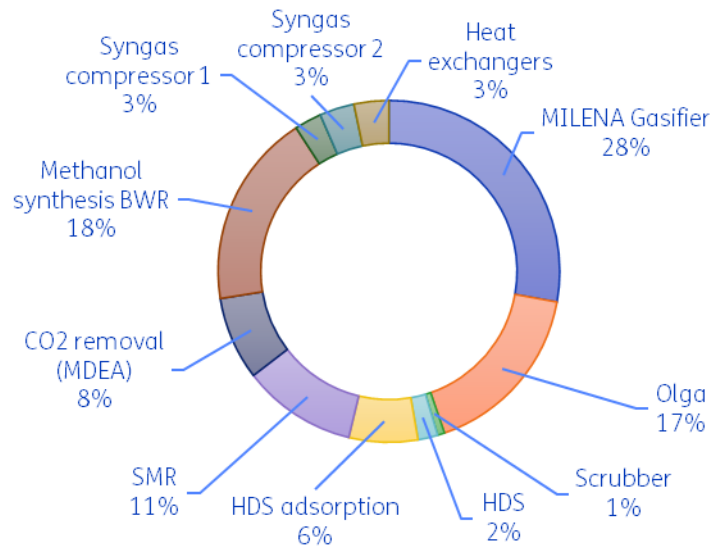


# Two processes modelled in ASPEN



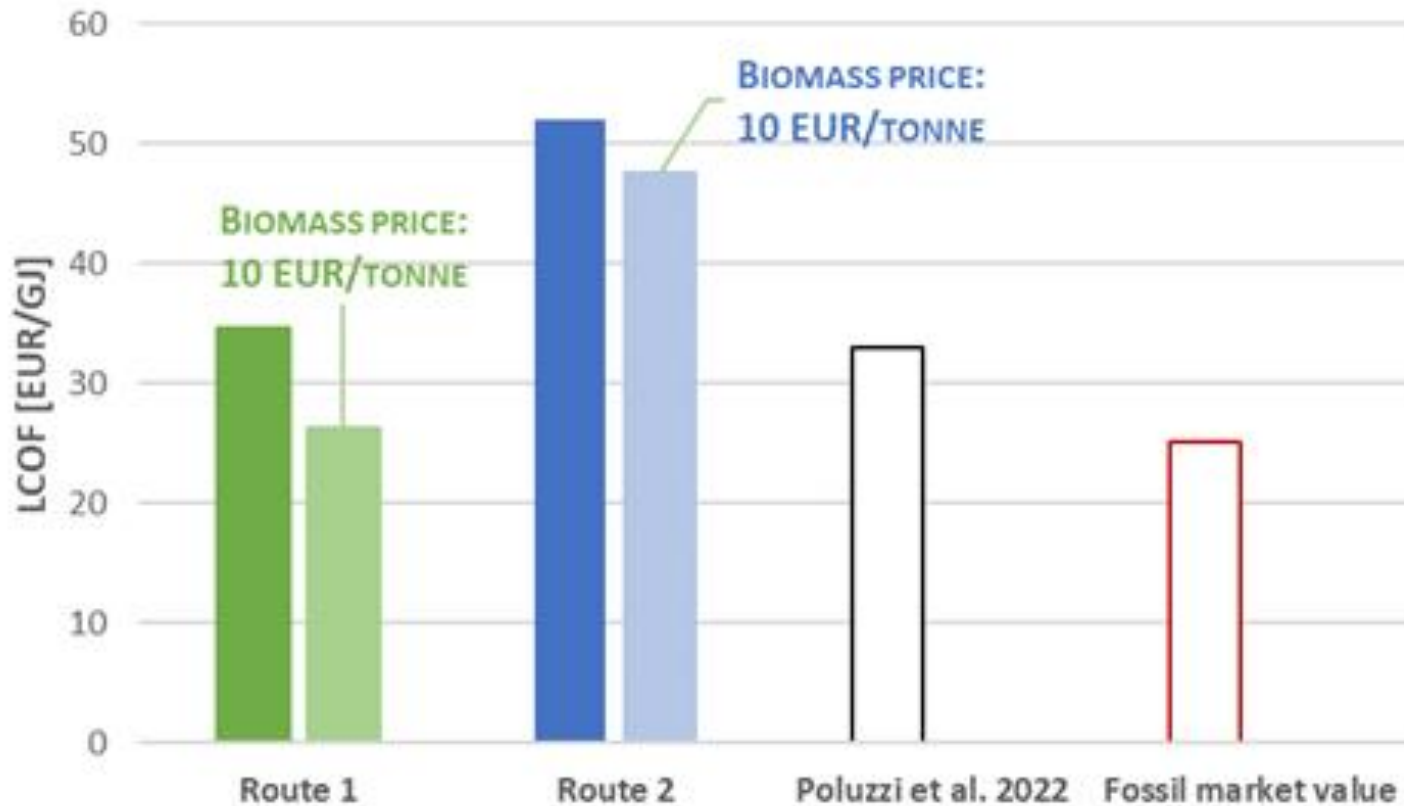


# Results of a TEA between the two systems



Route 1 MILENA SMR	Route 2 MILENA Thermal cracker
CAPEX 55 M€	CAPEX 63 M€
Fuel efficiency 62%	Fuel efficiency 57.5%
LCOF ~34 €/GJ	LCOF ~51 €/GJ
	CAPEX higher due to ASU and syngas compressor OPEX higher due to larger power consumption

# Comparison with other studies / fossil MeOH



- Biomass in base case is 30% of the overall LCOF, with a reduction of feedstock price this will reduce significantly the LCOF.
- The difference in CAPEX and efficiency translate to a big gap in LCOF for route 1 and 2.
- Study of Poluzzi includes direct (32,6 €/GJ) and indirect (34,2 €/GJ) gasification but both using and ASU to produce O<sub>2</sub>. Both also at very large scale (300ktpa)

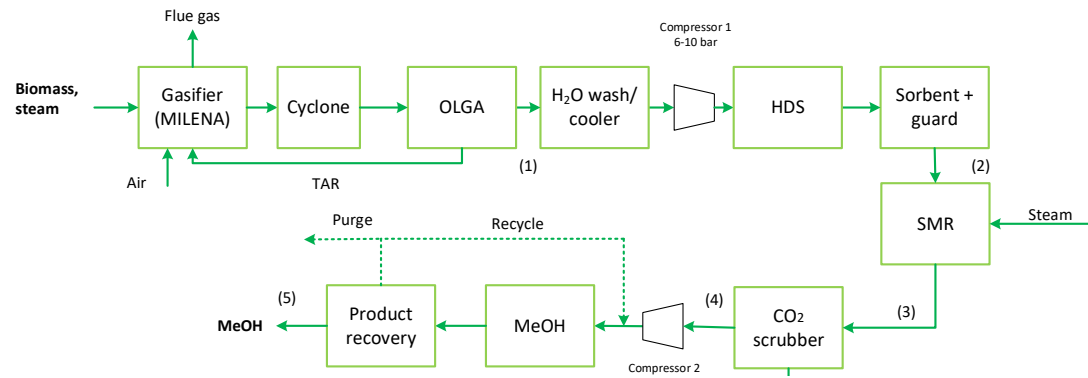
# Quick scan results

- Two indirect pathways compared
- Distinct differences in CAPEX for both routes
- Distinct differences in overall efficiency
- Feedstock prices becomes more dominant when overall CAPEX is lower

*The low temperature pathways to syngas (OLGA SMR) is looking more attractive from an efficiency and OPEX/CAPEX point of view*

Image of a MeOH flame ;-)





# Future outlook for MeOH production

- Focus on the processing steps after MILENA to generate the proper syngas quality for MeOH synthesis
- Develop a process design package
- Supporting LCA and TEA to identify weaknesses in the line-up
- Partnering to engage in a FEED study

# Conclusions


- TNO has several technology under development for the production of advanced fuels and/or developments that aid in the line up towards advanced biofuels
- Indirect gasification is a feedstock flexible, small to medium scale attractive pathway to produce advanced biofuels
- TNO is looking for partnership to:
  - Help develop your specific pathway by providing access to state of the art lab facilities.
  - Co-develop indirect gasification based value chains toward MeOH (DME, FT, H<sub>2</sub> etc not excluded)
  - Co-develop the back-end solutions for synthesis of biofuels taking into account the limited availability of feedstock and hence smaller scale compared to fossil routes.



# Thank you for your attention

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